Enzymatic Degradation of Synthetic Polymers

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Table of Contents

Tab	le of Content	I		
List	of Abbreviations			
Sco	pe & Outline	V		
<u>1.</u>	BACKGROUND	1		
1.1.	PLASTIC – ADVANTAGES AND DISADVANTAGES OF A CONTROVERSIAL POLYM	IER1		
1.2.	TYPES OF PLASTIC	2		
1.3.	RECYCLING OF PLASTIC	3		
1.4.	ENZYMATIC DEGRADATION OF POLYETHYLENE TEREPHTHALATE	5		
1.4.	1. IMPROVING REACTION PERFORMANCE OF PET HYDROLASES	8		
1.4.	2. PET OLIGO- AND MONOMER DEGRADING ENZYMES	9		
1.5.	PROTEIN ENGINEERING	10		
1.6.	DEGRADATION OF POLYVINYL ALCOHOL	12		
1.6.	1. MICROBIAL DEGRADATION OF POLYVINYL ALCOHOL	13		
1.6.	2. ENZYMATIC DEGRADATION OF POLYVINYL ALCOHOL	15		
2.	RESULTS & DISCUSSION	16		
2.1.	MECHANISM AND STRUCTURAL INSIGHTS INTO PET DEGRADING ENZYMES			
2.1.	1. MECHANISM-BASED DESIGN OF EFFICIENT PET HYDROLASES (ARTICLE I)	16		
2.1.	2. STRUCTURAL INSIGHTS INTO (TERE)PHTHALATE-ESTER HYDROLYSIS	BY A		
CAF	BOXYLESTERASE AND ITS ROLE IN PROMOTING PET DEPOLYMERIZATION (ARTIC	le II) .20		
2.2.	2.2. DEGRADATION OF MODIFIED POLYVINYL ALCOHOL USING AN ENZYMATIC CASCADE			
	(ARTICLE III)	23		
<u>3.</u>	CONCLUSION	27		
4.	REFERENCES	29		
<u>э.</u>	AUTHOR CONTRIBUTIONS			
Articles				
Article 141				
Article 2				
Article 3				
Eigenständigkeitserklärung111				
List of Publications				
Ack	Acknowledgements115			

List of Abbreviations

ADH	Alcohol dehydrogenase
BDH	β -diketone hydrolase
BHET	Bis(2-hydroxyethyl) terephthalate
BVMO	Baeyer-Villiger monooxygenase
СНМО	Cyclohexanone monooxygenase
Cryo-EM	Cryo-electron microscopy
DEP	Diethyl phthalate
DNA	Deoxyribonucleic acid
DMT	Dimethyl terephthalate
E. coli	Escherichia coli
EG	Ethylene glycol
GPC	Gel permeation chromatography
HPLC	High-performance liquid chromatography
HTS	High throughput screening
<i>ls</i> PETase PM	<i>Is</i> PETase ^{S121E/D186H/R280A/N233C/S282C}
I. sakaiensis	Ideonella sakaiensis
LCC	Leaf-compost cutinase
LK-ADH	Alcohol dehydrogenase from Lactobacillus kefir
LMWPs	Low-molecular-weight products
MEP	Monoethyl phthalate
MHET	Mono-(2-hydroxyethyl)-terephthalic acid
M _n	Average molecular weight
M _w	Weight average molecular weight
NMR	Nuclear magnetic resonance
PA	Phthalic acid
PCR	Polymerase chain reaction

PDI	Polydispersity index
PE	Polyethylene
PET	Polyethylene terephthalate
PETase	PET hydrolase
P. pastoris	Pichia pastoris
PQQ	Pyrroloquinoline quinone
PS	Polystyrene
PVA	Polyvinyl alcohol
PVA-DH	PVA dehydrogenases
SA	Succinic anhydrate
TfCa	Carboxylesterase from T. fusca
T. fusca	Thermobifida fusca
Tg	Glass transition temperature
T _m	Melting temperature
TPA	Terephthalic acid
TTCE	Thermus thermophilus carboxylesterase
UHPLC	Ultra-high performance liquid chromatography
wt	Wildtype
3PET	Bis[2-(benzoyloxy)ethyl] terephthalate

In addition to the listed abbreviations, the one-letter codes for proteogenic amino acids, units based on the International System of Units (SI), and SI-derived units were used.

Scope & Outline

This work investigated the enzymatic degradation of polyethylene terephthalate (PET) (**Articles I and II**) and polyvinyl alcohol (PVA) (**Article III**). Physical or chemical degradation of plastic polymers is often performed under extreme conditions like high temperatures or pressure. In comparison to that, recycling of plastics with enzymes can be carried out at ambient temperatures and neutral pH. Enzymes themselves are non-toxic, environmentally friendly, and have been used successfully in a variety of industrial processes.

Enzymatic degradation of polyesters is well studied. Their heteroatomic backbone, which is connecting monomers via ester bonds offers a target for an enzymatic attack. Especially PET, one of the most common polyesters, has been in the focus of research. The first enzyme capable of degrading the polymer was found in 2005. Since then, researchers discovered several enzymes with similar functions and subjected them to enzyme engineering. Improving the enzyme's substrate affinity, activity, and stability aims at making PET recycling more efficient. **Article I** provides an overview of limitations that enzymatic PET recycling is still facing and the research carried out to overcome them. More precisely, enzyme–substrate interactions, thermostability, catalytic efficiency, and inhibition caused by oligomeric degradation intermediates are summarized and discussed in detail.

Article I Mechanism-Based Design of Efficient PET Hydrolases

R. Wei, <u>G. von Haugwitz</u>, L. Pfaff, J. Mican, C. P. S. Badenhorst, W. Liu, G. Weber, H. P. Austin, D. Bednar, J. Damborsky, U. T. Bornscheuer, *ACS Catal.*, **2022**, *12*, 3382–3396.

Article II further addresses one of the above-mentioned limitations, namely product inhibition of PET hydrolyzing enzymes. We elucidated the crystal structure of TfCa, a carboxylesterase from *Thermobifida fusca* (*T. fusca*), and applied semi-rational enzyme engineering. The article discusses the structure-function relationship of TfCa based on the apo-structure as well as ligand-soaked structures. Furthermore, it compares the structures of TfCa and MHETase, another PET hydrolase helper enzyme. Lastly, we determined the substrate profile of the carboxylesterase based on terephthalate-based oligo-esters of various lengths and one *ortho*-phthalate ester. In a dual enzyme system, TfCa degraded intermediate products derived from the PET hydrolysis of a variant of PETase hydrolase from *Ideonella sakaiensis* (*I. sakaiensis*). The dual enzyme system utilized PET more efficiently in comparison to solely PETase due to relieved product inhibition. Since TfCa

successfully degraded oligomeric intermediates, the reaction not only released terephthalic acid as the sole product but also increased the overall product yield.

 Article II Structural Insights into (Tere)phthalate-ester Hydrolysis by a Carboxylesterase and its Role in Promoting PET Depolymerization G. von Haugwitz, X. Han, L. Pfaff, Q. Li, H. Wei, J. Gao, K. Methling, Y. Ao, Y. Brack, J. Mican, C. G. Feiler, M. S. Weiss, D. Bednar, G. J. Palm, M. Lalk, M. Lammers, J. Damborsky, G. Weber, W. Liu, U. T. Bornscheuer, R. Wei, ACS Catal., 2022, accepted.

While PET contains an ester bond that can be attacked and hydrolyzed by esterases or lipases, PVA consists of a homoatomic C-C-backbone with repeating 1,3-diol units. The polymer is water soluble with remarkable physical properties such as thermostability and viscosity. PVA is often described as biodegradable, but microbial degradation is slow and frequently involves cost-intensive cofactors. In this study, we present an improved PVA polymer with derivatized side chains and an enzyme cascade that can degrade not only modified but also unmodified PVA in a one-pot reaction. The enzyme cascade consists of a lipase, an alcohol dehydrogenase (ADH), and a Baeyer-Villiger monooxygenase (BVMO). In comparison to the scarcely published research on PVA degradation with free enzyme, this cascade is not only independent from the frequently required cofactor pyrroloquinoline quinone (PQQ) but, in principle, contains an *in vitro* cofactor recycling mechanism.

Article III Synthesis of Modified Polyvinyl Alcohols and their Degradation Using an Enzymatic Cascade <u>G. von Haugwitz</u>, K. Donnelly, M. Di Filippo, D. Breite, M. Phippard, A. Schulze, R. Wei, M. Baumann, U. T. Bornscheuer, Angew. Chem. Int. Ed., under review.

1. Background

1.1. Plastic – Advantages and Disadvantages of a Controversial Polymer

Synthetic polymers have been manufactured on industrial scales since the 1950s and have contributed to society with health and safety benefits.¹ Plastics are widely used in a variety of applications, including food packaging and medical applications. The polymer's resistance to degradation was regarded one of the most significant advantages, alongside lightness, low cost, and ease of processing. These material properties make plalstics suitable materials for a broad spectrum of applications.² The two largest end-use markets of plastics are packaging and building construction which together make up for over 60 % of the plastic demand.¹ However, due to their persistence, polymers have become a major source of pollution in the environment. Around 307 million tons of plastic were produced worldwide in 2020¹ and it is estimated that 12,000 million metric tons of plastic will accumulate in the environment by 2050 primarily in landfills and oceans making plastic the fourth most common type of waste.³ This is partly because 40 % of the produced plastic is employed for single-use applications.⁴

In addition to the poor waste management of end-of-life products, the entire lifecycle of plastic products impacts the ecosystem. Microfibers from textile production and maintenance (e.g., from laundry wastewater) and microplastics (MPs) from shower gels or toothpaste, are accumulating in both terrestrial and marine ecosystems.^{4–6} The consequences for these ecosystems are tremendous. Aside from the obvious concerns such as physical harm to wildlife animals, there are less obvious and more long-term consequences.⁶ Plastic debris can transport invasive species, pathogens, or harmful algal bloom species over long distances and thus from one ecosystem to another.^{7,8} Toxic compounds used to gain desired properties of plastics, such as Bisphenol A or plasticizers, and MPs are eaten by fish and can accumulate up the food chain thereby also affecting human health.^{9–13}

Even though the research on terrestrial environments is still limited, MPs with a size <5 mm were found in many different soil samples. According to current estimations MPs are present in every terrestrial ecosystem.¹⁴ In soil, MPs potentially impact microbial activity and root growth or provide toxins that penetrate plants.^{14,15} Thus, plastic management is an urgent and important issue that researchers from all over the world address in various disciplines. In addition to lowering plastic consumption and reusing plastic items, recycling the polymers is a significant aspect of plastic management with the objective of a circular plastic economy.¹⁶

1.2. Types of Plastic

Plastics can be categorized into fossil-based chemicals or bio-based polymers with the vast majority of the synthetic polymer being fossil-based.¹⁷ While bio-based polymers derive from renewable sources such as corn, starch, or cellulose, fossil-based plastics are polymers made from petrochemicals and are commonly considered traditional plastics.¹⁶ Fuel-based plastics comprise varying chemical structures and can be further subdivided by the bonds linking the building blocks. Regarding enzymatic degradation, polymers containing a homoatomic carbon-carbon backbone are the most difficult to degrade due to their lack of a functional group for an enzymatic attack. Nevertheless, polymers with a carbon-carbon backbone represent 77 % of global plastics.³ Examples of synthetic polymers with a homoatomic backbone are polyethylene (PE), polypropylene (PP), and polystyrene (PS). Several kinds of plastics and their respective bond linkages are presented in **Figure 1**.



Figure 1: Examples of different types of plastics. The plastics can be subdivided by their chemical structure, or more specifically, by their bond linkages: ester bonds (blue), urethane bonds (pink), ether bonds (green) and carbon-carbon bonds (red). Plastics with a homoatomic carbon-carbon backbone are the most difficult substrate for enzymatic degradation due to the lack of a functional group for biocatalysts to attack.

1.3. Recycling of Plastic

Even though plastic recycling already started in the 1980s, up to today plastic waste management primarily entails accumulation in landfills or incineration for energy recovery.³ The diversity and complexity of the polymer material, especially in multilayer packaging materials, requires a time- and cost-intensive presorting of post-consumer plastic waste for most recycling methods. High energy costs and a low-quality polymer output of existing recycling methods combined with the low production costs of virgin polymers, render plastic recycling unattractive for the industry.¹⁸ In addition to incineration for energy recovery, plastic recycling can also be achieved mechanically or chemically. All of these pathways have advantages, disadvantages, and limitations which are further discussed in the following.

Mechanical recycling produces secondary items from plastic recycling. These items are mostly low-value products since mechanical processing alters the properties and structure of the recycled polymer.¹⁹ The procedure utilizes large-scale solid waste which is shredded, melted, and remolded into new plastic materials.⁴ Prior to mechanical recycling, the post-consumer waste is sorted by material properties such as size, color, and density as well as polymer type. An additional washing step removes organic material and other contaminants.¹⁶ The need for this extensive pretreatment of the diverse material results in increased processing costs.¹⁶ Furthermore, the approach has limited processing cycles, delaying eventual disposal rather than contributing to a circular plastic economy.²⁰ Combining the outcome of mechanical recycling with virgin plastic, can improve the quality of the resulting product. However, the need for virgin plastic makes mechanical recycling less efficient.

A sub-category of mechanical recycling is primary recycling which refers to reusing the product without altering it. This recycling process is performed for pre-consumer plastic waste that accumulates during plastic manufacturing. After mechanical recycling, the pre-consumer plastic can be returned to the plastic-manufacturing loop.²⁰ However, primary recycling requires the polymer to be pure and uncontaminated and, as in general mechanical recycling, the recycled material loses its integrity and stability.

In the process of incineration, the polymer itself is not recycled but the energy contained in the polymer is released. The energy content of plastics like PE and PP was measured to be above 40 MJ/kg and thus comparable to gasoline, kerosene, and diesel.²¹ At a first glance, recycling energy appears to be a viable approach to recycle plastic. However, burning plastic requires cost-intensive pollution control mechanisms. Furthermore, new plastics must be synthesized from non-renewable resources. As a

result, incineration is a less desirable approach for environmental and economic reasons than mechanical recycling. However, in comparison to other recycling methods, no presorting of plastic waste is needed.

Chemical recycling is for example used for PET post-consumer waste to regain lowmolecular-weight products (LMWPs) by thermolysis or monomers by solvolysis. Depending on the chemical reaction, PET can be depolymerized into bis(2-hydroxy-ethyl) terephthalate (BHET), terephthalic acid (TPA), or dimethyl terephthalate (DMT). Methanolysis and glycolysis of PET are performed under high temperature (up to 280 °C) and high pressure (up to 4 MPa) using methanol or glycols such as EG for the depolymerization process.²² The monomers are subsequently purified and used for the synthesis of virgin polymers.²³

For the chemical recycling of PE, Jia et. al. published an efficient and selective cascade depolymerization using a co-catalyst system that can perform at comparably low temperatures around 150 °C.²⁴ However, the authors could not achieve recovery of monomers from their system which is needed for high-quality recycled plastics.

In general, chemical recycling improves the qualitative outcome of the gained polymers in comparison to mechanical recycling techniques. However, the drawback of this method is the need for expensive catalysts, high temperatures, and pressures as well as purity of the post-consumer plastic.^{4,25} Furthermore, in chemical recycling, additives such as dye and plasticizers can influence and impede the reaction.^{20,26}

Combining different approaches could overcome the limitations of each recycling process. Sullivan et. al. recently reported a hybrid recycling system that uses metal-catalyzed autooxidation to depolymerize mixed plastic waste which is then further used as a substrate for biological conversion by *Pseudomonas putida* to yield useful chemical products such as β -ketoadipate and polyhydroxyalkanoates.²⁷

In comparison to the afore-mentioned recycling processes, enzymatic or microbial degradation of plastics have two major advantages: a high selectivity of the biocatalyst which allows the complete depolymerization of the polymer into monomers as well as a performance at ambient temperatures, decreasing the energy costs of the recycling process. However, for cost-efficient enzyme recycling of plastic, much research must still be conducted not only to identify enzymes capable of performing this task but also to improve the activity as well as stability of such enzymes.⁴

1.4. Enzymatic Degradation of Polyethylene Terephthalate

When it comes to enzymatic recycling of plastics, polyesters are currently the most investigated group, especially PET has been the subject of many studies of enzymatic degradation.²⁸ The aromatic polymer contains repeating TPA and EG and is used for the production of plastic bottles and textiles, among other things. In industry, PET is valued for its hydrophobicity and thermoplastic properties. PET accounts for approximately 10 % of global plastic waste, various recycling routes are described, and, in some cases, industrially applied. Despite that only 10 % of the produced PET is being recycled.¹⁹

In recent years, enzymatic depolymerization of PET has emerged as an alternative technology to conventional mechanical and chemical plastic recycling approaches. While the microbial and enzymatic degradation of most plastics is still intensively discussed among researchers, enzymatic polyester degradation and recycling evolved fast in recent years. The heteroatomic backbone of PET containing ester bonds makes the polymer accessible for enzymatic hydrolysis.²⁹ PET degrading enzymes are commonly from the α/β -hydrolase fold family, which cleave ester bonds by the addition of water. Enzymes from this family originate from varying phylogenetic branches and differ in their catalytic function and include lipases, esterases, amidases, and proteases, among others.³⁰ They are mainly characterized by an α/β -folding motif composed of eight, mostly parallel β -sheets which are stabilized and connected by six α -helices (**Figure 2**).³¹



Figure 2: Representation of the α/β **-hydrolase fold.** Six α -helices are shown as red columns (A-F) which are connecting and stabilizing the eight mostly parallel β -sheets depicted as blue arrows (1-8). Amino acids of the catalytic triad are shown as red spheres. Instead of aspartic acid, the catalytic triad can also contain glutamic acid. The figure was adapted from Bornscheuer et. al..³²

The catalytic triad of α/β -hydrolases consists of a nucleophilic serine, glutamic acid or aspartic acid, and histidine. The ester hydrolysis is performed in three steps. First, the substrate binds in the active site and is attacked by the nucleophilic serine. The first tetrahedral intermediate is formed and stabilized by an oxyanion hole which is created by

the backbone of conserved amino acids close to the catalytic triad. Second, through the nucleophilic attack, an alcohol is formed as the first product and released from the serine which results in the formation of an acyl-enzyme complex. Lastly, the nucleophilic attack of water forms a second tetrahedral intermediate within the acyl-enzyme complex. The collapse of the second intermediate leads to a carboxylic acid function in the substrate as well as the free enzyme.³²

Enzymatic PET hydrolysis produces small-molecule degradation products which can be recovered and used for the synthesis of virgin polymers (**Figure 3**).^{5,6} In addition to the desired PET monomers TPA and EG, BHET and mono-(2-hydroxyethyl)-terephthalate (MHET) are often gained as intermediate products and can cause inhibition of selected PET hydrolases.^{33,34} Biocatalytic recycling of PET is a promising approach which is already successfully performed at laboratory and pilot plant scales.^{35,36}



Figure 3: Enzymatic degradation of PET. The PET polymer, consisting of EG and TPA connected by ester bonds, can be degraded by PET hydrolyzing enzymes. The main aromatic products of enzymatic PET degradation are the building block TPA as well as the intermediate substrates BHET and MHET which are known to cause inhibition of selected PET hydrolases.

So far, over 20 enzymes with PET degrading ability have been described and can be classified as esterases (EC 3.1.1.) or more specifically, as carboxylesterases (EC 3.1.1.1.), cutinases (EC 3.1.1.74) and lipases (EC 3.1.1.3.).³⁷ PET hydrolyzing enzymes are often characterized by an active site close to the surface as well as an active cleft providing enough space for macromolecules and a high affinity towards hydrophobic

materials.³⁸ The first enzyme with a PET hydrolase-like activity, *Tf*H from *T. fusca*, was discovered in 2005 by Müller et. al.³⁹ This hydrolase can convert over 50 % of meltquenched post-consumer PET film at 55 °C within three weeks.³⁹ In the years after the discovery of *Tf*H, more PET cutinases were found in the *Thermobifida* species which includes *T. fusca*, *T. alba*, and *T. cellulosilytica*.⁴⁰⁻⁴²

Another milestone in PET degradation was reached in 2016 when Yoshida et. al. discovered that the mesophilic bacterium *I. sakaiensis* can utilize PET as a source of carbon under laboratory conditions.²⁹ The authors isolated and characterized *Is*PETase, an enzyme with the remarkable ability to degrade highly amorphous PET at ambient temperatures.²⁹ The enzyme consists of 290 amino acids and can function as a monomer. The crystal structure of *Is*PETase was solved and revealed a central β -sheet composed of nine mixed β -strands as well as seven α -helixes. The overall surface of the biocatalyst is highly polarized, as evident for many PET hydrolases, resulting in an isoelectric point of 9.6.^{28,43} Furthermore, the enzyme contains two disulfide bridges, one between C203 and C239 and the other one between C273 and C289, that are stabilizing the protein. The first disulfide bridge is thought to be crucial for the activity of *Is*PETase by providing the structural basis for the positioning of the catalytic histidine.^{44,45} In the following years, *Is*PETase was intensively studied^{29,46} and engineered towards a higher thermostability⁴⁷ and activity⁴⁸. A new enzyme class, the PET hydrolase class, (EC 3.1.1.101) was created.³⁷

A variant of leaf-compost cutinase (LCC), so far outperforms all other discovered PET hydrolases and their engineered variants at high temperatures.³⁵ Tournier et. al. described 90 % depolymerization of amorphized PET into monomers after treatment of the polymer with an improved variant of LCC for 10 h at 72 °C.³⁵ The enzyme also folds as an α/β -hydrolase and is composed of nine β -strands forming the β -sheet as well as eight α -helices and strongly resembles the previously elucidated structure of a cutinase from *T. alba.*⁴⁹ A protruding groove that is built from a hydrophobic amino acid patch and extended from the catalytic pocket promotes the binding of long-chain substrates.⁴⁹ Molecular docking of a model substrate confirmed the role of the groove in substrate binding and made it a target for enzyme engineering. Eleven residues within the hydrophobic groove were chosen by Tournier et. al. for mutagenesis. Two mutations (F243I/W) showed improved activity and four others an enhanced melting point (T69M, Y127G, N246D/M) in comparison to the wildtype enzyme.³⁵ The combination of the mutations resulted in the LCC^{ICCG} mutant (F243I/D238C/S283C/Y127G). The crystal structure of this mutant was recently elucidated

by Zeng et. al. in complex with MHET revealing the enzyme-substrate interaction network.⁵⁰

Next to the bacterial enzymes, PET hydrolases also exist in eukaryotes. Among them are *Thermomyces insolens* (formerly *Humicola insolens*), the fungus *Fusarium solani pisi,* and *Fusarium oxysporum*.^{51–53} *Hi*C, a cutinase from *T. insolens* with an optimal temperature of 70 °C⁵⁴, was successfully commercialized and optimized in terms of process engineering.^{52,55,56} Using low-crystallinity PET (7 % crystallinity) as a substrate, Ronkvist et. al. reported 97 % of degradation within 96 h at 70 °C, determined by weight loss measurements.⁵²

1.4.1. Improving the Reaction Performance of PET Hydrolases

Even though many enzymes were found to degrade PET, the degradation performance is mostly too inefficient for an industrial application. Hence, many strategies were developed to improve the enzymes themselves as well as the degradation process.³⁷

Improved thermostability of PET hydrolases is required to overcome the issue of crystallinity in enzymatic PET degradation. The degree of crystallinity of the thermoplastic can range from 2-40 % and is the result of uniformly packed crystalline regions in combination with randomly arranged amorphous regions.^{37,57} Enzymes preferentially hydrolyze the flexible amorphous regions of the polymer. The glass transition temperature (T_g) marks the temperature at which the amorphous parts of the polymer become flexible and therefore, better accessible for an enzymatic attack. For PET T_g lies in a range of 65-71 °C⁵⁸⁻⁶⁰ but can be influenced, at least on the surface, by solvents e.g., water which is used in most attempts of enzymatic degradation of PET. In water, T_g can be lowered by up to 16 °C.^{61,62} Nonetheless, a lot of research is focused on increasing enzyme stability since the optimal working temperature of most enzymes lies even below the reduced T_g of PET.^{35,47,52,63} In general, wildtype PET hydrolases often possess a low catalytic activity as well as low thermostability, which is why enzyme engineering is needed to improve the enzymes.⁶⁴

Furthermore, the adsorption and desorption of the PETase to the polymer as well as the complexation are being researched for efficient PET degradation. The enzyme activity largely depends on the enzyme-substrate interaction; however, the system of PET hydrolysis is heterogenic and hence, not ideal for enzymatic activity. While the PET polymer is mostly insoluble, the biocatalyst is soluble which prevents the enzyme from efficiently binding to the polymer in larger amounts.^{37,65} To promote the adsorption, natural

substrate-binding modules e.g., from cellulases are used as model systems to enhance the adsorption of the PET hydrolyzing enzyme to the polymer surface. The degradation performance of PETases could thus be increased by fusing cellulose-binding domains^{66– 68}, polyhydroxyalkanoate-binding modules^{67,} or chitin-binding modules⁶⁹ to the enzyme. Graham et. al. reported that CBMs can be beneficial for the degradation of PET with LCC if the solid loading is below 10 weight percent.⁷⁰

To improve the complexation of the enzyme and the substrate, information about the detailed mechanism of PET degradation with a biocatalyst are of utmost importance.⁷¹ In a recent study, various substrate-binding modes were identified in ligand-soaked PES-H1 and PES-H2 crystal structures.⁷¹ From these structures, several key residues involved in the binding of PES-H1 and PES-H2 to PET could be identified. Furthermore, the study revealed that substrate intermediates MHET and BHET bind too far from the catalytic triad for a nucleophilic attack supporting previous studies about product inhibition of PETases.⁷¹ Further studies using substrate homologs could elucidate the enzyme-substrate interaction network of LCC and its variants as well as *Is*PETase.^{44,50}

1.4.2. PET Oligo- and Monomer Degrading Enzymes

Methods for mitigating the product inhibition during enzymatic PET hydrolysis include the continuous removal of small-molecule products using ultrafiltration membranes,⁸ the use of engineered PETase variants that are less affected by the inhibitors,⁹ or the introduction of a helper enzyme with specific hydrolytic activity on the inhibitors. In nature, the degradation of recalcitrant polymers is often achieved by a synergistic enzyme system.³³ In the plastic-utilizing bacterium *I. sakaiensis* the issue of product inhibition was relieved by the helper enzyme MHETases.⁷² Also *in vitro* introduction of MHETase or other helper enzymes can decrease product inhibition and thus increase the yield of the monomeric products TPA and EG.^{33,72} Knott et. al. generated a chimeric enzyme from *Is*PETase and MHETase. The chimeric enzyme performed approximately four times better in comparison to *Is*PETase alone in the degradation of PET. Additionally, TPA was the sole degradation product in reactions with the chimeric enzyme whereas in reactions with only *Is*PETase approximately one-third of the reaction product was MHET.⁷³

Mrigwani et. al. reported a two-enzyme system with free enzyme using LCC as the polymer-degrading enzyme and a carboxylesterase from *Thermus thermophilus* (TTCE) as the oligomer hydrolyzing enzyme.⁷⁴ The high melting point of both enzymes allows for performance at 60 °C, which gives this system an advantage over the system proposed by Knott et al., which performed at 30 °C. Even though the two systems cannot be

compared easily due to different substrates and reaction conditions, it should be mentioned here that Knott et. al. reached a 400 % higher overall product outcome with TPA as the sole product using 550 nM of each enzyme.⁷³ Mrigwani et. al. increased the yield of TPA by 30-100 % when using the dual enzyme system in comparison to solely LCC and applied 2 μ M of each enzyme to the reaction. Despite the helper enzyme TTCE, small amounts of MHET were detected in the reaction.⁷⁴

Billig et. al.⁷⁵ first described the carboxylesterase TfCa, another PET oligomerdegrading enzyme, which originates from *T. fusca*. The enzyme was shown to function with a typical serine hydrolase mechanism and retained 37 % of its activity over 96 h at 50 °C.⁷⁵ Billig et. al. could furthermore show that the enzyme hydrolyzes cyclic PET trimers.⁷⁵ Immobilized TfCa was successfully deployed in a dual enzyme system together with LCC or TfCut2. The addition of the carboxylesterase to the reaction with LCC and TfCut2 led to a 91 % and 104 % increase in overall product outcome respectively. The immobilization via a sulfo-link resin made the enzyme more resistant to increased reaction temperatures of up to 60 °C.⁷⁶

1.5. Protein Engineering

As mentioned before, many of the discovered PET hydrolases and their helper enzymes for oligomer hydrolysis are lacking either activity, thermostability, or both to function efficiently for enzymatic PET recycling on an industrial scale.²⁸ Thus, protein engineering is used to modify proteins in order to improve the affinity for their substrate, turnover number, or stability at higher reaction temperatures and over longer reaction periods.^{77–79} Protein engineering is subdivided into two main strategies: directed evolution and rational design.⁸⁰ Depending on the information available the respective strategies can be more or less advantageous.⁸¹

Directed evolution deploys diversity and evolution to influence enzymatic behavior and has developed into a common laboratory tool.^{82,83} As a result, directed evolution not only aids in the evolution of new protein functions but also with the characterization and understanding of natural protein function and stability.^{84,85} The Darwinian cycle of mutation, selection, and amplification is employed with the gene of interest.^{83,86,87} For example, through error-prone polymerase chain reaction (PCR) or deoxyribonucleic acid (DNA) shuffling, random mutations are introduced into a target gene sequence, mimicking evolutionary processes.^{82,87} The *ex vivo* diversification results in a large gene library which is subsequently transformed into cells where proteins are expressed and undertaken a selection process. Importantly, in each of the iterative cycles, the stringency of the

selection is enhanced through competition or changing experimental conditions.⁸² Due to the vast size of the resulting library, well-established high-throughput screening (HTS) methods are essential for successful directed evolution. However, due to a lack of robust assays, HTS is also frequently limiting directed evolution.⁸⁸ HTS is mostly based on spectrophotometric or fluorometric assays which can be automated using a robotic screening platform.⁸⁹ For the degradation of PET, Bell et. al. used directed evolution to improve the thermostability of *Is*PETase. Starting from an *Is*PETase variant with a melting point of 56.8 °C, the authors yielded the HotPETase with a melting point of 82.5 °C by employing sequential rounds of saturation mutagenesis of the gene of interest and using ultra-high performance liquid chromatography (UHPLC) as the screening method.⁹⁰

In comparison to directed evolution, the rational design uses mechanistic and structural information as well as molecular modeling for a targeted alteration of the enzyme property. Targeted mutations result in significantly smaller enzyme libraries in comparison to directed evolution, opening possibilities for screening methods without high throughput.⁹¹ Recently, the development of an artificial intelligence system e.g., DeepMind Technologies' AlphaFold2 brought new opportunities for rational enzyme design. In experimental approaches, enzyme structures are commonly solved by X-ray crystallography, nuclear magnetic resonance (NMR) spectroscopy, or cryo-electron microscopy (cryo-EM).^{92–95} In contrast, AlphaFold2 can predict the enzyme's structure with atomic accuracy and within hours. The prediction is solely based on the amino acid sequence of the target protein.⁹⁶ Furthermore, computational methods and tools such as Rosetta which uses the atomic representation of protein structures and energy functions as models or molecular dynamics can be used to understand the structure-function relationship of enzymes.⁹⁷

Directed evolution and rational design methods, can also be employed together in a combined approach called semi-rational enzyme design. Here, the creation of small and smart libraries is of the essence. The reduced libraries allow for less screening effort and at the same time might overcome potentially false predictions from rational approaches. Site-saturation mutagenesis is often applied in semi-rational enzyme design, exchanging one amino acid of a predicted hotspot with all possible mutations at this position. Hence, the choice of the mutated position remains rational whereas the amino acid exchange becomes random as in the directed evolution approach.⁹⁸

1.6. Degradation of Polyvinyl Alcohol

PVA is a water-soluble synthetic vinyl polymer consisting of a carbon-carbon backbone with repeating 1,3-diol groups. Due to its versatile properties such as tensile strength, flexibility, and thermostability, PVA is used in many industrial applications e.g., fabric and paper sizing, fiber coating, films for packaging, and many more.⁹⁹ Its water solubility made the polymer furthermore an easy solution for water-dissolvable laundry and dishwasher detergent packaging. The polymer's low cytotoxicity¹⁰⁰ and the alleged biodegradability make the material also a widespread choice in biomedical¹⁰¹ and biomaterial¹⁰² research fields. In biomedical applications, PVA is used to form hydrogels by crosslinking the polymer chemically (e.g., boric acid or sulfosuccinic acid), physically (e.g. freeze-thaw cycles), or through radiation treatment.¹⁰³⁻¹⁰⁵ The hydrogels can subsequently be used for vascular grafts, wound dressings, drug delivery, and many more.^{101,106,107} Furthermore, PVA is deployed for immobilization e.g., as a carrier for enzymes or microbes.^{108,109}

The vinyl polymer is considered biodegradable and thus, a more sustainable alternative in comparison to other plastics. However, the requirements for microbial decomposition are highly specific and microorganisms for PVA degradation are not omnipresent.⁹⁹ Additionally, PVA is released in large quantities into the environment, making the polymer a major pollutant.¹¹⁰ A recent study by Rolsky and Kelkar revealed that over 70 % of PVA used as packaging for laundry and dish detergent pods ends up in the environment.¹¹⁰ The presence of the polymer in the environment, even though solubilized in water, can be tremendous due to the potential of mobilizing heavy metals and other hydrophilic contaminants.^{10,111,112} Furthermore, the polymer forms a foam that inhibits oxygen from being recovered in water and therefore, threatens marine life.³⁸

The printing and dyeing industries in particular are major PVA emitters. As a sizing agent, PVA is applied to act as a protective layer on the final product. Treatment of PVA wastewater with chemical or physical methods such as adsorption, filtration, ultrasonic degradation, and Fenton's reaction are cost intensive, less efficient, and can cause secondary pollution.¹¹³ Therefore, alternative and more sustainable approaches (e.g., with microorganisms or enzymes) are required for the remediation of wastewater contaminated by PVA.⁹⁹ Additionally, in comparison to conventional desizing methods, enzymatic PVA degradation can be carried out under mild conditions.¹¹⁴ Enzymes themselves are nontoxic, environmentally friendly, and have been used successfully in a variety of industrial processes for many years.

1.6.1. Microbial Degradation of Polyvinyl Alcohol

Microbial degradation of PVA was already described for bacterial strains such as *Pseudomonas putida* and *Spingomonas* sp. SA3 and SA2.^{115,116} The degradability of PVA is thereby dependent on factors such as the degree of polymerization, the tacticity of the main chain, and the degree of saponification.³⁸ The latter results from the process of manufacturing PVA which involves the hydrolysis of polyvinyl acetate. PVA can either be fully hydrolyzed with solely the 1,3-diol groups remaining on the C-C-backbone or it can be partially hydrolyzed, with individual acetate groups remaining in the polymer (**Figure 4**).⁹⁹ However, the acetylated PVA causes complications for the degradation of PVA since the microorganism also needs to express an enzyme for hydrolysis of the acetate group.

Shimao et. al.¹¹⁶ and Sakazawa et. al.¹¹⁵ already reported in the 1980s that the strain *Pseudomonas sp.* VM15C depends on a growth stimulant for effective PVA degradation. The unique stimulant was produced by another strain *Pseudomonas putida* VM15A in a symbiotic manner and was identified as PQQ.



Figure 4: Different structures of PVA resulting from the manufacturing process of PVA. PVA is yielded from either **A**) partially hydrolyzed or **B**) fully hydrolyzed polyvinyl acetate. In partially hydrolyzed PVA irregular repetitions of hydroxyl groups and acetate groups occur whereas fully hydrolyzed PVA solely consists of the repetition of 1,3-diols on the C-C-backbone.

Kim et. al.¹¹⁷ observed the same symbiotic behavior for the strains *Sphingomonas sp.* SA3 and SA2 with *Sphingomonas sp.* SA2 being the PQQ-producing strain.

However, PQQ-independent strains for PVA degradation were reported as well. *Pseudomonas vesicularis* var. *povalolyticus* PH can degrade PVA independently of PQQ but relies on thiamin as a growth factor as well as the amino acids tyrosine or phenylalanine, isoleucine and cystine for PVA degradation.¹¹⁸ Recently, Wu et. al. published the degradation of simulated PVA wastewater by mixed PVA-degrading bacterial strains using 1 g/L of the substrate.¹¹⁹ Higher concentration of substrate, however, led to a decrease of degradation by the mixed bacteria. The authors claim that PVA was degraded into ketones, fatty acids, and alcohols which were then further processed by microbes into carbon dioxide, hydrogen, and methane.¹¹⁹ These findings are in accordance with the observations from many other studies that led to the proposal of

microbial degradation of fully hydrolyzed PVA (**Figure 4 B**) by bacteria as a two-step process (**Figure 5**), i) the oxidation of one or two adjacent hydroxyl groups and ii) the subsequent cleavage of the resulting mono- or di-ketone structure. Step one is carried out by PVA oxidases or PQQ-dependent PVA dehydrogenases (PVA-DH) while an aldolase or a β -diketone hydrolase (BDH) catalyzes the second step.^{113,119–121}

Kawai and Hu¹¹³ hypothesized that the polymer is cleaved extracellularly by PVA oxidases which results in fragments small enough to enter the periplasmic space. They based their suggestion on two observations: I) PVA oxidases were found extracellularly whereas PVA-DHs were discovered membrane-bound or periplasmatic¹²² and II) oxidized PVA can be hydrolyzed by enzymes¹²³ but can also undergo spontaneous oxidation¹²¹. In the periplasm, the smaller PVA fragments are further oxidized by the PQQ-dependent PVA-DH. Aldolases or diketone hydrolases subsequently degrade the PVA further until it can be taken up by the organism through the inner membrane.¹¹³ However, some organisms express only PVA-DH and no PVA oxidases, which suggests that extracellular PVA degradation plays a secondary role.¹¹³



Figure 5: Proposed microbial degradation of PVA in the periplasm. After entering the bacterial periplasm through the outer membrane, PVA is firstly oxidized by the PQQ-dependent PVA-DH. Depending on the second step, oxidation needs to occur either on one or two adjacent hydroxyl groups. The ketone is subsequently cleaved by an aldolase whereas the di-ketone is cleaved by a BDH. The Figure was adapted and modified from Kawai and Hu.¹¹³

In summary, the current literature suggests that microbial degradation of PVA relies on highly specific organisms, growth factors, cofactors, and environmental conditions.^{115–} ^{117,119} Taken together with the vast amounts of PVA being released by the industry and from packaging, complete biodegradation of PVA is highly unlikely.

1.6.2. Enzymatic Degradation of Polyvinyl Alcohol

Although the microbial mechanism for PVA degradation has been known for a long time and some enzymes involved in PVA degradation were purified and characterized¹²⁴⁻¹²⁷, research has been scarce on the degradation of PVA with free enzymes. More recently, the crystal structure (PDB ID: 3WL6) of a hydrolase from *Sphingopyxis* sp. 113P3 and *Pseudomonas* sp. VM15C utilizing oxidized PVA was elucidated and the first enzyme engineering approaches were implemented.¹²⁴ Further investigations of the PVA-DH from *Sphingopyxis* sp. 113P3, the enzyme carrying out the first step of PVA degradation according to the proposed mechanism of Kawai et. al. (**Figure 5**), have failed because the recombinantly expressed enzyme formed largely insoluble inclusion bodies.¹²⁸ Wei et. al. investigated *Stenotrophomonas rhizophila* QL-P4 and were able to efficiently express a novel PQQ-independent PVA oxidase.¹²⁵ Nonetheless, current literature suggests that PQQ-dependent enzymes are needed for the complete degradation of PVA. Since PQQ is an expensive cofactor, this method is unattractive for industrial purposes.

2. Results & Discussion

2.1. Mechanism and Structural Insights into PET Degrading Enzymes

PET is one of the most investigated plastics when it comes to enzymatic degradation. In its heteroatomic backbone, the building blocks TPA and EG are connected by ester bond linkages making the polymer a suitable substrate for hydrolases. However, only a few hydrolases have been subject to a thorough characterization, and subsequent enzyme engineering. The degradation performances of PET hydrolases are still partly limited due to low thermostability, unbalanced enzyme-substrate interaction, low catalytic efficiency, and product inhibition. The following articles (**Article I** and **II**) provide an overview of the current benchmark PET hydrolases, their limitations, and the research of the scientific community on overcoming them.

Furthermore, we elucidated the crystal structure and the degradation mechanism of TfCa, a PET hydrolase helper enzyme. Using semi-rational enzyme design, we improved the activity of the enzyme and employed both, the wildtype and the improved variant, in a dual enzyme system for enhanced PET degradation.

2.1.1. Mechanism-Based Design of Efficient PET Hydrolases (Article I)

In a Perspective article, **Article I**, we analyzed the limitations of benchmark PET hydrolases for efficient industrial applications of enzymatic PET degradation. More precisely, we discussed the engineering of PET hydrolases towards higher thermostability as well as the de/adsorption properties of the enzymes and the release of product inhibition.

After Müller et. al. discovered *Tf*H, the first enzyme capable of hydrolyzing amorphous PET³⁹, scientific attention was soon drawn towards the material properties of PET including the glass transition temperature T_g and its importance for the enzymatic degradation of the polyester.^{52,129} It was found that for efficient enzymatic PET hydrolysis, the amorphous regions of the polymer need to transition from hard and brittle to a rubbery state.^{57,130} The T_g of PET is in the range of 65-71 °C but can be influenced by experimental factors.^{58–60} For instance water, a reactant, and solvent in enzymatic PET degradation has a plasticization effect on the polyester and can decrease its T_g by up to 16 °C.^{58,131,132} Additionally, Shinotsuka et. al. observed for PET films with different thicknesses that the T_g on the surface up to about 13 nm depth is significantly lower (approx. 48.1 °C).¹³³ Both effects taken together explain the comparably fast degradation of amorphous PET by

mesophilic enzymes such as *Is*PETase.²⁹ However, many studies showed that thermophilic and thermostable enzymes are more capable biocatalysts in comparison to mesophilic enzymes.^{47,52,134} Hence, enzyme engineering as well as process optimization were carried out to enhance the degradation performance (**Figure 6 A**). For instance, the optimal temperature of some bacterial PET hydrolases was increased by up to 10 °C in the presence of bivalent ions like Ca²⁺ or Mg²⁺.^{135,136} However, since Ca²⁺ reacts with terephthalate, one of the aromatic products from PET degradation, and forms insoluble byproducts, the Ca²⁺ binding site was substituted by a salt bridge or a putative disulfide bridge.^{35,47,137–140} Furthermore, varying the expression host resulted in an increased thermostability. For LCC the melting temperature (T_m) was increased by >4 °C or >12 °C, respectively, when it was expressed in *Bacillus subtilis* or *Pichia pastoris* (*P. pastoris*) in comparison to *Escherichia coli* (*E. coli*). In *P. pastoris* the large increase in T_m is due to glycosylation of the protein.^{141,142}

Protein engineering was performed for many PET hydrolases, increasing their T_m by stabilizing the enzyme. Over years of research, the T_m of an *Is*PETase variant (HotPETase) was increased by 42.5 °C in comparison to the wildtype enzyme.⁹ The BhrPETase, expressed in *B. subtilis* even reached a T_m of 101 °C.¹⁴² However, increasing the reaction temperature for enzymatic PET degradation from 65 to over 75 °C causes the polymer microstructure to transform from a less-ordered amorphous state to a nondegradable crystalline state.³⁵ Furthermore, at higher T_m the enzymatic degradation reaction has to compete against the physical aging of the polymer with increasing reaction temperature.¹⁴³ Hence, a higher T_m of enzymes is not always desirable.

Additionally, the stabilization of the enzyme and the subsequent thermostability often come with lower flexibility of catalytic regions and thus possibly impede the activity of the enzyme. Focusing on a thermo-active approach in protein engineering for an optimal reaction temperature of around 75 °C is therefore indispensable. **Figure 6 A** shows the progress made by enzyme and process engineering in the enhancement of the optimal temperature for benchmark PET hydrolases as well as their degradation performance.

In the Perspective article, we furthermore discussed the understanding of interfacial enzymatic PET hydrolysis from a structure-function perspective. Water, which acts as both the solvent and reactant, as well as the enzyme itself can only interact with the surface of the PET polymer. This limits accessible ester bonds and thus implies that the reaction occurs under enzyme-excess conditions.¹⁴⁴ PET degradation kinetics are therefore commonly calculated with the inverse Michaelis-Menten equation or the derivation of the Langmuir adsorption isotherm.^{33,52,145–150} The binding of PET hydrolases to the surface of

PET was investigated using biophysical methods such as quartz crystal microbalance^{67,151,152}, chemiluminescence⁶⁷, and fluorescence⁶⁹.

In nature, the binding of enzymes to polymers is promoted by binding modules. In PET hydrolysis binding modules such as the cellulose-binding domains (CBM) CenA from *Cellulomonas fimi*⁶⁶ and cellobiohydrolase I from *Trichoderma reesei*^{67,153} were fused to PET hydrolases which increased the degradation performance of the enzyme. The binding modules can be further optimized for PET binding. CBM's tryptophan residues were found to be mutational hotspots. Protein engineering of these hot spots resulted in an enhanced hydrogen bond formation with the PET substrate.^{66,68} Furthermore, binding of PET hydrolases to the substrate surface was shown to be improved by hydrophobins¹⁵⁴⁻¹⁵⁶, lytic polysaccharide monooxygenase (LPMO) derived from the white-rot fungus *Pycnoporus coccineus*¹⁵⁷ and a zwitterionic polymer (EKylation)¹⁵⁸. Hydrophobins are produced by filamentous fungi.¹⁵⁹ They are small amphiphilic proteins with a surfactant-like activity that can enhance the binding affinity of PET hydrolases to their substrate when applied as free molecules or pre-treatment for the degradation reaction. However, the hydrophobins were most effective when directly fused to the PET hydrolase.^{154–156}

So far, only a few co-crystallized PETase hydrolase structures were published in complex with a monomer which is why most investigations regarding enzyme-substrate interactions were performed using molecular docking.^{35,43,160-163} For bacterial PET hydrolases, the surface landscape in close vicinity to the active site is comparable. The favored angle of the substrate requires a high conformational selectivity.^{43,162,164} The highest activation free energy barrier for the catalytic reaction was determined using quantum mechanics/molecular mechanics (QM/MM) adiabatic mapping which suggested the nucleophilic attack as the rate-limiting step.^{165,166} **Chapter 1.4** describes the catalytic mechanism of hydrolases in detail. Figure 6 B depicts the schematical hydrolysis reaction with the activation free energy barriers for each step. The well-conserved residue W185 was found in IsPETase and many other PET hydrolases and is thought to be part of a dynamic catalytic site with aromatic subsites that are locally stabilized upon substrate binding.^{43,44,160,167} Substitution of this residue decreased the activity of the biocatalyst drastically.^{44,167} The steric hindrance of W185 within the active site is uniquely reduced in IsPETase due to two residues (S214 and I218) which allow higher flexibility of the indole side chain and thus a higher hydrolysis rate.¹⁶⁸ Further enhancement of the enzymatic activity of PET hydrolases was approached by widening the substrate binding pocket.^{150,169} Since the free energy barrier and hydrolytic reaction thermodynamics are similar in both the thermophilic LCC^{ICCG} and the mesophilic *Is*PETase¹⁶⁵, we concluded that the increase in activity is mostly due to better accessibility of the PET at elevated temperatures rather than to the fundamental interaction affinity. In further studies, it was also observed that an enzyme variant with a narrower substrate binding pocket in comparison to the wildtype enzyme can still exhibit increased activity.^{35,160,170} These findings suggest that polymer binding is a dynamic rather than static process.^{171,172} Thus, to gain a better understanding of the rate-limiting interactions of PET hydrolases it could be beneficial to systematically engineer all variable amino acids in the substrate binding pocket.



Figure 6: Identification and improvement of selected PET hydrolases over a course of 16 years and their reaction mechanism. A The normalized maximal conversion rates of *Is*PETase, TfH, HiC, and LCC as well as their mutants were calculated based on various publications^{29,35,47,49,52,63,143,173-175} and plotted on a logarithmic scale. The optimal temperature of each enzyme is shown in varying colors. The improvement of the degradation performance (dashed arrows) was gained by either enzyme or process engineering. B The hydrolysis reaction mechanism of PET hydrolases starts with the nucleophilic attack of the substrate by the catalytic serine. The tetrahedral intermediate one which is formed during this step is stabilized by the catalytic residues histidine and glutamate or aspartate as well as the oxyanion hole. Upon the collapse of intermediate one into an acyl-enzyme and an alcohol, the catalytic aspartate or glutamate as well as the histidine activate a water molecule that attacks the acyl-enzyme's carbonyl and thus forms a second tetrahedral intermediate. The subsequent diacylation of the second intermediate releases a carboxylic acid. The activation free energy barriers of each step are indicated in kcal/mol with the rate-limiting step marked in red. Values are summarized from different studies calculating the Boltzmann-weighted average from 20 QM/MM MD simulations (top number) or derived from adiabatic mapping studies (bottom number).^{165,166} The figure was adapted and modified from Wei et. al.176

However, varying experimental conditions such as pH, buffer, agitation speed and substrate material properties which have a major impact on the outcome of the enzymatic degradation performance are making it difficult to compare different studies, even when the same hydrolyzing enzyme was used.^{177–179} Additionally, under laboratory conditions post-consumer low-crystallinity PET packaging is often used as a substrate in various forms such as powder, foil, sheet, and others.^{180,181} In relevant industrial applications,

however, the substrate contains all crystallinity patterns. Furthermore, contaminants in the substrate impeding the enzymatic degradation have to be removed which is typically done by a washing step prior to thermomechanical processing followed by amorphization and micronization.^{35,182,183} Using such pre-treated PET in laboratory research would thus result in more reliable and comparable data for industrial applications.

2.1.2. Structural Insights into (Tere)phthalate-ester Hydrolysis by a Carboxylesterase and its Role in Promoting PET Depolymerization (Article II)

As mentioned in **Chapters 1.4.1.** and **2.1.1.**, one of the restrictions in enzymatic PET degradation is the product inhibition of selected PET hydrolases by the degradation intermediates MHET and BHET.^{34,71,72} Helper enzymes for PET hydrolases can be used to overcome this inhibition and thus expedite and improve the degradation performance as described in detail in **Chapter 1.4.2**. In **Article II** we elucidated the apo-structure of TfCa, a carboxylesterase from *T. fusca*. Additionally, we elucidated the crystal structure of TfCa in complex with PET monomers and a monomer analog and investigated the structure-function relationship between the enzyme and various *ortho*- and *para*-phthalate esters. Further, we conducted enzyme engineering in a semi-rational approach, resulting in a TfCa variant with 3.3-fold enhanced activity. Both the wildtype and the variant of TfCa were introduced to a dual enzyme system with a recently published *Is*PETase variant.⁴⁷

The carboxylesterase TfCa has been subject to research in PET degradation for over ten years.^{75,76,184} However, the crystal structure of the enzyme was never solved, making rational enzyme engineering of the hydrolase rely on homology models only. In this work, we elucidated the apo-structure of TfCa (PDB-ID: 7W1K, 1.40 Å) in collaboration with the groups of Prof. Dr. Weidong Liu at the Tianjin Institute of Industrial Biotechnology and the University of Chinese Academy of Sciences in Beijing, Prof. Dr. Manfred Weiss at the Helmholtz-Zentrum Berlin für Materialien und Energie GmbH, and Prof. Dr. Lammers at the Institute of Biochemistry. The apo-structure of TfCa folds has a canonical α/β hydrolase with a central antiparallel β -sheet surrounded by α -helices, a lid domain A, and a lid domain B (Figure 7 A). The strictly conserved catalytic triad consists of S185, E319, and H415. The ligand-soaked structures of TfCa with BHET (PDB-ID: 7W1L, 2.43 Å), MHET and BHET (PDB-ID: 7W1I, 1.67 Å) as well as MHETA (PDB-ID: 7W1J, 1.92 Å), a substrate analog for MHET, which were elucidated in the same collaboration, revealed a deep active site cleft containing the hydrophobic residues L282, L322, and V376. When the ligand-soaked structure of TfCa with MHETA is compared to the ligand-soaked structure of MHETase with MHETA (Figure 7), three hydrogen bonds (H-bonds) form with



the amide bond and the neighboring hydroxyl end of the substrate (**Figure 7 B**), whereas five H-bonds form with both ends of the ligand in MHETase (**Figure 7 D**).

Figure 7: Comparison of ligand-free and ligand-soaked structures of TfCa from *T. fusca* **and MHETase from** *I. sakaiensis.* **A** Elucidation of the crystal structure of TfCa revealed three subdomains: a hydrolase domain (TfCa^{Hyd}, brown), a lid domain A (TfCa^{LidA}, dark blue), and a lid domain B (TfCa^{LidB}, cyan). In **B** the active site of TfCa with bound MHETA (yellow) is shown (PDB-ID: 7W1J, 1.92 Å). Residues from different domains are depicted in brown (TfCa^{Hyd}), dark blue (TfCa^{LidA}), and cyan (TfCa^{LidB}). **C** The MHETase structure from *I. sakaiensis* contains two domains: the hydrolase domain (MHETase^{Hyd}, orange) and the lid domain (MHETase^{Lid}, dark aquamarine) (PDB-ID: 6QGA).⁷² In **D** the view of the active site of TfCa with bound MHETA in yellow is shown. Dark aquamarine (MHETase^{Hyd}) and orange (MHETase^{Hyd}) represent residues from various domains (MHETase^{Lid}). H-bond formation is indicated by dashed lines, and molecules and interacting residues are colored according to the kind of atom: oxygen is red, nitrogen is blue, and carbon is a variety of colors. Green sticks represent the catalytic triad residues. This figure was adapted from von Haugwitz et. al. 2022.¹⁸⁵

Using terephthalate-based oligo-esters of various lengths we determined the substrate profile of TfCa and suggested a degradation pathway for the longest substrate bis[2-(benzoyloxy)ethyl] terephthalate (3PET) which we determined from the high-performance liquid chromatography (HPLC)-derived product profile. Furthermore, we estimated the specific activity of TfCa for the various substrates (**Figure 8 A**). The highest specific activity of TfCa was calculated for the first hydrolytic step from BHET to MHET and EG. The second hydrolytic step of BHET (MHET into TPA and EG), however, is approximately 500 times slower compared to the first one. Interestingly, the specific activity of TfCa for the *ortho*-phthalate ester diethyl phthalate (DEP) is three times lower in comparison to BHET and only one hydrolysis step occurs, leaving monoethyl phthalate (MEP) as the product. Phthalic acid (PA), the product of the second hydrolysis step for DEP was not observed in

the reactions suggesting that MEP is a less preferred substrate for TfCa. Molecular docking revealed that MEP binds unproductively to the active site of TfCa (**Figure 8 B**). Overall, the estimated specific activities suggest diesters as the preferred substrates of the carboxylesterase.



Figure 8: Estimated specific activity of TfCa for terephthalate-based oligo-esters of various lengths and molecular docking results for TfCa with DEP and MEP. The specific activity for TfCa with the indicated substrates was calculated and is shown on a logarithmic scale. A shows the specific activity for the first hydrolysis of the respective substrate and **B** the specific activity of the second hydrolysis step which only occurs for the substrates BHET and 3PET. Error bars indicate the standard deviations calculated from at least three replicates. **C+D** show molecular docking results for TfCa with DEP (**C**) and MEP (**D**). One of the esters in DEP is in close proximity to the catalytic S185 and allows the cleavage into EG and MEP. The most favorable docking pose of MEP reveals that its only hydrolyzable ester bond is positioned too far from the oxyanion hole and the catalytic triad. Thus, MEP binds unproductively to the active site of TfCa. Residues from different enzyme domains are shown in brown (TfCa^{Hyd}), dark blue (TfCa^{LidA}), and cyan (TfCa^{LidB}). Ligands are shown as yellow sticks and the catalytic triad as green sticks. This figure was adapted and modified from von Haugwitz et. al. 2022.¹⁸⁵

Based on the elucidated structures of TfCa, semi-rational enzyme engineering was performed within the substrate binding pocket of TfCa. Amino acid residues within 5 Å of the soaked ligands were mutated to alanine (alanine scan) except alanine, glycine, proline residues, the catalytic triad, and the highly conserved GxSxG motif. Two variants exceeded the activity of the wildtype enzyme by over 1.2-fold while the mutation I69A resulted in a loss of function for the enzyme. Thereafter, site-saturation mutagenesis was performed with residue 69 and the variant TfCa^{I69W} was found to be over 2-fold more active in comparison to the wildtype enzyme. The three more active mutants were subsequently

combined in double and triple mutants leading to the most active mutant TfCa^{I69W/V376A} with a 3.3-fold increased activity which was titled TfCa WA and characterized regarding its optimal temperature and its activity in BHET and MHET hydrolysis. Furthermore, both, the wildtype of TfCa and the variant with increased activity were subjected to a dual enzyme system PET degradation using the for recently published IsPETase^{S121E/D186H/R280A/N233C/S282C} (IsPETase PM)⁴⁷ as the polymer degrading enzyme. Using different PET substrates (PET nanoparticles, PET powder, or PET film) we could show that the main product of *Is*PETase PM is MHET, independently of the substrate used. Adding either TfCa wildtype (TfCa wt) or TfCa WA to the reaction mixture resulted in TPA as the sole degradation product. With the substrates PET powder and PET film as well as with higher amounts of PET nanoparticles, the dual enzyme system generated an overall increased product yield. The best results with the dual enzyme system were gained using the variant TfCa WA for the hydrolysis of the intermediate products BHET and MHET. TPA yields were thus increased up to 14-fold in comparison to reactions containing solely IsPETase PM.

2.2. Synthesis of Modified Polyvinyl Alcohols and their Degradation Using an Enzymatic Cascade (Article III)

Compared to the heteroatomic polyester PET, polymers with a homoatomic backbone such as PVA raise another challenge for degradation by microbes and enzymes as specified in **Chapter 1.2**. PVA is a synthetic but water-soluble vinyl polymer containing a carbon-carbon backbone and repeating 1,3-diols. Despite its classification as biodegradable by microorganisms, the vast amount of PVA released into the environment causes pollution. Microbial degradation of PVA is slow and often relies on the expensive cofactor PQQ which makes it an inefficient process for the industry. In **Article III** we present a modified PVA with derivatized side chains that results in better properties for biodegradation. This section presents an enzymatic cascade, consisting of three enzymes that can degrade the modified PVA in four steps and the unmodified PVA in three steps in a one-pot reaction.

In collaboration with the group of Dr. Marcus Baumann from the School of Chemistry at the University College Dublin (Ireland), we used a simple ester-forming reaction introducing succinate groups to the hydroxyl groups of the polymer to alter the properties of PVA towards better biodegradability. Succinic anhydrate (SA) was chosen because of its renewable, non-toxic, and inexpensive characteristics. Different amounts of SA (2, 4, and 6 g per 30 g PVA) were explored and will be referred to as PVA-2 (2 g SA), PVA-4 (4 g SA), and PVA-6 (6 g SA). External testing revealed that critical metrics such as tensile strength and puncture can be efficiently altered in response to the amount of the utilized succinic anhydride. All modified PVA materials retained water solubility.

Furthermore, we developed an enzymatic cascade that can degrade the derivatized and unmodified PVA in a one-pot reaction (Figure 9). All steps are carried out by wellcharacterized enzymes^{186,187} which are either easily expressible in *E. coli* or commercially available. In the first step, the ester-bound modifications (acetylation and succinvlation) are hydrolyzed by the commercially available and immobilized lipase originating from Thermomyces lanuginosus (TL-IM) which utilizes water for the reaction. The resulting unmodified PVA with 1,3-repeating diols can be oxidized to ketones by an alcohol dehydrogenase from Lactobacillus kefir (LK-ADH) in step 2 using nicotinamide adenine dinucleotide phosphate (NADP⁺) as the cofactor and converting it into NADPH. NADPH is used in the next reaction step by cyclohexanone monooxygenase (CHMO) variant M15, originating from Acinetobacter calcoaceticus. CHMO M15 belongs to the class of BVMOs which catalyze the insertion of an oxygen atom between C-C bonds in ketones and aldehydes and thus introduces an ester bond into the polymer. The cofactor NADPH is converted into NADP⁺ by CHMO M15 which, in theory, results in an advantageous cofactor recycling within the enzymatic cascade. In the last step of the reaction, the ester bond is hydrolyzed by TL-IM which produces smaller PVA fragments.



Figure 9: Reaction scheme of the proposed enzymatic cascade for the degradation of PVA. The ester bonds of PVA modifications, namely acetylation and succinylation, are cleaved by the lipase TL-IM. The enzymatic reaction utilizes water and results in unmodified PVA. Next, LK-ADH oxidizes one or more of the 1,3 repeating hydroxyl groups on PVA into ketones using NADP⁺ as a cofactor. During the reaction, LK-ADH converts NADP⁺ into NADPH. The BVMO CHMO M15 implements an ester bond while utilizing NADPH and converting it into NADP⁺. Finally, in step 4 the newly introduced ester bond is cleaved by the same lipase that performed step 1 resulting in a carboxylic acid and an alcohol. This figure was adapted from von Haugwitz et. al. 2022.¹⁸⁸

The reaction of the enzyme cascade was investigated using the Finley method. Finley reported that PVA forms a green complex with iodide in the presence of boric acid¹⁸⁹ which can be spectrophotometrically detected at 500 nm. The degradation of film PVA-4 was investigated regarding the effects of reaction temperature, buffer pH, initial NADP⁺ amount, enzyme stability, and LK-ADH to CHMO ratio (**Figure 10**).



Figure 10: Analyzing the impact of different reaction conditions on PVA-4 degradation. The degradation of PVA-4 was investigated regarding temperature, pH, reaction time, amount of cofactor, and ADH to CHMO ratio. pH 8.5, 20 °C, 4 mM of NADP⁺, and a ratio of 1:1 or 2:1 of ADH to CHMO were shown to be the ideal reaction conditions in the range tested. Using the model substrates (*R*)-1-phenyl ethanol (LK-ADH) and cyclohexanone (CHMO M15), the stability of the indicated enzymes was investigated over 24 h by following NADP/H decrease or increase. One unit was defined as the amount of substrate converted by 1 µL enzyme lysate per minute. Error bars originate from the standard deviation of at least three replicates. This figure was adapted and modified from von Haugwitz et. al. 2022.¹⁸⁸

Firstly, we investigated the optimal temperature for single enzymes by incubating them for one hour at a temperature range of 4 to 50 °C and subsequently determining the residual activity using model substrates. LK-ADH and CHMO M15 were found to be less stable than TL-IM which is in agreement with the manufacturer's information regarding the

lipase. Step 2 and step 3 of the enzymatic cascade reaction were thus considered the crucial steps of the reaction.

With the Finley method, the optimal settings for the enzymatic cascade were found to be pH 8.5, 20 °C, and 4 mM NADP⁺ out of the range of parameters evaluated. The optimal enzyme ratio of LK-ADH to CHMO M15 is important for sufficient cofactor recycling. The ratios 2:1 and 1:1 were observed with equal efficiency and thus, in the subsequent gel permeation chromatography (GPC) measurements both ratios were further investigated.

GPC measurements were performed with PVA-2, PVA-4, PVA-6, and unmodified PVA using the optimized reaction conditions for PVA-4. The number average molecular weight (M_n), the weight average molecular weight (M_w), and the polydispersity index (PDI) were determined from the GPC measurements. In all measurements taken, the PDI increased when PVA was treated with the enzyme cascade in comparison to untreated PVA. The increase in PDI indicates a broader distribution of molecular weight in the sample and hence, indicates degradation of the PVA film by the enzyme cascade. For PVA-4, independently of the enzyme ratio of ADH to CHMO, M_n decreased by 10 %, confirming the results gained with the Finley method that the enzyme ratio does not significantly impact the reaction. However, it should be noted that the amount of cofactor and the enzyme ratio are most likely interdependent, and the GPC analysis was only performed with 4 mM NADP⁺.

With film PVA-4, the largest decrease in M_n (10 %) was observed, independently of the LK-ADH to CHMO ratio. However, the largest reduction in M_w was measured for unmodified PVA. When using a 2:1 LK-ADH to CHMO ratio, M_w decreased by 10 % for unmodified PVA and 7 % for PVA-4. In general, the proportional decrease of M_w was lower in comparison to M_n in most cases except for unmodified PVA film. After enzymatic treatment with an enzyme ratio of 2:1, M_w was reduced by 10 % and M_n by 9 %. With an enzyme ratio of 1:1 M_w was reduced by 4 % and M_n by 7 %. These findings indicate that the enzyme ratio of LK-ADH to CHMO M15 has a higher impact on PVA without modification in comparison to modified PVA.

LK-ADH has been shown to accept a wide range of substrates, including those with bulky side chains.¹⁹⁰ Nevertheless, the polymer is likely a difficult substrate for the biocatalyst. An increase in the enzyme's concentration may aid in the degradation of larger molecules. Further increasing the rate of PVA breakdown may be possible by genetically modifying the enzyme LK-ADH to accept larger side chains.

3. Conclusion

Enzymatic PET degradation has evolved impressively in the past 17 years since the first PET hydrolase was discovered. A lot of research was conducted, using protein or process engineering to make enzymatic PET degradation more and increasingly efficient. Many limitations of the natural enzymes such as low stability, low activity, low substrate binding affinity, and product inhibition are already being addressed in multiple studies. These limitations were summarized and discussed in Article I, giving an overview of methods employed to overcome these challenges. However, varying experimental conditions have a major impact on the outcome of the enzymatic degradation performance.^{177–179} Additionally, in relevant industrial applications the substrate is likely to contain contaminants that can impede the enzymatic degradation and must be removed prior to the reaction. Using such pre-treated PET in laboratory research and comparable reaction conditions would therefore result in more reliable data with industrial relevance. In Article II we addressed one of the above-mentioned limitations in PET degradation, substrate inhibition, which was reported for several PET hydrolases. Using the carboxylesterase TfCa we performed a dual enzyme reaction using a recently published variant of IsPETase. We elucidated the enzymes' structure and employed enzyme engineering to create a more active mutant. TfCa WA was 3.3-fold more active and increased the TPA yield in the dual enzyme system up to 14-fold with various PET substrates in comparison to solely the PET hydrolase.

In addition to PET, researchers are also interested in degrading other synthetic polymers. Among them is PVA, a polymer that was claimed to be degradable by microorganisms. However, microbial biodegradation occurs at a small scale which is not sufficient for the PVA amounts being released into the environment. In **Article III** we studied PVA degradation using an enzymatic cascade in a one-pot reaction. So far, most enzymes that were characterized and performed PVA degradation are PQQ-dependent. The herein-reported conceptionally new enzymatic cascade is PQQ-independent and contains an advantageous cofactor recycling system. All enzymes used in the cascade are either easily expressible in *E. coli* or commercially available. The cascade can degrade PVA with derivatized side chains in four steps and unmodified PVA in three steps.

In summary, in this work, enzymatic plastic degradation was performed using PET and PVA as the substrates. The structure-function relationship of TfCa was investigated by comparing its hydrolytic activity on various *ortho*-and *para*-phthalate esters of different lengths and the enzymatic activity improved using semi-rational enzyme engineering.

Lastly, an enzymatic cascade was shown to degrade unmodified PVA in a three- and the modified PVA in a four-step reaction.
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5. Author Contributions

Article I Mechanism-Based Design of Efficient PET Hydrolases R. Wei, <u>G. von Haugwitz</u>, L. Pfaff, J. Mican, C. P. S. Badenhorst, W. Liu, G. Weber, H. P. Austin, D. Bednar, J. Damborsky, U. T. Bornscheuer, *ACS Catal.*, **2022**, *12*, 3382–3396.

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Article II Structural Insights into (Tere)phthalate-ester Hydrolysis by a Carboxylesterase and its Role in Promoting PET Depolymerization G. von Haugwitz, X. Han, L. Pfaff, Q. Li, H. Wei, J. Gao, K. Methling, Y. Ao, Y. Brack, J. Mican, C. G. Feiler, M. S. Weiss, D. Bednar, G. J. Palm, M. Lalk, M. Lammers, J. Damborsky, G. Weber, W. Liu, U. T. Bornscheuer, R. Wei, ACS Catal., 2022, accepted.

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an Enzymatic Cascade
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M. Baumann, U. T. Bornscheuer, Angew. Chem. Int. Ed., under review.

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Articles

Article I



Mechanism-Based Design of Efficient PET Hydrolases

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ABSTRACT: Polyethylene terephthalate (PET) is the most widespread synthetic polyester, having been utilized in textile fibers and packaging materials for beverages and food, contributing considerably to the global solid waste stream and environmental plastic pollution. While enzymatic PET recycling and upcycling have recently emerged as viable disposal methods for a circular plastic economy, only a handful of benchmark enzymes have been thoroughly described and subjected to protein engineering for improved properties over the last 16 years. By analyzing the specific material properties of PET and the reaction mechanisms in the context of interfacial biocatalysis, this Perspective identifies



several limitations in current enzymatic PET degradation approaches. Unbalanced enzyme-substrate interactions, limited thermostability, and low catalytic efficiency at elevated reaction temperatures, and inhibition caused by oligomeric degradation intermediates still hamper industrial applications that require high catalytic efficiency. To overcome these limitations, successful protein engineering studies using innovative experimental and computational approaches have been published extensively in recent years in this thriving research field and are summarized and discussed in detail here. The acquired knowledge and experience will be applied in the near future to address plastic waste contributed by other mass-produced polymer types (e.g., polyamides and polyurethanes) that should also be properly disposed by biotechnological approaches.

KEYWORDS: Hydrolase, enzymatic degradation, interfacial biocatalysis, plastic recycling, protein engineering, polyethylene terephthalate (PET), product inhibition, thermostability

1. INTRODUCTION

Scientists began to study biological degradation of plastic waste in the early 1970s.¹ Around the same time, the distribution of plastic waste in the Pacific Ocean was first quantified.² After nearly 50 years, climate change and environmental pollution caused by mass production, mass consumption, and improper end-of-life management of petroleum-based plastic products have become unprecedented challenges for human society.^{3–5} Consciousness of these issues spreading among governments and policymakers, industries producing or relying on plastics, and end-users of plastic products, has recently boosted research and development of novel plastic replacement materials and waste plastic valorization strategies to enable a transition from a linear to a circular plastic economy.^{6–9}

To this end, biotechnological plastic recycling has become a thriving research area in recent years.^{6,9,10} The biodegradation of hydrophobic vinyl polymers, such as polyolefins and polystyrene, which represent over 80% of all conventional plastics produced,¹¹ is still an intensively debated topic.^{9,12,13} In contrast, the biocatalytic degradation of polyester-type plastics, such as polyethylene terephthalate (PET), has evolved in the last two decades from verifying trace amounts of released monomers after weeks of incubation to highly efficient

depolymerization within several hours.^{14–17} PET is a heteroatomic polymer consisting of terephthalic acid (TPA) and ethylene glycol (EG) connected by ester bonds. It is a semicrystalline thermoplastic composed of crystalline regions with uniformly packed molecules and amorphous regions with randomly arranged microstructures.¹⁸ With a first patent filed for its synthesis in 1941 and commercialization starting in the early 1950s,¹⁹ particularly as synthetic polyester fabric for the textile industry and as packaging materials for food and beverages,^{20,21} PET has become one of the most important mass-produced petrochemical plastics.²² The majority of PET products have a high crystalline fraction (usually 30–40% crystallinity)^{23,24} benefiting their durability against mechanical and chemical stress.²⁵ Post-consumer PET accounts for a considerable fraction of the global solid waste stream, and its

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Figure 1. Selected milestones of a 16-year-long history of identifying and engineering PET hydrolases. Both optimal reaction temperatures (in varying colors) for PET degradation and normalized maximal conversion rates (diamonds corresponding to logarithmic values on the vertical axis) calculated based on various publications are denoted, regardless of the material properties of applied PET substrates. The successes in raising the degradation performance using certain benchmark enzymes by both protein and process engineering are indicated by arrows with broken lines. *Tf*H: hydrolase from *T. fusca* DSM43793;³¹ *HiC: Humicola insolens* cutinase;⁴² LCC: leaf-branch compost cutinase;^{33,52} *IsPETase: I. sakaiensis* PET hydrolase;^{16,34} *Tf*Cut2: *T. fusca* KW3 cutinase;⁵³ LCC^{ICCG}: LCC variant with indicated quadruple substitutions;¹⁶ DuraPETase, ThermoPETase, etc.: various thermostabilized *IsPETase* variants.

breakdown is a source of microplastics and microfibers that further pollute the environment. $^{11,26-28}$

Tokiwa et al. suggested in the 1970s that aromatic polymers are resistant to enzymatic and microbial attack.²⁹ Later research found, however, that crude enzyme preparations from specific fungal species can induce surface modifications on high-crystallinity PET materials.³⁰ The first breakthrough was achieved with the cutinase TfH (from the filamentous actinomycete Thermobifida fusca) which caused >50% weight loss of melt-quenched post-consumer PET bottles (10% crystallinity) following 3 weeks of incubation.³¹ During 16 years of extensive research, the initial low PET degradation activity of T. fusca PET hydrolase has been considerably enhanced by more than an order of magnitude (Figure 1) as a result of both protein and process engineering.³² The development of metagenomic approaches has allowed for the identification of a more active leaf-branch-compost cutinase LCC_{1}^{33} which has emerged as the most promising benchmark thermophilic PET hydrolase. In 2020, Nature published a breakthrough article on engineered LCC variants which can rapidly depolymerize amorphized (i.e., by lowering the crystallinity through a thermomechanical process to allow for enzymatic degradation) PET waste at an industrially relevant scale within 10 h, and the recovered monomers were readily used to synthesize virgin polymers, thereby closing the recycling loop.¹⁶ IsPETase and the related monoester-hydrolyzing IsMHETase, both derived from the bacterium Ideonella sakaiensis, which was isolated from plastic-contaminated sediment samples, have also been intensively studied.^{34,35} The uniqueness of this bacterium in degrading and metabolizing highly amorphous PET led not only to the discovery of a tandem polymer degradation pattern by two distinct enzyme classes,³⁶ but also to its utility in the efficient bio-upcycling of PET waste to other useful biopolymers when it was applied as a whole cell-based catalyst.³

Based on >65 crystal structures so far elucidated,³⁸ these bacterial PET hydrolases exhibit conserved structural properties and can be classified into a single subclass of the α/β hydrolase fold enzyme superfamily as represented by the first solved *Streptomyces exfoliates* lipase structure (PDB ID: 1JFR).^{39,40} This subclass is distinct from the polyesterhydrolyzing fungal cutinases (EC 3.1.1.74) with shorter polypeptides and more compact structures.⁴¹ Thermomyces insolens (formerly named Humicola insolens) cutinase HiC is a prominent member of the fungal PET hydrolase family. It has been successfully commercialized and also received broad attention in recent years by researchers working on PET waste degradation. However, here the emphasis was more on process engineering and improvement rather than protein engineering.⁴²⁻⁴⁵

This Perspective intends to provide a deeper understanding of important obstacles in the engineering of effective industrially applicable PET hydrolases, as well as to provide guidance for further efforts in this intriguing research field. Previous research has indicated that enzymatic polyester hydrolysis occurs preferentially in its amorphous parts rather than the well-ordered crystalline regions with poor chain mobility.⁴⁶ Understanding the accessibility of amorphous polymer chains around the polymer glass transition temperature, in conjunction with tailoring the thermostability of biocatalysts, has thus become a focus of contemporary research.^{38,47} As a typical surface erosion process, it is not yet fully understood how the adsorption and desorption of biocatalysts onto the polymer surface influence the overall degradation kinetics and performance. This problem is reminiscent of the decades spent investigating the relationship between the binding of cellulases onto crystalline cellulose and catalytic activity.⁴⁸ Altering their affinity to polymer substrates by protein engineering, on the other hand, has proven to be a viable approach to maximize the catalytic capacity of both cellulose and PET depolymerases. Similar to the aforementioned natural polymer-degrading enzymes such as cellulases, mass transfer of certain degradation intermediates that can function as inhibitors of the biocatalysts, has been identified as the third main bottleneck that must be addressed with a lowcost solution for adequate reaction efficiency.⁴⁹⁻⁵¹ This Perspective summarizes and discusses special efforts devoted to the engineering of thermostability (Section 2), to study the de/adsorption properties, and to address the product inhibition (Sections 3 and 4).



Figure 2. Frequently reported mutation hot spots illustrated on the superposed crystal structures of known bacterial PET hydrolases. Backbones shown in the cartoon are derived from the structural superposition with selected homologous enzymes. The catalytic triad (S160, D206, and H237) as well as two aromatic residues (W159 and W185) are involved in the interaction with the monomer analogue 1-(2-hydroxyethyl)-4-methyl terephthalate (HEMT) (A, B) based on the *Is*PETase structure (PDB ID: SXH3; the numbering of residues is modified consistently with other structures solved later for easy comprehension). (A) One frequently reported mutation hotspot equivalent to S209 (B) in *Is*PETase can adopt various residues which might influence the widths of the binding pocket: 65,90 F found in 4CG1, 4EB0, and 7OSB and also conserved in many other PET hydrolase; S found in the *Is*PETase structure SXH3; I found in an LCC mutant 6THT; L found in another PET hydrolase 7CUV. (C) One of the putative Ca²⁺ binding sites revealed by cocrystallized structures such as 4WFJ, SLUL, and SZNO can be replaced by a disulfide bridge (6THT, 7CTS, and 7CTR) to thermostabilize several PET hydrolases.

2. DESIGN OF THERMOSTABLE PET HYDROLASES BASED ON MATERIAL PROPERTIES

Earlier research on enzymatic degradation of aromatic and aliphatic copolyesters suggested that increasing the proportion of aromatic moieties raises the melting point, thus lowering the polymer chain mobility and biodegradability at the optimal reaction temperatures of the applied hydrolases.^{57,58} For a long time, enzymatic depolymerization of PET with a melting point over 260 °C was thought to be unachievable according to this idea, until, in 2005, Müller et al. showed significant weight loss of amorphized PET waste using TfH.³¹ This discovery drew attention to the preferential (or perhaps exclusive) degradation of amorphous PET, as well as the importance of its glass transition temperature (T_g) in understanding enzymatic degradation.^{42,46} T_g is the temperature range in which the glass transition process occurs, i.e., the amorphous polymer structure transitions from a "glassy" (hard and brittle) state into a sticky-liquid or rubbery one as a function of increasing temperature.^{18,59} The T_g of bulk amorphous PET is in the range of 65-71 °C, estimated based on data collected with differential scanning calorimetry (DSC) at zero heating rate.⁶⁰⁻⁶² This has so far been accepted as a standard value by research communities working on enzymatic PET hydrolysis.^{31,42,53,63-65} In addition to its role as both a solvent and a reactant in enzymatic PET degradation, water has a plasticization effect on the PET polymer, as reported since the early 1980s, 66,67 by lowering the T_g of bulk polymer by up to 16 °C. 60,68,69 This influence is more pronounced on the surface polymer layer of about 13 nm which has an intrinsically lower T_{σ} (~48.1 °C) than that of the bulk polymer even when water

is not present.⁷⁰ With both effects taken into account, the superficial PET layer exposed to enzymatic degradation in an aqueous milieu can indeed have a biocatalysis-relevant $T_{\rm g} \lesssim 40$ °C, explaining the considerably fast degradation of amorphous PET by, for example, *I. sakaiensis* and its *Is*PETase at ambient temperature.³⁴ The enhanced segmental mobility of the surface polymer, on the other hand, may decrease to a level similar to that of the bulk polymer as a result of superficial crystallization.⁷¹ For example, as a result of UV-treatment-induced crystallization, the overall degradation performance could be significantly impaired.⁷²

Based on these PET material characteristics, the advantage of using thermophilic and thermostable enzymes in depolymerization, over their mesophilic counterparts, is obvious and evident from preliminary studies.^{42,56,73,74} In this regard, searching for new thermophilic enzymes, such as those found in metagenomic libraries,^{33,75} as well as known thermostabilizing ones, provides viable options for improving degradation performance.⁷⁴ In the presence of selected bivalent ions such as Ca^{2+} or Mg^{2+} , the overall thermostability of many bacterial PET hydrolases has been improved, as indicated by increased midpoints of thermal denaturation (T_m) by 10–16 °C and enhanced optimal temperatures (T_{opt}) for PET degradation by at least 10 °C.^{52,76–78} The probable Ca^{2+} binding site was found to be close to the catalytic triad based on cocrystallized structures (Figure 2) and molecular dynamics simulations.^{76–81} The interaction with Ca^{2+} controls the process of opening and closing the active site during substrate binding and unbinding by Cut190 from *Saccharomonospora viridis.*^{78,80} Because Ca^{2+} will precipitate terephthalate to generate insoluble byproducts from the reaction super-

Table 1. Selected IsPETase Engineering Studies Designed to Improve Thermal Stability

nomenclature and introduced mutations	improved stability ^a	design approach and interpretation	refs
\$238F/W159H	$T_{\rm m}$ = 56.5 °C, $\Delta T_{\rm m}$ = +9.7 °C	Structural and sequence comparison with homologous PET hydrolases	65,90
ThermoPETase: S121E/D186H/R280A	$T_{\rm m}$ = 57.6 °C, $\Delta T_{\rm m}$ = +8.8 °C	Structure-based design; Water-mediated hydrogen bond between E121 and H186	54
DuraPETase: A214H/I168R/W159H/S188Q/R280A/A180I/G165A/ Q119Y/L17F/T140D	$T_{\rm m} = 77.0 \ ^{\circ}{\rm C},$ $\Delta T_{\rm m} = +31.0 \ ^{\circ}{\rm C}$	Structure-based design and machine learning approach; Multiple stabilizing interactions	55
W159H/F229Y	$\Delta T_{\rm m}$ = +10.4 °C	Sequence comparison with other homologous PET hydrolases	91
DuraPETase+N233K	$T_{\rm m} = 83.5 \ ^{\circ}{\rm C},$ $\Delta T_{\rm m} = +38.4 \ ^{\circ}{\rm C}$	Machine learning; Introduction of salt bridge between K233 and E204	88
FAST-PETase: ThermoPETase+R224Q/N233K	$T_{\rm m}$ = 67.4 °C, $\Delta T_{\rm m}$ = +22.3 °C	Machine learning; Introduction of a hydrogen bond between Q224 and S192	88
TS-PETase: ThermoPETase+N233C/S282C	$T_{\rm m} = 69.4 ^{\circ}{\rm C},$ $\Delta T_{\rm m} = +22.3 ^{\circ}{\rm C}$	Structural comparison with other homologous PET hydrolases	83
TM3: ThermoPETase+K95N/F2011/N233C/S282C	$T_{\rm m} = 70.8 \ ^{\circ}{\rm C}$, $\Delta T_{\rm m} = +25.8 \ ^{\circ}{\rm C}$	Random mutagenesis based on error prone PCR and structural comparison with $\mathrm{LCC}^{\mathrm{ICCG}}$ mutant	56
D1: DuraPETase+N233C/S282C	$T_{\rm m} = 81.1 \ {}^{\circ}\text{C},$ $\Delta T_{\rm m} = +36.1 \ {}^{\circ}\text{C}$	Structural comparison with $\mbox{LCC}^{\mbox{ICCG}}$ mutant	56
HotPETase: TS-PETase+P181V/S207R/S214Y/Q119K/S213E/R90T/ Q182M/N212K/R224L/S58A/S61V/K95N/M154G/N241C/K252M/ T270Q	$T_{\rm m}$ = 82.5 °C, $\Delta T_{\rm m}$ = +37.5 °C	Directed evolution	89

 ${}^{a}\Delta T_{\rm m}$ was estimated compared to $T_{\rm m}$ of the wild-type *Is*PETase either determined in the same publication or that of 45.1 °C determined by Brott et al. ⁵⁶ $T_{\rm m}$ values were determined by circular dichroism, differential scanning calorimetry, or differential scanning fluorimetry.

natants,⁸² relying on Ca²⁺ salts for high degradation efficiency is undesirable and can be minimized by tailoring the Ca²⁺binding sites of the biocatalysts. Earlier research was carried out by substituting one major Ca²⁺-binding site with a salt bridge or a putative disulfide bond, resulting in an increased T_m of the *T. fusca* cutinase *Tf* Cut2 by up to 25 °C.^{77,79} The latter strategy was then adopted in engineering other homologous PET hydrolases, resulting in increased T_m by up to 26 °C,^{16,56,81,83} although the formation of this disulfide bond was indeed validated by protein crystallography for only two enzymes.^{16,81} More recently, Nakamura et al. have also introduced cysteine pairs to form putative disulfide bonds at alternative positions in the homologous hydrolase PET2, but this led only to a marginal increase of T_m by less than 3.1 °C.⁸⁴

Enhanced thermostability of PET hydrolases has also been reported when they were recombinantly expressed in alternative hosts other than *Escherichia coli*, for example, *Bacillus subtilis*^{53,85} or *Pichia pastoris*.⁸⁶ Compared to the wild-type LCC obtained from *E. coli*, an increased $T_{\rm m}$ of >4 °C or >12 °C has been described when it was expressed in *B. subtilis* or *P. pastoris*, respectively.^{85,86} The remarkable improvement with the latter host was attributed to glycosylation which mitigated the enzyme thermal aggregation at high reaction temperatures.⁸⁶

Despite the fact that *Is*PETase is distinguished by its high PET hydrolyzing activity at ambient temperature, an effect which is presumably due to its more flexible and open substrate binding cleft,⁸⁷ efforts to thermostabilize this enzyme have been widely reported recently, with the goal of outperforming other cutinase-like PET hydrolases also at higher temperature ranges (Table 1). A ThermoPETase mutant with three residue substitutions, generated based on a structure-based engineering strategy, exhibited an increased T_m by 8.8 °C and up to 14-fold improved PET hydrolyzing activity compared to the wild-type *Is*PETase at 40 °C.⁵⁴ DuraPETase is an *Is*PETase variant with ten mutated residues, discovered by a novel GRAPE (greedy accumulated strategy for protein engineering) computational method.⁵⁵ Compared to wild-type *Is*PETase, DuraPETase showed a T_m increase of 31 °C and over 300-fold higher hydrolytic activity against highcrystallinity PET powder. By applying a convolutional neural network, MutCompute, trained for stability optimization, Lu et al. reported in a recent preprint the most thermostable IsPETase variant based on a single N233K substitution in addition to the DuraPETase, resulting in a T_m of 83.5 °C.⁸⁸ FAST-PETase, the most promising variant based on additional mutations of ThermoPETase, demonstrated significantly improved PET degradation activity against low-crystallinity PET waste at 50 °C compared to the wild-type and other known mutants of IsPETase. By screening a randomized IsPETase library based on error-prone PCR, at least one of their computationally targeted stability-related hot spots was also discovered.⁵⁶ Further substitutions related to thermostabilizing IsPETase found by other protein engineering strategies have been reported to be distributed across the entire sequence (Table 1). In another recent preprint, >13,000 IsPETase variants were evaluated by applying catalytic activity at elevated temperatures as a primary selection pressure. This directed evolution procedure afforded a HotPETase variant with 21 mutations compared to wild-type IsPETase and a T_m of 82.5 °C.89 Therefore, the thermostability of IsPETase and other homologous enzymes depends on the interplay of many effects, necessitating further comprehensive research.

By raising the reaction temperature from 65 to 75 °C, the transition of the polymer microstructure from a less-ordered amorphous state to a nondegradable crystalline state can occur significantly earlier and faster.¹⁶ This "physical aging" reaction competes with the enzymatic depolymerization and thus becomes the main determining factor of the total achievable degradation level.⁵³ As a result, using biocatalysts with only very high thermostability, such as the BhrPETase with a $T_{\rm m}$ of 101 °C,⁸⁵ is not always a good way to improve the degradation performance. As thermostabilizing an enzyme usually comes at the expense of lowering the flexibility of certain catalysis-relevant structural segments, a more balanced protein engineering strategy focusing on a thermo-active biocatalyst with $T_{\rm opt}$ at 75 °C and sufficient long-term robustness will hold promise for industrial applications. A recent techno-economic



Figure 3. Interfacial biocatalytic hydrolysis of PET and its reaction mechanism. The states of a PET hydrolase are schematically illustrated in the upper right panel. In the lower panel, individual steps of the hydrolysis reaction are schematically shown in line with their activation free-energy barriers in kcal·mol⁻¹ summarized based on different studies.^{107,108} The reaction is initiated by a nucleophilic attack by a catalytic serine resulting in a tetrahedral intermediate stabilized by a catalytic histidine, an aspartic acid, and the oxyanion hole, followed by breakdown of the tetrahedral intermediate 1 into an acyl—enzyme intermediate and release of an alcohol. The aspartate—histidine pair activates the water for attack on the acyl—enzyme intermediate carbonyl, resulting in the formation of the second tetrahedral intermediate. The deacylation of this tetrahedral intermediate releases the carboxylic acid product. The rate-limiting step is regarded as the initial nucleophilic attack and highlighted in red with two free-energy activation barriers denoted. The top number is the Boltzmann-weighted average from 20 QM/MM MD simulations,¹⁰⁸ and the bottom number comes from adiabatic mapping studies.¹⁰⁷

analysis of a simulated enzymatic PET recycling process revealed that the reaction duration and enzyme price have a greater influence on process costs than the energy cost to maintain an operating temperature of up to 80 °C.⁹² Therefore, a commercially viable biocatalytic PET degradation process will rely on highly efficient enzymes rather than more heat-stable ones, which have, for example, $T_{\rm opt}$ in a higher temperature range but are less active at 75 °C.

3. UNDERSTANDING INTERFACIAL ENZYMATIC PET HYDROLYSIS FROM A STRUCTURE-FUNCTION PERSPECTIVE

Enzymatic PET hydrolysis is a surface erosion process characterized by the primary degradation of the exterior polymer to expose the inside of the material.^{42,46,93} Because neither water (as both a solvent and a reactant) nor the biocatalysts can permeate the inner core of the polymer, only a limited number of superficial ester bonds can be accessed, implying that the reaction occurs primarily under conditions using an excess of enzyme.⁹⁴ As a consequence of this, research on PET hydrolysis kinetics has commonly employed an inverse Michaelis–Menten equation^{90,95,96} or its mathematically equivalent expression based on the derivation of the Langmuir adsorption isotherm.^{42,63,97–99} By simultaneous analysis using the conventional Michaelis–Menten equation, which is typically used to analyze bulk reactions on soluble substrates in great excess to enzymes, the accessible enzyme attack sites on the PET surface can be estimated using the ratio of parameters derived from these swapped kinetic models.^{90,96}

The degradation-relevant binding of these PET hydrolases and variants was investigated by various biophysical approaches, such as quartz crystal microbalance,^{100–102} chemiluminescence,¹⁰⁰ and fluorescence.¹⁰³ Binding isotherms have been directly estimated based on the concentrations of free enzymes determined in the supernatant after incubation with PET.^{104–106} Selected PET hydrolases were shown to have a high affinity for the PET surface, as evidenced by the rapid formation of a monolayer, although this was thought to be mainly contributed by nonspecific adsorption.¹⁰⁶ A related kinetic study indicated that PET polymers were hydrolyzed at a remarkably lower rate than PET oligomers, regardless of their water solubility.⁹⁶ The conversion rates of these oligomers were found to be comparable to those of small-molecule *para*-

binding module	enzyme	fold improvement	reaction condition	ref	
PcAA14A	ThermoPETase	1.3	PET granules (3 g/L) incubated with 8.3 mg _{Enzyme} /g _{PET} in glycine- NaOH buffer (pH 9) for 5 days	137	
RolA	<i>Is</i> PETase	1.2 (by weight loss) 1.5 (by HPLC)	Preincubation with RolA for 3 h, then degradation of PET fiber waste and high-crystallinity PET powder (15 g/L) at pH 8, 30 $^{\circ}$ C with 1.3	136	
HGFI	<i>Is</i> PETase	 1.3 (by weight loss) 1.6 (by HPLC) 	g_{Enzyme}/g_{PET} for S days		
Zwitterionic polypeptide (EK)	<i>Is</i> PETase	11	Degradation of amorphous Goodfellow PET film and high-crystallinity (45.2%) beverage bottle with 200 nM enzyme in glycine-NaOH-buffer at pH 9 and 30–40 °C for up to 6 days	138	
СВМ	A cutinase from <i>T. fusca</i>	1.4–1.5 (only affinity)	Incubated with PET fiber and 50 μM enzyme in 50 mM Tris-buffer (pH 8) at 50 $^{\circ}\mathrm{C}$ for 24 h	104	
ChBD	LCCICCG	1.2	With 0.6 g/L amorphous Goodfellow PET film, post-consumer waste		
СВМ	LCC ^{ICCG}	1.3	PET (1ễ% crystallinity), or high crystallinity (40%) PET at 65 °C fc 12 h		
CBM	ThC_Cut1	1.4	With amorphous Goodfellow PET film and 25 mM enzyme in 100 mM	100	
PBM	ThC_Cut1	3.8	potassium phosphate buffer (pH 7) at 50 $^\circ\mathrm{C}$		

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nitrophenyl esters. This suggests that the complexation or dissociation with the degradable polyester strands requires large activation barriers, determining the overall conversion rate rather than the chemical catalysis itself, which showed, in addition, a similar hydrolysis enthalpy to those reported in the literature for other readily accessible esters.⁹⁵ Recently, the hydrolysis reaction mechanism of several PET hydrolases against PET-related oligomers was investigated using QM/ MM molecular dynamics (MD) simulations or adiabatic mapping to resemble polyester degradation.¹⁰⁷⁻¹¹⁰ Because there is only one cocrystallized IsPETase structure in a complex with a PET monomer analogue available so far, molecular docking of oligomeric aromatic esters has been widely used to study the substrate interaction in the binding groove as well as with the catalytic triad of various PET hydrolases. $^{16,65,87,111-113}$ The protein surface landscapes of bacterial PET hydrolases are comparable in close vicinity to the catalytic triad, requiring a high conformational selectivity of accommodated PET repeating units directly around the target ester bond at favored twisting angles.¹¹²⁻¹¹⁴ In contrast, it is unclear and unlikely if distal PET repeating units are involved in a catalysis-related interaction with additional surface residues which requires a long PET strand to adopt a specific conformation.^{113,115} Nonetheless, the defined polymer segment conformation directly next to the target ester bond will require a steric reconfiguration of the polymer chains with adequate mobility in order to form the productive tetrahedral intermediate via the initial nucleophilic attack by the catalytic serine.¹¹⁵ This is evidenced by the highest activation freeenergy barrier determined by QM/MM adiabatic mapping, suggesting the nucleophilic attack as a probable rate-limiting step (Figure 3).^{107,108} Further reaction steps of the PET hydrolysis mechanism are canonically the same as for other conventional ester hydrolases, in agreement with the recent findings in kinetic studies.⁹⁶

PET hydrolases are thought to possess dynamic catalytic sites with aromatic subsites which are locally stabilized upon substrate binding.^{65,112,116} For example, the conserved W185 in *Is*PETase was also found in many other known PET hydrolases (Figure 2B).^{116,117} A substitution of this residue usually resulted in a drastically reduced hydrolytic activity on PET.^{112,118} Recently, Chen et al. identified that S214 and I218 are uniquely present in *Is*PETase to reduce the steric hindrance of W185, therefore enabling a higher flexibility of the indole side chain, allowing a higher polymer hydrolysis rate.¹¹⁹

Introduction of the corresponding double-residue substitutions into homologous polyester hydrolases indeed boosted PET hydrolyzing activity, albeit at the expense of stability at temperatures >60 $^{\circ}$ C.

Large polymer segments may be unable to fit into a binding cleft that is too narrow. The overall catalytic properties of several PET hydrolases can be changed by widening or narrowing the binding clefts.^{97,120} Interestingly, the free energy barrier and hydrolytic reaction thermodynamics do not differ significantly between the thermophilic LCCI^{ICCG} mutant and the mesophilic IsPETase.¹⁰⁷ This suggests that the high activity of thermostable PET hydrolases is attributable mostly to the increased accessibility of PET polymer to nucleophilic attack at elevated temperatures, rather than to the fundamental interaction affinity. Austin et al. measured the width of the substrate binding cleft of IsPETase via the residue pair T88/ S238.⁶⁵ By substituting S238 to F, which is highly conserved in homologous cutinase-like PET hydrolases, increased hydrolytic activity on PET was determined when accompanied by the mutation W159H, although the binding cleft width appeared to be narrowed. This phenomenon suggests that the polymer binding in the surface groove is more likely a dynamic rather than static process, as supported by an NMR analysis of PET chain mobility in the context of enzymatic hydrolysis.^{115,121} The residue equivalent of the IsPETase S238 is F in TfCut2 and LCC.^{52,111} By substitution to A, I, and W, significantly increased PET hydrolysis activity was reported.^{16,122} These findings suggest that further systematic iterative engineering of all variable residues in the PET hydrolase binding pocket may be beneficial for gaining a thorough understanding of the ratelimiting interactions with aromatic polyesters and, as a result, improving the overall degradation performance.

Mono(2-hydroxyethyl) terephthalate (MHET) and bis(2hydroxyethyl) terephthalate (BHET) are degradation intermediates well-known to inhibit the efficiency of depolymerization catalyzed by various PET hydrolases, except for HiC and Cut190.^{50,78,123,124} MHET has a stronger inhibitory effect and can hardly be hydrolyzed by the wild-type *IsPETase*.⁹⁶ Thus, *I. sakaiensis* produces a distinct MHETase to yield TPA and EG for its growth.³⁴ This serves as a template for developing a dual enzyme system for effective PET degradation containing an oligo-ester-specific helper enzyme.¹²³ Recently, a chimeric dual-enzyme system with MHETase linked to *IsPETase* resembling their natural microbial host was established, resulting in PET degradation efficiency improved by at least 2.8-fold.¹²⁵ Additional MHETase-like enzymes from *Comamonas thiooxydans* and *Hydrogenophaga sp.* PML113¹²⁵ and an enzyme from a marine consortium¹²⁶ with similar structures but considerably lower substrate affinity for MHET than the *Is*MHETase¹²⁷ were also identified. This distinction in catalytic characteristics may provide a wide range of choices for combining with other depolymerizing enzymes, particularly for the use in whole cell-based multiple enzyme systems.^{128,129} While *Is*PETase has been successfully stabilized, additionally thermostabilizing MHETase-like enzymes would provide a robust two-enzyme system with industrial promise. Other technical solutions have been proposed in this regard, such as employing enzyme mutants that are less susceptible to product inhibition⁹⁹ or a membrane reactor for continuous removal of the inhibitors.¹³⁰

4. ENGINEERING ENZYMATIC DE/ADSORPTION ONTO PET SURFACES BY INCLUDING BINDING MODULES

To resemble other natural polymer degrading enzymes, specific polymer binding modules were either directly added in the reaction mixture or covalently fused to appropriate PET hydrolases. Among these, the cellulose-binding domains (CBM) CenA from *Cellulomonas fimi*¹⁰⁴ and that of cellobiohydrolase I from *Trichoderma reesei*,^{100,131} the polyhydroxyalkanoate (PHA)-binding module of PHA depolymerase from *Alcaligenes faecalis*,¹⁰⁰ and the chitin-binding module from the chitinase CmChi1 from *Chitinolyticbacter meiyuanensis* SYBCH1¹⁰³ increased the degradation performance when they were fused to the C-termini of PET hydrolases (Table 2). Selected tryptophan residues in CBMs were identified as mutation hot spots for enhanced hydrogen bond formation with aromatic moieties at the PET surface.^{104,132}

Hydrophobins are small amphiphilic proteins (about 20 kDa) produced by filamentous fungi with surfactant-like activity.¹³³ Although the highest boosting effect with hydrophobins was discovered when fused to a PET hydrolase, they can already improve the enzymatic binding affinity to the PET surface when introduced to the degradation mixtures as free molecules or applied to material as a pretreatment.^{134–136}

In this regard, the lytic polysaccharide monooxygenase (LPMO) from the white-rot fungus *Pycnoporus coccineus* (PcAA14A)¹³⁷ and a zwitterionic polymer based on positively charged lysine and negatively charged glutamate¹³⁸ were both recently shown to improve PET degradation performance when added to *Is*PETase. LPMO and the so-called EKylation, on the other hand, appear to promote the enzymatic degradation via different mechanisms than hydrophobins or other binding modules.

While the necessity of binding modules for effective cellulase-catalyzed cellulose degradation has been questioned,¹³⁹ their presence was recently found to alter the binding and hydrolysis kinetics at various solid loading levels.¹⁴⁰ The CBM was shown to favor low solid loading level in an adsorption-controlled scenario where higher catalytic efficiency is associated with tighter substrate binding but disfavored at high substrate concentrations, as shown by a so-called "volcano plot" of specific reaction rates against the binding strengths.¹⁴⁰ Accordingly, optimal PET hydrolases are suspected to also follow this Sabatier principle and will function at an intermediate substrate binding strength. Future research should be conducted to confirm this hypothesis based on comprehensive binding and hydrolysis kinetic studies with

various PET hydrolases, as well as those containing artificially introduced polymer binding modules, to clarify their roles for the interfacial biocatalysis, which is obviously missing so far. This is of great interest for potential industrial applications, where a very high solid loading level is generally preferred, in terms of an economical use of biocatalysts.

5. CONCLUDING REMARKS AND FUTURE PERSPECTIVES

More than 16 years have elapsed since the first microbial PET hydrolase was reported. Many research efforts have been expended in the quest for new PET hydrolases as well as in the optimization of known enzymes. A large number of highquality studies have been conducted using a few benchmark enzymes, such as cutinase(-like) enzymes from Thermobifida species,¹⁴¹ the plant compost-derived LCC cutinase, and IsPETase. Different research groups employed varying experimental conditions, such as pH, buffer compositions (different salts) and concentrations (different ionic strengths), and agitation techniques and speeds, making a balanced comparison of the degradation data very challenging, even when the same benchmark enzyme was used. Selected experimental parameters can also have a significant impact on the degradation performance as well as the related data interpretation in terms of interfacial biocatalysis mechanisms. For example, buffer salts can influence the enzyme performance¹⁴² and the solubility of degradation products or inhibitors,¹⁴³ and they can also fundamentally modify the water interaction with polymeric substrates.¹⁴⁴ When simultaneous mechanical treatment is occurring, the ideal water volume for enzymatic PET degradation can vary dramatically.⁴⁴ More crucially, studies employed PET materials from various suppliers, with varying crystallinity (even that of the widely used amorphous Goodfellow PET film may differ from batch to batch) and in various forms (powder, foil, sheet, etc.). As a result, standardization of PET hydrolysis tests and conditions using polymer samples with defined material sources and properties should be applied in future investigations to allow for a straightforward data comparison. Several recent studies used manually picked post-consumer low-crystallinity PET packaging in order to achieve striking enzymatic degradation performance at a small laboratory scale.^{88,145} However, in a real-world scenario, post-consumer PET packaging with all crystallinity patterns ends up in mixed household plastic waste which is collected and then separated in an industrial plastic sorting system according to polymer type and color, but not crystallinity.^{146,147} To remove the contaminants which may hamper the subsequent recycling process, a washing step (e.g., with hot soda water) is usually applied prior to thermomechanical reprocessing (e.g., shredding and drying).¹⁴⁸ These processes will age the sorted waste polymer considerably and consequently eliminate the lowcrystallinity fraction of PET. Following additional amorphization and micronization steps, these waste plastic flakes can be readily used for biotechnological recycling.^{16,92} Therefore, for lab-scale research in the field of PET hydrolases, using equally pretreated real-world PET waste (e.g., with the same amorphization and micronization equipment and protocols) instead of biased selection of a low-crystallinity fraction will deliver more reliable standardized data on the enzymatic degradation performance of industrial relevance.

As an alternative to the energy-consuming amorphization step,⁹² the challenge in lowering the polymer crystallinity is



Figure 4. Potential PET hydrolase screening methods arranged in order of increasing potential throughput. (A) Fluorogenic substrates like fluorescein dilaurate can be trapped in polyester films or particles^{175,176} and can be released and hydrolyzed upon polymer hydrolysis, generating a fluorescence signal. (B) Fluorimetric method based on the reaction of terephthalic acid with hydroxyl radicals to form the fluorophore 2-hydroxyterephthalic acid.^{177–179} Tens of thousands of clones can be screened using microtiter plate-based assays (A, B). (C) Agar plate assay based on the hydrolysis of polyester (PET) nanoparticles.^{75,180,181} Clear zones (halos) form around clones expressing active polyester-hydrolyzing enzymes, allowing simple visual identification. Millions of clones can easily be screened using this method. (D) Recently reported ultra-high-throughput droplet-based assay for PETase activity.¹⁸² The use of the fluorogenic surrogate substrate fluorescein dibenzoate indicates a low selectivity, since many other esterases would also be identified using this assay. Tens of millions of clones could be analyzed using this method. Combinations of the turbidimetric assay (C) and droplet-based methods (D) seem promising. (E) Ultra-high-throughput assay based on a terephthalic acid biosensor.¹⁸³ Cells could be entrapped in hydrogel beads¹⁸⁴ containing reporter cells that express GFP in response to terephthalic acid formed by clones expressing active PET-hydrolyzing enzymes. Because fluorescence-activated cell sorting (FACS) can be used to sort the beads, the throughput of this method is potentially in the hundreds of millions. (F) Envisaged growth selection approach based on the conversion of terephthalic acid to protocatechuic acid, which could be catabolized by engineered strains of *E. coli* or other model organism.^{183,185} The throughput of this method would be limited only by library size and transformation efficiencies, making it one of the most attractive methods.

envisaged to be possibly solved with a specific crystalline PET depolymerase, like those found in natural cellulase systems to decrystallize cellulose.¹⁴⁹ To this end, continuously growing PET hydrolase sequence data from large-scale sequencing projects can be used for exploring this missing enzyme activity and other novel PET hydrolases in genomic and metagenomic databases. EnzymeMiner and other available in silico tools provide useful computational platforms for automated identification of promising enzyme candidates for experimental validation.¹⁵⁰ Pan-genome analysis focusing on microbes which produce known PET hydrolases, e.g., in the Thermobifida and Ideonella genera, could facilitate finding yet-unknown MHETase-like enzymes to address the product-inhibition problem. Nevertheless, as the substrates of identified PET hydrolases and carbon sources for the host strains are unlikely to be synthetic polyester in their natural habitats, the probability of success of such a research activity is hard to

predict. The explored sequence space can also be used to predict enzymes with improved properties by machine learning and ancestral sequence reconstruction.^{151–153} Robust proteins can be designed by sequence-based approaches and fully automated computational workflows, like FireProt^{ASR}, making complex protocols of ancestral inference accessible to nonexperts.¹⁵⁴ Recent developments of highly accurate protein structure prediction methods, like AlphaFold2 and RoseTTA-Fold, can assist a structure-based design of novel PET hydrolases identified by database searches.¹⁵⁵⁻¹⁵⁷ While hydrolytic biocatalysis might fundamentally be unable to crack the well-ordered crystalline PET, oxidative enzymes, which may have a mechanistically comparable function to LPMOs known from lignin and cellulose degrading systems,¹⁵⁸ can offer further options for mining for polyester decrystallizing activities.

High-quality structures incorporating PET relevant ligands will be required for further understanding of the structurefunction relationship and related engineering of PET hydrolases. Application of novel cryoEM techniques to examine the binding of bigger polymer substrates may be required for a thorough understanding of the substrate-enzyme interaction at the solid-liquid interface. To date, these mechanistic insights have primarily been derived from docking and simulation experiments using flexible PET oligomers, which overlook the inherent mobility and steric constraints given by neighboring polymers under realistic reaction conditions. The utilization of particular force fields designed for interface reactions, as well as taking into account real-world material properties, will help in silico protein engineering even more.¹⁵⁹ The calculated energy barriers for PET hydrolysis are balanced for individual reaction stages (Figure 3), implying that more than one catalytic step would need to be enhanced at the same time. This is typically difficult to address rationally, providing room for directed evolution and machine learning. Hence, the future development of suitable screening assays applicable to large enzyme libraries is of particular relevance in this regard. Due to technical limitations of individual approaches, achieving ultra-high-throughput screening specifically for PET degradation activity still remains a challenge (Figure 4).

Furthermore, researchers may investigate the power and specific advantages of using biocatalysts over chemical catalysts, such as when combined with living cells as wholecell catalysts, which can potentially allow for a one-pot process that simultaneously includes an enzyme cascade not only to degrade the plastics but also to convert the degradation intermediates into a variety of products with added value.³² The utility of mesophilic enzymes can potentially be reemphasized using such a procedure, because numerous metabolic pathways converting monomers to other valueadded compounds are currently only available/engineerable in mesophilic microbial frameworks. Aside from the wellengineered frameworks such as Pseudomonas putida, E. coli, and P. pastoris,¹⁶⁰⁻¹⁶⁴ I. sakaiensis has recently emerged as a new promising strain for genomic engineering with considerably high conversion efficiency from PET substrates to PHA biopolymers.^{37,129} On the other hand, thermophilic whole-cell biocatalysts such as Clostridium thermocellum can be easily employed for faster PET depolymerization, for example, targeting textile waste also containing cellulose, which may be degraded and valorized simultaneously.^{21,165} For more details regarding the biotechnological potential of enzymatic textile recycling, readers are referred to a recent comprehensive review by Jönsson et al.²¹ In this regard, designing the PET degrading multienzyme complex by combining the advantages of various enzyme classes to resemble an architecture similar to the natural cellulosome might be a viable option.¹²⁸

A photosynthetic microalga, *Phaeodactylum tricornutum*, has been engineered to functionally express *Is*PETase and is able to degrade selected PET-related materials in a saltwater environment at 21-30 °C.¹⁶⁶ This has been suggested to be a potential bioremediation approach for seawater polluted by PET microplastics, although the conversion rate was very low and the application of genetically engineered microorganisms in an open environment is currently strictly forbidden worldwide.⁹ Although a recent study has reported wild-type marine microbes with PET-metabolizing activity,¹⁶⁷ microplastics present in aquatic ecosystems can hardly support microbial growth and will therefore remain as persistent xenobiotics that cannot be remediated easily.¹⁶⁸

Scientists have thus far succeeded in identifying and creating biocatalysts that appear to fit the need for PET waste depolymerization on an industrial and commercial scale. The fundamental understanding of interfacial biocatalysis on PET should be extended and transferred to address the challenges associated with the biotechnological degradation of other more abundant plastics such as polyolefins or more similar plastics such as polyamides (PA) and polyurethanes (PUR) with hydrolyzable backbones.^{21,32,169} While the breakdown of carbon-carbon backbones in polyolefins can be energetically very challenging,^{170,171} chemical and thermal pretreatments have been shown to enable subsequent biochemical transformation^{172,173} and thus should be extensively studied in future research. On the other hand, the identification of putative PUR or PA hydrolases is envisioned as a result of collaborative large-scale research activities (e.g., the MIX-UP project¹⁷⁴ and the upPE-T project) on plastic recycling. A combination of these novel biocatalysts will pave a new path for the valorization of unsorted mixed plastic waste that cannot be efficiently recycled via other disposal approaches at an industrial scale.

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Notes

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Article II



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¹ Structural Insights into (Tere)phthalate-Ester Hydrolysis by a ² Carboxylesterase and Its Role in Promoting PET Depolymerization

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7 ABSTRACT: TfCa, a promiscuous carboxylesterase from *Thermobifida fusca*, was found to hydrolyze 8 polyethylene terephthalate (PET) degradation intermediates such as bis(2-hydroxyethyl) terephthalate 9 (BHET) and mono-(2-hydroxyethyl)-terephthalic acid (MHET). In this study, we elucidated the 10 structures of TfCa in its apo form, as well as in complex with a PET monomer analogue and with BHET. 11 The structure-function relationship of TfCa was investigated by comparing its hydrolytic activity on 12 various ortho- and para-phthalate esters of different lengths. Structure-guided rational engineering of 13 amino acid residues in the substrate-binding pocket resulted in the TfCa variant I69W/V376A (WA), 14 which showed 2.6-fold and 3.3-fold higher hydrolytic activity on MHET and BHET, respectively, than 15 the wild-type enzyme. TfCa or its WA variant was mixed with a mesophilic PET depolymerizing enzyme 16 variant [*Ideonella sakaiensis* PETase (*Is*PETase) PM] to degrade PET substrates of various crystallinity. 17 The dual enzyme system with the wild-type TfCa or its WA variant produced up to 11-fold and 14-fold 18 more terephthalate (TPA) than the single *Is*PETase PM, respectively. In comparison to the recently 19 published chimeric fusion protein of *Is*PETase and MHETase, our system requires 10% *Is*PETase and 20 one-fourth of the reaction time to yield the same amount of TPA under similar PET degradation



21 conditions. Our simple dual enzyme system reveals further advantages in terms of cost-effectiveness and catalytic efficiency since it 22 does not require time-consuming and expensive cross-linking and immobilization approaches.

23 KEYWORDS: PET hydrolysis, plastic, dual enzyme system, carboxylesterase, structure, enzyme engineering

24 INTRODUCTION

25 In recent years, enzymatic depolymerization of polyethylene 26 terephthalate (PET) has emerged as an alternative technology 27 to conventional mechanical and chemical plastic recycling 28 approaches.¹ TfH from Thermobifida fusca (T. fusca) was the 29 first enzyme discovered in 2005 to possess PET degrading 30 activity.² Since then, many new PET hydrolases (PETases) 31 have been identified and engineered for higher PET 32 degradation efficiency.³⁻⁵ Enzymatic PET hydrolysis produces 33 small-molecule degradation products, which can be recovered 34 and used to synthesize virgin polymers.^{5,6} In addition to the desired PET monomers terephthalate (TPA) and ethylene 35 glycol (EG), bis(2-hydroxyethyl) terephthalate (BHET) and 36 37 mono-(2-hydroxyethyl)-terephthalate (MHET) are also re-38 leased as degradation intermediates that are known as inhibitors for selected PETases. 39

⁴⁰ Methods for mitigating the product inhibition during ⁴¹ enzymatic PET hydrolysis include the continuous removal of ⁴² small-molecule products using ultrafiltration membranes,⁸ the ⁴³ use of engineered PETase variants that are less affected by the ⁴⁴ inhibitors,⁹ and the introduction of a helper enzyme with a ⁴⁵ specific hydrolytic activity on the inhibitors. *Ideonella sakaiensis* (*I. sakaiensis*) is a bacterium that can degrade PET and 46 assimilate its monomers.¹⁰ In addition to the extracellular *I.* 47 sakaiensis PETase (*Is*PETase) which can depolymerize PET 48 predominantly to MHET, the intracellular MHETase has been 49 assumed to facilitate the PET assimilation by converting 50 MHET to TPA and EG.^{10,11} This allowed for the development 51 of a chimeric MHETase:*Is*PETase fusion protein exhibiting 52 markedly improved PET depolymerization activity.¹² At 30 °C 53 and pH 7.5, this chimeric system produced approximately 54 sixfold more degradation products in 96 h than single *Is*PETase 55 in the PET hydrolysis. TfCa is a *T. fusca* carboxylesterase with 56 hydrolytic activity on PET oligomers, including MHET, 57 BHET, and a cyclic PET trimer.^{13,14} When TfCa was 58 immobilized on a SulfoLink resin and then coupled with 59 various PETases such as LC-cutinase or TfCut2 for PET 60

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Α

61 degradation, the yield of degradation products was up to 62 twofold higher than when TfCa was absent.¹⁵ Nevertheless, 63 both dual enzyme systems may be less feasible for industrial 64 applications due to the need of an efficient cross-linking 65 method or the high cost of the immobilization matrix. 66 Therefore, a low-cost dual enzyme system with enhanced 67 PET oligomer hydrolyzing activity is required.

While the crystal structures of MHETase have been recently 68 69 solved and repeatedly reported, 11,12,16 the structural basis 70 underlying the mechanism of TfCa-catalyzed hydrolysis of 71 TPA esters remains elusive. In this study, we elucidated the 72 first crystal structure of TfCa in its apo form and in complex 73 with the MHET-like analogue 4-[(2-hydroxyethyl) carbamoyl] 74 benzoic acid (MHETA) and BHET at atomic resolutions. By 75 comparing its specific activity on various TPA esters and an 76 ortho-phthalate ester (diethyl phthalate, DEP), the structural 77 basis for substrate recognition and hydrolysis by TfCa was 78 explored. Moreover, we rationally engineered TfCa and 79 obtained a mutant with significantly higher MHET and 80 BHET hydrolytic activity. This TfCa variant was applied in a 81 simple dual enzyme system in combination with an IsPETase
 82 penta-mutant, IsPETase^{S121E/D186H/R280A/N233C/S282C} (IsPETase 83 PM), for enhanced degradation of a variety of PET substrates 84 with different crystallinity.

85 MATERIAL AND METHODS

Materials. Chemicals and consumables were purchased 86 87 from Merck KGaA (Darmstadt, Germany), Sigma-Aldrich (Steinheim, Germany), Thermo Fisher Scientific (Waltham, 88 89 MA, USA), and New England Biolabs GmbH (Frankfurt am 90 Main, Germany) unless stated otherwise. Primers were ordered 91 from Eurofins (Ebersberg, Germany) and Thermo Fisher 92 Scientific (Waltham, MA, USA). The amorphous PET film 93 (GfPET, ES30-FM-0001445) and the semi-crystalline PET 94 powder (maximum particle size: 300 μ m, crystallinity >40%, 95 product number: ES306031/1) were purchased from Good-96 fellow GmbH (Bad Nauheim, Germany). PET nanoparticles 97 (PET-NPs) were prepared as described previously by Pfaff et 98 al.,¹⁷ bis[2-(benzoyloxy)ethyl] terephthalate was defined as 99 3PET and synthesized according to Fischer-Colbrie et al.,¹⁸ 100 MHETA was synthesized as described by Palm et al.¹¹

101 METHODS

Crystallization, Data Collection, Structure Determi 103 nation, and Refinement. All crystallization experiments **104 were conducted at 25** °C using the sitting-drop vapor-diffusion **105 method.** In general, 1 μ L TfCa solution (40 mg/mL in 25 mM **106 Tris**-HCl containing 150 mM NaCl, pH 7.5) was mixed with **107 1** μ L reservoir solution in 48-well Cryschem Plates and **108 equilibrated against 100** μ L of the reservoir solution. The **109 optimized crystallization conditions of TfCa and TfCa E319L 110 were 22% (w/v) poly(acrylic acid) sodium salt 5100, 0.02 M 111 MgCl**₂, 0.1 M HEPES at pH 7.5. The mutant TfCa E319L was **112 created to eliminate residue E319 of the catalytic triad to avoid 113 the hydrolysis of the substrate during the soaking period. A 114 detailed description of the enzyme expression for crystal-115 lization purposes is included in the Supporting Information.**

Within 5–6 days, the crystals reached their final size suitable for X-ray diffraction. The TfCa and TfCa E319L crystals in complex with MHETA, BHET, or MHET plus BHET were obtained by soaking the enzyme with 10 mM of each compound for 72 h.

All the X-ray diffraction data sets were collected at the 121 National Facility for Protein Science in Shanghai at Shanghai 122 Synchrotron Radiation Facility at the beamlines BL10U2/ 123 BL02U1(BL17U)/BL17B/BL18U1/BL19U1, and in Berlin at 124 the third-generation synchrotron radiation source (BESSY II) 125 with beamline 14.1.¹⁹ The crystals were mounted in a cryoloop 126 and soaked with cryoprotectant solution [25% w/v poly(acrylic 127 acid sodium salt) 5100, 0.02 M MgCl₂, 0.1 M HEPES pH 7.5, 128 10% glycerol] prior to data collection at 100 K. The diffraction 129 images were processed using HKL2000. The crystal structure 130 of TfCa was solved by the molecular replacement method with 131 the Phaser program²⁰ from the Phenix²¹ suite using the 132structure of the carboxylesterase from Geobacillus stearothermo- 133 philus (PDB-ID: 20GT) as a search model. Further refinement 134 was carried out using the programs phenix.refine²² and Coot.²³ 135 Prior to structural refinement, 5% of randomly selected 136 reflections were used for calculating $R_{\rm free}^{24}$ to monitor the 137 refinement process. Data collection and refinement statistics 138 are summarized in Table S1. 139

Expression and Purification of Recombinant TfCa 140 and IsPETase PM. For enzymatic PET degradation, the TfCa 141 gene was cloned into a pET20b(+) vector and the plasmid was 142 transformed into Escherichia coli BL21 (DE3). Bacterial cells 143 were grown in lysogeny broth (LB) medium at 37 °C to an 144 optical density at 600 nm (OD₆₀₀) of 1 and then further 145 incubated at 18 °C. When the OD_{600} reached 1.5, recombinant 146 protein expression was induced by adding 1 mM isopropyl β - 147 D-thiogalactopyranoside and cells were further grown at 18 °C 148 until an OD₆₀₀ of 3. Cells were harvested by centrifugation at 149 $10,000 \times g$ for 5 min. Cell pellets were re-suspended in lysis 150 buffer containing 50 mM Na₂HPO₄, pH 8, and 150 mM NaCl, 151 followed by disruption by ultrasonication $(3 \times 90 \text{ s}, 50\% \text{ pulse}, 152)$ 50% power, 2 min breaks). Cell debris was removed by 153 centrifugation at 10,000 \times g for 30 min. The supernatant was 154 then applied to a Ni²⁺-nitrilotriacetic acid column, washed with 155 lysis buffer and a 20-90 mM imidazole gradient as described 156 before.¹⁴ The enzyme with an apparent molecular mass of 55 157 kDa was eluted with 250 mM imidazole, which was then 158 exchanged to the assay buffer (25 mM Tris-HCl, pH 7.5, set 159 at 45 °C) using Vivaspin (Sartorius Lab Instruments, 160 Göttingen, Germany) with 10 kDa cutoff. The membrane of 161 the Vivaspin was equilibrated with 5 mL Tris-HCl buffer (25 162 mM, pH 7.5, set at 45 °C) by centrifugation for 5 min at 5000 163 \times g. Afterward, the eluted protein was added to the Vivaspin, 164 topped with 5 mL Tris-HCl buffer, and centrifuged for 15 min 165 at 5000 \times g and 4 °C. After repeating this four times, the 166 enzyme was removed from the upper compartment of the 167 Vivaspin column. The enzyme concentration was determined 168 using a NanoDrop 1000 device (Thermo Fisher Scientific, 169 Waltham, MA, USA). IsPETase PM was expressed as described 170 by Brott et al.²⁵ and purified as described here for TfCa. The 171 model substrate para-nitrophenyl acetate (pNPA) was used for 172 determining the enzymatic activity as described before.¹⁴ 173

Site-Directed Mutagenesis. Mutation of the TfCa- 174 encoding gene was performed using the Q5 Site-Directed 175 Mutagenesis Kit (New England Biolabs GmbH, Frankfurt am 176 Main, Germany) according to the supplier's protocol. 177 Successful mutagenesis was confirmed by sequencing. 178

Enzymatic Production of the Substrate MHET. Similar 179 to terephthalic acid, commercially available MHET has a 180 benzoic acid end group and is hence almost insoluble in 181 aqueous solutions without organic solvents. Therefore, soluble 182 MHET with a deprotonated carboxylate end was prepared 183

266

184 from controlled enzymatic BHET degradation using TfCa as 185 described earlier.⁷ Up to 100 mM BHET was added into 186 ethanol and sonicated in a water bath for 30 min until BHET 187 was dissolved to form a clear solution. The production of 188 MHET was carried out in a 50 mL reaction volume, containing 189 20 mM of BHET in ethanol, 550 nM of purified TfCa, and 25 190 mM Tris-HCl buffer (pH 7.5, set at 45 °C). The final 191 concentration of ethanol in the reaction was 10%. The solution 192 was incubated at room temperature for 30 min without 193 agitation. After incubation, the sample was heated to 80 °C for 194 10 min to inactivate TfCa and then centrifuged $(10,000 \times g, 5)$ 195 min) to remove insoluble compounds. The supernatant was 196 analyzed using high-performance liquid chromatography (HPLC) to ensure MHET purity and then used as a substrate 197 198 for further enzyme characterizations.

Enzymatic Hydrolysis of Various Substrates. Enzy-199 200 matic hydrolysis of the small ester substrates 3PET, BHET, 201 MHET, and DEP was performed in 1 mL reaction volume 202 using 25 mM Tris-HCl buffer (pH 7.5) at 50 °C with 550 nM 203 purified enzyme unless stated otherwise. In total, 2 mM 3PET, 204 BHET, or MHET, or 5 mM DEP were used in the reactions. 205 For an enhanced solubility of the substrates, the hydrolysis of 206 3PET, BHET, and MHET was performed in the presence of 207 10% ethanol and that of DEP hydrolysis in 10% dimethyl 208 sulfoxide. Sampling at different time points during hydrolysis 209 reactions was performed as indicated below in the Results 210 section. The degradation products benzoic acid (BA), BHET, 211 MHET, and TPA were confirmed by HPLC, whereas 212 monoethyl phthalate (MEP) was confirmed by liquid 213 chromatography coupled with mass spectrometry (LC-MS). 214 A detailed description of the LC-MS method is included in 215 the Supporting Information.

In a dual enzyme system, PET NPs, PET powder, or PET 216 217 film were employed as substrates. PET NPs were used at a final 218 concentration of 2, 20, and 200 μ g/mL, whereas PET powder 219 and PET film were used at a final concentration of 60 mg/mL 220 in Tris-HCl buffer (set to pH 7.5 at 45 °C). Purified IsPETase 221 PM was used at a concentration of 30 nM for PET NPs and 50 222 nM for PET film and PET powder as described before.²⁵ The 223 amounts of the aromatic products were determined using 224 HPLC according to Palm et al.¹¹ The amount of TPA, MHET, 225 or BHET was calculated based on a TPA standard curve and 226 the amount of MEP was calculated based on a phthalic acid (PA) standard curve. The specific activity was calculated as U/ 227 228 mg_{enzyme}, while one unit (U) was defined as one μ mol substrate 229 converted per min.

Determination of Melting Points. The melting points $_{231}$ ($T_{\rm m}$) of TfCa and its mutants were determined using nano $_{232}$ differential scanning fluorimetry on a Prometheus NT.48 $_{233}$ device (NanoTemper Technologies, Munich, Germany). $_{234}$ Purified enzymes at a concentration of 300 μ g/mL were $_{235}$ used to monitor the thermal denaturation profiles from 40 to $_{236}$ 80 °C at 1 °C/min steps. $T_{\rm m}$ was calculated based on the $_{237}$ excitation changes at 285 nm with emission wavelengths at 330 $_{238}$ and 350 nm.

Molecular Docking. Molecular docking of 3PET, DEP, and MEP into the active site of TfCa was performed with an AutoDock Vina v1.2.0 and Dockprep as part of Chimera v1.15.²⁶ The docking for 3PET was performed in a box with an edge length of 50 Å around S185, the docking for DEP and MEP was performed in a box with an edge length of 25 Å for DEP and MEP around residue A108, which includes the active site and its surroundings. The AutoDock Vina score was set to 246 –9.9, –6.2, and –6.0 for 3PET, DEP, or MEP, respectively. 247

Molecular Dynamics Simulations. The crystal structures 248 of TfCa with the ligand MHETA (PDB-ID: 7W1J, 1.92 Å) as 249 well as the chain A structure of MHETase from *I. sakaiensis* 250 (PDB-ID: 6QGA, 2.1 Å)^{11,27} were used for molecular 251 dynamics (MD) simulations. In total, three independent MD 252 replicates with 20 ns long production simulation were run for 253 each system at 310 K (37 °C) using the Langevin thermostat at 254 a constant pressure of 1.0 bar and a pressure coupling constant 255 of 1.0 ps. Coordinates were saved at intervals of 4 ps. In total, 256 60 ns of simulation time was produced for each enzyme- 257 ligand system.

Each complex was clustered into three trajectories and the 259 molecular mechanics/generalized Born surface area (MM/ 260 GBSA)^{28,29} method was applied to calculate the binding free 261 energy (ΔG_{bind}) of MHET in the enzymes and the respective 262 residue-by-residue interactions.^{28,30} A more detailed descrip- 263 tion of these MD simulations is included in the Supporting 264 Information. 265

RESULTS

Structure of TfCa in Its Apo Form. The ligand-free wild- 267 type TfCa (TfCa wt) was crystallized in the monoclinic space 268 group P21 (PDB-ID: 7W1K, 1.40 Å). The enzyme is built from 269 three domains, a hydrolase domain that adopts the fold of a 270 canonical α/β hydrolase with a central antiparallel β -sheet 271 surrounded by α -helices, a lid domain A and a lid domain B 272 (Figure 1A). As predicted from sequence alignment with 273 fl homologous enzymes that exhibit carboxylesterase activity, 274 TfCa contains a strictly conserved catalytic triad consisting of 275 the residues S185, E319, and H415. Hence, a p-nitrobenzyl 276 esterase (pNB-E) from Bacillus subtilis (PDB-ID: 1QE3) and 277 the carboxylesterase Est55 from G. stearothermophilus (PDB- 278 ID: 2OGS) were used as templates for elucidating the 279 backbone structure of TfCa. Within the catalytic triad of 280 TfCa, S185 serves as the nucleophile and is located within 281 hydrogen-bond (H-bond) distance to be polarized by the base 282 H415, which is stabilized by the acid E319. A sequence 283 alignment, as well as structural alignments of pNB-E, Est55, 284 and TfCa, are shown in Figures S1 and S2. 285

Binding Modes to PET-Related Ligands. To explore the 286 catalytic mechanism of TfCa, protein crystals were soaked with 287 the substrates MHET and BHET as well as with the substrate 288 analogue MHETA. MHETA has an amide bond in place of the 289 ester bond in MHET and can hence not be hydrolyzed by 290 esterolytic enzymes including TfCa. With TfCa wt, a ligand- 291 bound structure of TfCa with MHETA (PDB-ID: 7W1J, 1.92 292 Å) was solved. By mutating E319 in the catalytic triad, an 293 inactive TfCa variant E319L was generated. This variant 294 allowed for stable substrate binding and two additional 295 complex structures with BHET (PDB-ID: 7W1L, 2.43 Å) 296 and with both degradation intermediates, MHET and BHET 297 (PDB-ID: 7W1I, 1.67 Å). In the ligand-bound structures of 298 TfCa, the ligands were located at the bottom of a deep active 299 site cleft containing the hydrophobic residues L282, L322, and 300 V376. The side chain of the catalytic S185 is within H-bonding 301 distance to the ester oxygen atom of BHET (PDB-ID: 7W1I, 302 Figure 1E) and the nitrogen atom of MHETA (PDB-ID: 303 7W1J, Figure 1B). 304

The overall structures of TfCa and MHETase and their 305 binding modes to the ligand MEHTA are compared as shown 306 in Figure 1A–D. While MHETase consists of one hydrolase 307



Figure 1. Ligand-free and complex structures of TfCa from T. fusca in comparison to MHETase from I. sakaiensis. (A) Crystallographic structure of TfCa reveals three subdomains: hydrolase domain (TfCa^{Hyd}, brown), lid domain A (TfCa^{LidA}, dark blue), and lid domain B (TfCa^{LidB}, cyan). The catalytic triad consisting of S185, E319, and H415 is shown as green sticks. (B) Close-up view of the active site of TfCa with bound MHETA (yellow) (PDB-ID: 7W1J, $1.92\,$ Å). Residues from different domains are shown in brown (TfCa^{Hyd}), dark blue (TfCa^{LidA}), and cyan (TfCa^{LidB}). (C) Structure of MHETase from I. sakaiensis with its two domains: the hydrolase domain (MHETase^{Hyd}, orange) and the lid domain (MHETase^{Lid}, dark aquamarine) (PDB-ID: 6QGA).¹¹ (D) Close-up view of the active site of MHETase with bound MHETA (yellow). Residues from different domains are shown in orange (MHETase $^{\rm Hyd})$ and dark aquamarine (MHETase^{Lid}). (E) Close-up view of the active site of TfCa E319L with bound BHET (yellow) and MHET (green) (PDB-ID: 7W1I, 1.67 Å). Dashed lines indicate H-bond formation, molecules and interacting residues are colored by atom types: carbon: varying colors, nitrogen: blue, oxygen: red. Residues of the catalytic triad are shown as green sticks.

308 domain and one lid domain, the overall structure of TfCa can 309 be divided into one hydrolase domain and two lid domains 310 (Lid A and Lid B). In the active site of TfCa, only three H-311 bonds are formed, preliminarily with the amide bond and the 312 neighboring hydroxyl end in MHETA (Figure 1B). By 313 comparison, five H-bonds are present in MHETase to interact 314 with both ends of the MHETA ligand (Figure 1D). Side chains 315 of selected phenylalanine residues (F323 and F377 for TfCa, 316 F495 and F415 for MHETase) were found to be potentially 317 involved in stabilizing the TPA moiety in MHETA. In 318 MHETase, F415 and F495 are located on both sides of the 319 benzoic ring of the soaked MHETA ligand. In contrast, F323 320 and F377 in TfCa are exclusively positioned on one side of 321 MHETA. This binding mode may only permit a staggered 322 stacking interaction of F323 and a very weak T-shaped 323 interaction of the more distant F377 from the same direction

to the TPA moiety (Figure 1B). Similar interactions between 324 these two aromatic residues and the BHET ligand (Figure 1E) 325 suggest that F377 plays a minor role in the substrate 326 stabilization. 327

We also investigated the binding of MHET to TfCa and 328 MHETase using MD simulations. As shown in Table S5, by 329 clustering the snapshots during the 60 ns productive 330 simulations, MHET has a significantly higher likelihood of 331 staying in the substrate binding pocket of MHETase than in 332 that of TfCa. For clustering the snapshots, the distance 333 between the MHET ester carbonyl atom and the side chain 334 oxygen of the catalytic serine in each enzyme is defined as the 335 catalytic C-O distance. Those snapshots with a catalytic C-O 336 distance less than 4.5 Å were selected to calculate the binding 337 free energy of MHET to individual residues in the substrate 338 binding pocket of each enzyme using MM/GBSA.²⁹ In 339 MHETase we found that, in addition to the aforementioned 340 F415 and F495, R411 and W397 considerably contribute to 341 the interaction with MHET (Table S3 and Figure S10B). By 342 contrast, in TfCa, certain small residues such as G106, G107, 343 and A108 appear to play an important role in the binding to 344 MHET, in addition to the amino acids neighboring S185 and 345 the aromatic residues F323 and F377 discovered in the crystal 346 structures (Figures 1B,E and S10A). In accordance with the 347 crystal structure analysis, MD simulation results support the 348 conclusion that MHETase has a higher overall binding affinity 349 to MHET than TfCa.

Substrate Profile of TfCa. The substrate profile of TfCa 351 was investigated with TPA-based oligo-esters of various 352 lengths, such as MHET, BHET, and 3PET, as well as the 353 ortho-phthalate ester DEP. HPLC-derived product profile 354 allowed us to hypothesize the degradation pathways of longer 355 substrates and estimate the specific activity of TfCa in 356 hydrolyzing various esters at each reaction step (Figure 2). 357 f2

MHET is the monoester of TPA and EG and also the 358 smallest among all the investigated substrates. The specific 359 activity of MHET hydrolysis by TfCa was 0.024 U/mg_{enzyme} as 360 shown in Figure 2A. BHET is the diester of one TPA with two 361 EG. The first hydrolysis of BHET will form MHET and EG, 362 while the second hydrolysis step yields TPA and EG (Figure 363 2B). The specific activity of TfCa for the first BHET hydrolysis 364 step was found to be much higher $(5.12 \text{ U/mg}_{enzyme})$ than that 365 of the second hydrolysis step (0.011 U/mg_{enzyme}) (Figure 366 2A,B). Although the second hydrolysis step of BHET is 367 equivalent to the MHET hydrolysis, it revealed an approx- 368 imately two times lower specific activity than the primary 369 MHET hydrolysis. This can be attributed to a less-preferred 370 binding of MHET in the presence of the competitive substrate 371 BHET, which can be hydrolyzed nearly 500 times faster by 372 TfCa. 373

Similar to BHET, DEP is a diester of ortho-phthalate and 374 ethanol (Figure 2D). After 1 h of incubation at 50 °C, DEP 375 was not detectable as a result of TfCa-catalyzed hydrolysis. 376 LC-MS analysis suggested that DEP was completely 377 converted to MEP (Figure S11), which can also be monitored 378 as a new peak at a retention time of 11.25 min on HPLC. The 379 specific activity of this primary hydrolysis step is 1.64 U/ 380 mg_{enzyme}, which is 3 times lower than BHET hydrolysis but 82 381 times higher than MHET hydrolysis. MEP was not further 382 hydrolyzed to PA, suggesting that it is a less-preferred substrate 383 for TfCa than MHET. 384

3PET is the longest oligomer investigated in this study with 385 four ester bonds. TfCa-catalyzed hydrolysis of 3PET can yield 386


Figure 2. TfCa catalyzed hydrolysis of (tere)phthalate esters of various lengths. (A) Specific activity of TfCa for the hydrolysis of the first ester bond in each model substrate. The specific activity is shown on a logarithmic scale. (B) Specific activity of TfCa for the hydrolysis of the second ester bond in 3PET and BHET. The specific activity is shown on a logarithmic scale. Error bars indicate the standard deviations calculated from at least three replicates. Putative degradation pathways for (C) BHET, (D) DEP (TfCa can only catalyze the hydrolysis of DEP to MEP), and (E) 3PET. For simplicity, EG is not shown as a degradation product. Chemical structures and schemes were drawn with ChemDraw 21.0.0.

387 different product profiles depending on where the first 388 hydrolysis step occurs (Figures S9 and 2E). After 10 min 389 hydrolysis reaction with TfCa at 50 °C, 2-hydroxyethyl-390 benzoate (HEB) was detected as one product, of which the 391 amount decreases with the reaction duration. Consequently, 392 we suggest a preferential degradation pathway of 3PET, which 393 releases HEB as an intermediate product from 3PET by TfCa. 394 This degradation pattern is similar to that described by Eberl et 395 al.³¹ for 3PET hydrolysis catalyzed by a *T. fusca* cutinase. 396 However, the other product from the first hydrolysis step, 4-397 {[2-(benzoyloxy)ethoxy]-carbonyl} benzoic acid (BECBA) cannot be detected by HPLC. Based on the rate of HEB 398 399 formation, we determined a specific activity of 0.06 U/mg_{enzyme} 400 for the first hydrolysis step of 3PET. This is three times higher 401 than that for MHET but 85 times and 27 times lower than for 402 BHET and DEP, respectively. The lower specific activity for 403 3PET is probably due to the size of the substrate. The high 404 specific activity observed for BHET and DEP suggests that 405 (tere)phthalate diesters may have the ideal size for the 406 substrate binding pocket of TfCa. In the second hydrolysis step 407 of 3PET, both HEB and BECBA are further hydrolyzed. This 408 can be verified by the decreasing concentration of HEB and the 409 increasing amounts of BA and MHET in the samples at the 410 later reaction stage. The estimated specific activity of this

reaction step is lower than the first step hydrolysis of 3PET but 411 slightly higher than MHET (Figure 2A). HEB is a monoester 412 comparable to MHET, whereas BECBA is a diester with two 413 aromatic moieties. The markedly lower specific activity 414 observed for BECBA compared to BHET suggests that the 415 additional aromatic ring may hinder the TfCa hydrolysis 416 efficiency. This is consistent with a previous study demonstrat- 417 ing that TfCa can hydrolyze BHET faster than 1,2-ethanediyl 418 bis(4-methylbenzoate).³² Similar to BECBA, the latter model 419 substrate is a diester with two aromatic moieties and is also 420 commonly used to resemble PET repeating units. The final 421 reaction step of 3PET hydrolysis is MHET hydrolysis, which 422 releases TPA and EG. After a 6 h reaction, MHET was the 423 major product measured by HPLC, followed by BA and TPA 424 (Figure S6). 425

A previous study has shown that MHETase possesses an 426 exo-PETase activity allowing for the hydrolysis of the terminal 427 ester groups of PET polymers.¹⁶ Accordingly, we tested TfCa 428 for its capacity to hydrolyze PET end groups but were unable 429 to demonstrate its exo-PETase activity (Figures 2A and S7). 430

Structure-Based Enzyme Engineering of TfCa. To 431 improve the activity of TfCa on MHET and BHET, amino acid 432 residues within 5 Å of the soaked ligands (Figures 1B,E and 433 \$3) were selected for rational engineering. Among the 29 434



Figure 3. Semi-rational enzyme engineering of TfCa and characterization of the most active TfCa^{I69W+V376A} (WA) mutant. (A) Relative activity of mutants compared to TfCa wt based on the hydrolysis of 2 mM BHET into TPA at 45 °C in 25 mM Tris-buffer (pH 7.5, set at 45 °C). The amount of the degradation product TPA was determined by HPLC analysis. (B) Relative residual activity determined at 25 °C after 1 h incubation at various temperatures. The hydrolytic activity was determined with the model substrate pNPA in 25 mM Tris–HCl buffer (pH 7.5, set at 25 °C). The data determined at 4 °C were used as reference values to define 100% residual activity. (C) 2 mM BHET or MHET were degraded with TfCa wt or TfCa WA at various temperatures in 25 mM Tris–HCl buffer (pH 7.5) for 6 h. The amount of the degradation products MHET and TPA were determined by HPLC. (D) The rates of TPA yield from MHET were determined with 0.55 μ M TfCa wt or the variant WA at various substrate concentrations ranging from 0.5 to 7 mM. Reaction supernatants were taken after 30 min of incubation at 50 °C in 25 mM Tris-buffer (pH 7.5, set at 50 °C) and subjected to HPLC analysis. Error bars indicate the standard deviations calculated from at least three replicates.

435 amino acids identified, all alanine, glycine, and proline residues, 436 and those in the catalytic triad as well as the conserved GxSxG 437 motif were excluded from mutagenesis. The remaining 14 438 residues were individually substituted with alanine (alanine 439 scan). The resulting mutants were first evaluated for BHET 440 hydrolysis activity (Figure S4). Two variants, R428A and V376A, showed \geq 1.2-fold higher activity than TfCa wt and 441 442 were thus selected for further investigations (Figures 3A and 443 S4). R428 and V376 have rather bulky side-chains, which are assumed to affect the substrate binding. As a result, an alanine 444 substitution may possibly provide additional space to 445 accommodate larger substrates like BHET. By contrast, the 446 I69A and M189A variants were completely inactive. These two 447 residues were then subjected to site saturation mutagenesis. 448 The variant I69W was found to be more than twofold active 449 than that of TfCa wt (Figure 3A), whereas none of the M189 450 site-saturated mutants was significantly more active with the 451 model substrate pNPA (Figure S5). Based on the complex 452 structures shown in Figures 1 and S3, we hypothesize that the 453 mutation I69W, similar to the residues F323 and F377, may 454 455 facilitate to interact with the aromatic moiety in the substrate. All three variants with significantly increased activity, 456 457 namely, TfCa^{R428A}, TfCa^{V376A}, and TfCa^{I69W}, were combined 458 in all possible variations (Figure 3A). The highest activity was 459 achieved with the mutant TfCa^{I69W+V376A}, which had a 3.3-fold higher activity on BHET than TfCa wt at 45 $^\circ$ C and is $_{460}$ designated as TfCa WA in the following descriptions.

We further investigated the thermostability of TfCa wt and 462 WA. Although TfCa WA has a lower $T_{\rm m}$ (60.3 °C) than TfCa 463 wt (64.5 °C) (Table S2), its relative residual activities after 1 h 464 incubation at 45, 50, and 55 °C were comparable to those of 465 TfCa wt (Figure 3B). In contrast, TfCa WA became inactive 466 after 1 h at 60 °C whereas TfCa wt had still 40% of its initial 467 activity. Based on these results, we determined the temperature 468 profile of both enzymes for BHET hydrolysis in the 469 temperature range of 45–55 °C (Figure 3C). Although a 470 substrate conversion at a similar level of approximately 80% 471 was obtained with both enzymes after a 6 h reaction at 45 and 472 50 °C, an overall lower BHET conversion of nearly 60% was 473 determined at 55 °C (Figure 3C). At reaction temperatures up 474 to 50 °C, TfCa WA-catalyzed BHET hydrolysis yielded higher 475 amounts of TPA than TfCa wt. Because the biocatalytic 476 conversion of BHET to TPA requires two ester bond 477 cleavages, this suggested a superior hydrolytic activity of 478 TfCa WA over wt at up to 50 °C. Although TfCa wt showed a 479 marginally higher yield of TPA from BHET hydrolysis at 55 480 °C, the considerably lower total substrate conversion levels 481 with both enzymes exclude this temperature as the ideal 482 reaction condition. Thus, 50 °C appeared to be the optimal 483 temperature for BHET hydrolysis by both enzymes. Next, we 484 performed the enzymatic hydrolysis of MHET at 50 °C. At the 485



Figure 4. Degradation of various PET materials using a dual enzyme system. *Is*PETase PM is present in all samples, C: control without TfCa, wt: with 0.55 μ M TfCa wt, and WA with 0.55 μ M TfCa WA. The experiments were performed in 25 mM Tris–HCl buffer (pH 7.5, set at 45 °C). (A) Varying amounts of PET-NP (left: 2 μ g/mL, middle: 20 μ g/mL, and right: 200 μ g/mL) were degraded using 30 nM of *Is*PETase PM and 0.55 μ M of the indicated TfCa variant. The concentration of aromatic products was determined after 24 h of incubation at 45 °C. Aromatic products detected by HPLC include BHET, MHET, and TPA. (B) In the same set-up as shown in (A) with high-crystallinity GfPET powder (60 mg/mL) and amorphous PET film (60 mg/mL) as substrates in the presence of 50 nM *Is*PETase PM and 0.55 μ M of the indicated TfCa variant. Error bars indicate the standard deviations calculated from at least three replicates.

486 same substrate concentration of 2 mM, more than twofold 487 TPA was released from MHET compared to BHET with both 488 enzymes. TfCa WA yielded 3.3-fold and 2.6-fold more TPA 489 from the hydrolysis of BHET and MHET than TfCa wt, 490 respectively.

Finally, we compared the rates of TPA release as a result of 492 the enzymatic hydrolysis of MHET at various concentrations 493 ranging from 0.5 to 7 mM (Figure 3D). In agreement with the 494 other experiments described here, TfCa WA hydrolyzed 495 MHET at least three times faster than TfCa wt. The superior 496 activity of TfCa WA is more pronounced at higher substrate 497 concentrations up to 7 mM.

Degradation of PET Polymers Using a Dual Enzyme 498 499 System. We further used free TfCa in a dual enzyme system 500 in combination with a recently published variant of IsPETase 501 PM to degrade PET.²⁵ Based on its temperature profile 502 determined previously,²⁵ the degradation reaction was performed at 45 °C. At this condition, neither TfCa wt nor 503 504 TfCa WA can solely degrade PET-NP to release detectable 505 aromatic products (data not shown). First, varying amounts of 506 PET-NP (2, 20, and 200 μ g/mL) were degraded using the dual 507 enzyme system consisting of TfCa and IsPETase PM (Figure 508 4A). When only IsPETase PM was present, the main soluble 509 product was MHET independent of the substrate amount 510 used. By adding TfCa wt or its WA variant, TPA was the only s11 detectable product released from PET-NP. With 2 μ g/mL of 512 PET-NP, slightly decreased overall product yields were 513 obtained when TfCa enzymes are present. At higher substrate 514 concentrations, the overall product yield was up to 1.6-fold 515 higher with the TfCa WA based dual enzyme system than with 516 TfCa wt. The latter enzyme appeared to only convert the

MHET and BHET intermediates to TPA but did not further 517 boost the polymer degradation extent. 518

Next, we used the dual enzyme system to degrade the high- 519 crystalline GfPET powder and the amorphous GfPET film 520 (Figure 4B). These materials are less degradable for PETases 521 than PET-NP because of higher crystallinity and lower relative 522 surface area.³³ Therefore, we used higher substrate and enzyme 523 concentrations to simplify the detection of degradation 524 products. As shown in Figure 4B, the addition of TPA-ester 525 hydrolyzing enzymes has resulted in a markedly increased 526 overall yield of aromatic products with both GfPET film and 527 GfPET powder. When GfPET film was used as the substrate, 528 the overall yield is 3.4- and 4.2-fold higher, respectively, in the 529 presence of TfCa WA and TfCa wt compared to the reaction 530 with solely IsPETase PM. Accordingly, the overall product 531 yield improvements with GfPET powder were 4.7- and 5.2-fold 532 with TfCa wt and TfCa WA, respectively. Additionally, as 533 already observed in reactions with PET-NP, the addition of 534 TfCa enzymes eliminated almost completely the MHET 535 fraction in the degradation products. Overall, the TPA yield 536 was increased by 8.3-fold with PET-NP, 14-fold with PET 537 powder, and 11-fold with GfPET film as substrates using the 538 dual enzyme system with TfCa WA as a helper enzyme for 539 IsPETase PM. 540

DISCUSSION

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In this work, we elucidated the apo form as well as ligand- 542 soaked structures of the carboxylesterase TfCa and charac- 543 terized its enzymatic activity on (tere)phthalate-based oligo- 544 esters of various lengths. We found that BHET, an aromatic 545 para-diester, is the most easily hydrolysable substrate for TfCa. 546

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S47 When the diesters are ortho-positioned, like in DEP, or with S48 two aromatic moieties (BECBA), the specific activity becomes S49 lower but is still higher than the hydrolysis of MHET and other S50 monoesters (Figure 2). The aromatic monoester MEP has an S51 ortho-positioned carboxylic acid end group, and it cannot be S52 further hydrolyzed to PA by TfCa. Molecular docking of DEP S53 into the apo form of TfCa suggests that when MEP reenters S54 the active site, it cannot be further hydrolyzed due to its S55 unproductive positioning in the substrate-binding pocket S56 (Figure $SA_{,B}$). For the substrate 3PET, we suggest a





Figure 5. Docking results of various substrates to the TfCa apo structure. (A) Positioning of DEP in the active site of TfCa according to docking experiments. The ester closest to S185 will be cleaved, allowing EG and MEP to leave the active site. (B) The most favorable docking pose of MEP in the active site of TfCa is analogous to that after the hydrolysis event of DEP. In this manner, the ester bond in MEP cannot be hydrolyzed by the enzyme. (C) Positioning of 3PET, the largest substrate investigated, in the active site of TfCa supports the suggested degradation pathway. Residues from different domains are shown in brown (TfCa^{Hyd}), dark blue (TfCa^{LidA}), and cyan (TfCa^{LidB}). Ligands are shown as yellow sticks.

557 degradation pathway based on the analysis of the hydrolysis products. The first hydrolysis step of 3PET forms HEB and 558 559 BECBA, which is confirmed by docking results shown in 560 Figure 5C. The positioning of the oligo-ester in the substratebinding pocket of TfCa suggests a preferential hydrolysis of the 561 562 second ester bond (Figure 2) in 3PET, releasing the products 563 HEB and BECBA. While HEB should leave the binding site earlier in the hydrolysis event, BECBA could presumably bind 564 the same enzyme molecule more easily, allowing it to undergo 565 566 pseudo-processive hydrolysis to release MHET and BA. This 567 hypothesis is supported by the change of the product profile 568 determined by HPLC during the TfCa-catalyzed hydrolysis of 3PET (Figure S6). 569

We engineered TfCa toward higher oligo-ester hydrolyzing activity based on crystal structures of TfCa with different bigands. The mutant TfCa WA possesses a 3.3-fold higher activity in converting BHET to TPA compared to TfCa wt.

We used the variant TfCa WA in a dual enzyme system to s75 depolymerize PET together with a recently published variant s76 of *Is*PETase.²⁵ The addition of the carboxylesterase increased s77 the TPA yield in the reaction by up to 14-fold. Similar to s78 MHETase from *I. sakaiensis*, TfCa alone is not active on PET s79 but can promote the conversion of MHET, which is the major product of enzymatic PET depolymerization by many PET 580 hydrolases,³⁴ in a dual enzyme system with *Is*PETase PM. This 581 conversion will not only help to offset the inhibitory effect of 582 MHET on PET hydrolases, but it will furthermore aid in the 583 recovery of extremely pure TPA, which can be directly used for 584 the polymer synthesis.^{4,5} In the presence of immobilized TfCa, 585 an increased yield of TPA from PET film has been reported 586 with a dual enzyme system containing the PET hydrolases LC- 587 cutinase or TfCut2.¹⁵ The authors immobilized TfCa using a 588 SulfoLink matrix. This dual enzyme system resulted in an 589 increased overall product yield by 91% for TfCut2 and 104% 590 for LCC. Using another dual enzyme system containing 591 chimeric I. sakaiensis PETase and MHETase, Knott et al. 592 degraded the amorphous PET film (2-3% crystallinity, 593 Goodfellow, UK) at 30 °C for 96 h using 0.25 mg PETase 594 and 0.5 mg MHETase per gram PET.¹² IsPETase alone 595 produced approximately 0.2 mM TPA at this condition, 596 whereas the addition of free MHETase resulted in a twofold 597 higher TPA yield. The chimeric proteins of MHETase and 598 IsPETase constructed in the same study showed further 599 increased activity by up to sevenfold in comparison to the dual 600 free enzyme system.^{f2} In this study, we used a recently 601 published variant of IsPETase²⁵ in combination with TfCa wt 602 and WA. Compared to the results reported by Knott et al., we 603 yielded the same amount of TPA from the same substrate 604 (GfPET amorphous film) using 10% IsPETase (0.024 mg/g 605 PET) within one-fourth of the reaction time (24 h) at 45 °C. 606

In general, carboxylesterases such as TfCa are known to 607 exhibit similar functions and contain highly conserved regions. 608 We constructed a phylogenetic tree showing the relationship 609 between the different homologous sequences to TfCa (Figure 610 S8). Some of the strains we found in the phylogenetic tree, for 611 example, Thermobifida alba, Thermobifida halotolerans, and 612 Actinomadura hallensis, contain enzymes known to potentially 613 catalyze the PET polymer degradation.³⁵⁻³⁷ Furthermore, the 614 strains Actinomadura rubrobrunea, Actinomadura nitritigenes, 615 and Thermobifida cellulosilytica were mentioned in a 616 phylogenetic study on the characterization and isolation of 617 polyester degrading bacteria.³⁸ These findings lead to the 618 question of whether polyester depolymerases and oligomer 619 hydrolases co-exist in bacteria. Since both the PETase and the 620 MHETase were found in I. sakaiensis, the emergence of natural 621 dual enzyme systems appears to be a logical conclusion. 622 Additionally, I. sakaiensis was found to metabolize TPA and 623 possess a specific TPA translocation system.³⁹ However, the 624 lack of a specific transporter machinery for MHET in I. 625 sakaiensis invalidates the assumption that the extracellular 626 PETase and intracellular MHETase can work synergistically 627 during the bacterial assimilation of PET. Similarly, TfCa and 628 TfCut2, the artificially synergistic enzymes in PET depolyme- 629 rization, are derived from the same species of T. fusca.¹⁵ Unlike 630 I. sakaiensis, the genome of T. fusca⁴⁰ does not encode any 631 potential TPA metabolic pathway. Kleeberg et al. have grown a 632 T. fusca strain on mineral salt agar using a TPA-containing 633 aliphatic-aromatic co-polyester as the sole carbon source.⁴¹ 634 Although the polyesters depolymerized rapidly during the 635 culturing process, only poor bacterial growth was observed. 636 This is in line with the aforementioned genome analysis, which 637 suggests T. fusca cannot effectively metabolize PET degrada- 638 tion products, including MHET. As T. fusca is extremely 639 unlikely to be able to translocate MHET into the cytosol, 640 similar to I. sakaiensis, the role of TfCa in PET depolymeriza- 641 tion in the natural environment remains elusive. 642

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The ability of TfCa to degrade the ortho-phthalate ester 643 644 DEP broadens its substrate specificity. DEP is not only an 645 ortho-phthalate ester but also one of the widely used 646 plasticizers, which are produced annually on a million-ton 647 scale. Plasticizers are added to various polymer materials to 648 alter their properties for easier raw material handling or to ⁶⁴⁹ meet the application demands required for the end products.⁴² 650 However, phthalate-ester-based plasticizers like DEP are 651 known to have endocrine-disrupting, carcinogenic, teratogenic, 652 and mutagenic effects on humans and wildlife.⁴³ As a result, an 653 efficient decontamination of phthalic esters is a global concern. 654 PA can be assimilated by various microbes and used as a 655 carbon source.⁴⁴⁻⁴⁶ PA-ring opening enzymes, such as 656 dioxygenases and carboxylesterases, are needed by the PA 657 assimilating species like Rhodococcus, Sphingomonas, or 658 Arthrobacter and others. Nonetheless, our phylogenetic analysis (Figure S8) indicates that these strains are unlikely to express 659 660 TfCa homologous enzymes. Although the promiscuous 661 hydrolytic activity of TfCa on aromatic oligo-esters in nature 662 is still unknown, the recombinant form of this enzyme has the 663 potential to find ideal application scenarios in the area of 664 environmental biocatalysis and remediation.

In conclusion, the apo and complex crystal structures of 665 666 TfCa solved in this study shed light on the mechanistic aspects 667 of this enzyme in the hydrolysis of aromatic oligo-esters. These 668 findings allow us to rationally engineer TfCa and applied its 669 most active WA variant in a simple dual enzyme system to 670 relieve product inhibition during enzymatic PET depolymeri-671 zation. In comparison to previous efforts that employed cross-672 linked MHETase and IsPETase or immobilized TfCa, our 673 simplified dual enzyme system provides a more efficient and 674 less costly solution, which may hold greater promise for 675 industrial-scale applications.⁴⁷

ASSOCIATED CONTENT 676

677 Supporting Information

678 The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acscatal.2c03772. 679

Materials and methods; data collection of crystal 680 structures; melting temperature of TfCa mutants with 681 increased activity towards BHET; individual contribu-682 tions of amino acid residues to ligand binding for TfCa 683 and MHETase; ligand binding and unbinding events 684 defined by the catalytic C-O distance for individual 685 protein-ligand complexes with MHET as the ligand; 686 number of snapshots clustered based on the catalytic 687 distance; sequence alignment of TfCa with *p*-nitrobenzyl 688 esterase (pNB-E) and a carboxylesterase; structural 689 alignment of TfCa with p-nitrobenzyl esterase and a 690 carboxylesterase; ligand-soaked structure of TfCa with 691 ligand BHET as well as apo form of TfCa docked with 692 DEP and MEP; alanine scan of the substrate binding 693 pocket of TfCa; semi-rational enzyme engineering of 694 TfCa based on the elucidated structure; hydrolysis of 695 3PET by TfCa over a time course of 6 h; exo-PETase 696 function of TfCa; relation of TfCa to enzymes with 697 similar sequences; putative degradation pathways for 698 3PET; comparison of residues contributing to the 699 binding of MHET in TfCa and MHETase; confirming 700 MEP as the product of DEP degradation by TfCa; and 701 nucleotide and protein sequence of TfCa wt (PDF) 702

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821 Notes

822 The authors declare no competing financial interest.

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ABBREVIATIONS

BA BECBA	benzoic acid 4-{[2-(benzoyloxy)ethoxy]-carbonyl} benzoic acid	830 831
BHET	bis(2-hvdroxyethyl) terephthalate	832
DEP	diethyl phthalate	833
DMSO	dimethyl sulfoxide	834
DSF	differential scanning fluorimetry	835
EG	ethylene glycol	836
GfPET	amorphous PET film purchased from Good-	837
	fellow Ltd.	
HEB	2-hydroxyethyl-benzoate	838
HPLC	high-performance liquid chromatography	839
IPTG	isopropyl β -D-thiogalactopyranoside	840
IsPETase PM	a variant of PETase from Ideonella sakaiensis	841
LC-MS	liquid chromatography coupled with mass	842
	spectrometry	
MEP	monoethyl phthalate	843
MD	molecular dynamics	844
MHET	mono(2-hydroxyethyl) terephthalate	845
MHETA	4-[(2-hydroxyethyl) carbamoyl] benzoic acid	846
MR	molecular replacement	847
Ni-NTA	Ni ²⁺ -nitrilotriacetic acid	848
OD ₆₀₀	optical density measured at 600 nm	849
NP	nanoparticle	850
PA	phthalic acid	851
PET	polyethylene terephthalate	852
PETase	PET hydrolase	853
pNPA	para-nitrophenyl acetate	854
<i>p</i> -NP-Е	<i>p</i> -nitrobenzyl esterase	855
T. fusca	Thermobifida fusca	856
TfCa	carboxylesterase from T. fusca	857
$T_{\rm g}$	glass transition temperature	858
$T_{\rm m}$	melting temperature	859
TPA	terephthalate	860
WA	TfCa variant ^{169W/V3/6A}	861
3PET	bis[2-(benzoyloxy)ethyl] terephthalate	863

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Structural Insights into (Tere)phthalate-ester Hydrolysis by a Carboxylesterase and its Role in Promoting PET Depolymerization

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Methods

Cloning and site-directed mutagenesis for crystallography

The gene encoding TfCa (GenBank accession number: GAZ65068.1) from *Thermobifida fusca* KW3 was chemically synthesized by GENE ray Biotech Co. (Shanghai, China) and ligated into the pET32a vector. TfCa E319L mutant was prepared by using the QuikChange site-directed mutagenesis kit (Agilent Technologies, Santa Clara, CA, USA) with the TfCa-encoding plasmid as the template. The PCR products were incubated with DpnI (New England Biolabs, Hitchin, UK) to digest the original DNA template and then separately transformed into the *Escherichia coli* strain XL1-Blue. The mutations were confirmed by sequencing.

Protein expression and purification for crystallography

The TfCa-gene harboring plasmid was transformed into *E. coli* BL21trxB(DE3) cells which were grown in lysogeny broth (LB) medium at 37°C to an optical density (OD₆₀₀) of approximately 0.8 and then induced with 0.6 mM isopropyl β -D-thiogalactopyranoside (IPTG) at 16°C for 20 h. Cells were harvested by centrifugation at 5,000 x g for 15 min and then re-suspended in lysis buffer containing 25 mM Tris-HCl, pH 7.5, 150 mM NaCl and 20 mM imidazole, followed by disruption with a French Press (800-1200 bar, 2-5 cycles until homogenization). Cell debris was removed by centrifugation at 17,000 x g for 1 h. The supernatant was then applied to a Ni²⁺-NTA column with FPLC system (GE Healthcare, Chicago, USA). The target proteins were eluted at approximately 100 mM imidazole when using a 20250 mM imidazole gradient. Each protein was dialyzed against a buffer containing 25 mM Tris-HCl, pH 7.5, 150 mM NaCl, and subjected to tobacco etch virus (TEV) protease digestion overnight to remove the hexa-histidine (6×His) tag. The mixture was then passed through another Ni-NTA column. The untagged protein was eluted with 25 mM Tris-HCl, pH 7.5, 150 mM NaCl. The purity of each protein (> 95%) was checked by sodium dodecyl sulfate polyacrylamide gel electrophoresis (SDS-PAGE) analysis. Each of the purified proteins was concentrated to 40 mg/mL for crystallization screening.

Solid phase extraction and product identification with mass spectrometry

Prior to liquid chromatography mass spectrometry (LC-MS), solid phase extraction (SPE) was performed. For that purpose, the SPE cartridge (C18e) was conditioned $2\times$ with 1 mL acetonitrile and equilibrated with 1 mL distilled water. The sample was applied to the cartridge and washed with 1 mL distilled water. The solution 2×0.5 mL 1:4 (v/v) acetonitrile:water solution and afterwards the solvent was removed from the sample using TurboVap® (Biotage, Upsala, Sweden). Finally, the residues were dissolved in 100 µL of 1:4 (v/v) acetonitrile:water solution.

For the determination of the mass of the degradation products obtained from TfCa-catalyzed conversion of diethyl phthalate (DEP), the sample was injected without column into an Agilent 6460 Triple Quadrupole LC/MS system. The product ion scan was carried out in the negative mode in a range of mass to charge ratio (m/z) 70-300 with a collision energy of 6 V.

Molecular dynamics simulations

The crystal structure of TfCa with the ligand MHETA (PDB-ID: 7W1J, 1.92 Å) as well as the chain A structure of MHETase from *I. sakaiensis* (PDB-ID: 6QGA, 2.1 Å)^{5,6} were used for molecular dynamics (MD) simulations. Residues of the enzymes were numbered according to UniProt (UniProt IDs: TfCa: P86325 and MHETase: A0A0K8P8E7). All proteins were minimized⁷ and hydrogen atoms were added at pH 7.0.^{8,9} The three-dimensional structure of MHET was prepared in Avogadro¹⁰ and the

geometry was optimized using steepest descent algorithm until convergence using the MMFF94 molecular mechanics force field level of theory.¹¹ The optimized structure of MHET was parametrized for molecular dynamics using the R.E.D. server with default settings.¹²

The input topologies and coordinates of the enzyme and the ligand were prepared^{13,14} for MD simulation. Crystallographic waters were added to the systems and an octahedral set of water molecules¹⁵ was added leaving all atoms of the protein in a distance of at least 10 Å to the octahedron's surface. The average volumes of the equilibrated systems were used to add ions for a final NaCl concentration of 0.1 mol/L and the masses of the hydrogen atom-containing groups were repartitioned.¹⁶

Energy minimization was performed by 500 steps of steepest descent followed by 500 steps of conjugate gradient over five rounds with decreasing harmonic restraints. The subsequent MD simulations employed periodic boundary conditions, with treated electrostatic interactions¹⁷, a 10 Å cutoff for nonbonded interactions, and a 4-fs time step to fix all bonds containing hydrogens.¹⁸ Equilibration simulations consisted of two steps: (I) 40 ps of gradual heating from 0 to the final temperature of 310 K (37 °C) at constant volume using a Langevin thermostat with a collision frequency of 1.0 1/ps, and with harmonic restraints of 200.0 kcal/(mol·Å) on the positions of all solute atoms, and (II) 8,800 ps at the final temperature using the Langevin thermostat at a constant pressure of 1.0 bar using a pressure coupling constant of 1.0 ps. A production phase of the simulation was run with the same settings as in equilibration phase II for 20 ns. In total, three separate 20 ns long MD replicates were run for each system using the same settings as the second step of MD equilibration. Coordinates were saved at intervals of 4 ps. In total, 60 ns of simulation time was produced for each enzyme-ligand system.

Each enzyme-substrate complex was clustered into three trajectories and the molecular mechanics/generalized Born surface area (MM/GBSA)^{19,20} method was applied to calculate the binding free energy (ΔG_{bind}) of MHET in the enzymes and the respective residue-by-residue interactions. Solvents and ions were removed from the original topology files of each system²¹ to generate the corresponding topology files for the complex, receptor, and ligand. The ΔG_{bind} of the ligand in each structure was calculated.^{19,22}

Phylogenetic analysis of homologous enzymes to TfCa

A phylogenetic tree was built to identify homologous enzymes to TfCa. For this purpose, a blastp¹ search was conducted on the NCBI server (https://blast.ncbi.nlm.nih.gov/Blast.cgi) with the sequence of TfCa as the template. 53 sequences with an amino acid identity of 55 % or higher were extracted, and redundant sequences (CD-HIT, a cut-off with 0.99)² were discarded. The resulting 42 amino acids sequences were aligned using MUSCLE³ and the best model was determined based on ModelFinder (LG+F+I+G4).⁴ This model was then used for the tree-building process performed by IQTree.²³ The final tree was then visualized by FigTree (http://tree.bio.ed.ac.uk/software/figtree/) and edited with iTOL (https://itol.embl.de)

TABLES

	TfCa E319L with MHET and BHET	TfCa-apo	TfCa E319L with BHET	TfCa with MHETA
Beamline	SSRF-BL17B	SSRF-BL17U	SSRF-BL18U	SSRF-BL18U
Date	2021-07-04	2019-10-24	2021-07-11	2ß21-10-31
Exposure time/ frame	10 seconds (s)	0.1 s	0.5 s	0.3 s
Frame width	1	1	1	1
Total frames	400	360	400	600
Wavelength	1.0079	0.9792	0.9197	1.0331
Space group	P2 ₁	P2 ₁	P2 ₁	$P2_{1}2_{1}2_{1}$
a, b, c [Å]	44.74/110.24/ 53.42	45.27/112.96/54.7 8	44.52/109.93/53.2 4	55.43/79.94/113.0 7
α /β /γ (°)	90/106.42/90	90/106.04/90	90 /106.27/90	90/90 /90
Resolution (Å)	25.00 - 1.67 (1.73 - 1.67)	25.00 - 1.40 (1.45 - 1.40)	25.00 - 2.43 (2.52 - 2.43)	25.00 - 1.92 (2.03 - 1.92)
Unique reflections	56837 (5459)	103778 (10365)	18029 (1787)	38958 (2283)
Redundancy	7.4 (6.3)	6.6 (6.5)	7.2 (7.1)	13.2 (13.1)
Completeness (%)	98.7 (95.4)	99.4 (99.5)	99.7 (99.9)	99.3 (95.6)
Average I/σ(I)	17 (2.8)	27.2 (2.3)	11.7 (3.1)	15.1 (2.1)
CC 1/2	0.99 (0.84)	0.99 (0.86)	0.97 (0.89)	0.99 (0.82)
No. of reflections	56551 (5432)	103747 (9884)	17991 (1557)	38923 (3694)
No. of reflections (free set)	2832 (272)	5188 (494)	901 (78)	1946 (184)
R _{work} (95% data)	0.180 (0.223)	0.169 (0.225)	0.166 (0.216)	0.181 (0.293)
R _{free} (5% data)	0.208 (0.266)	0.186 (0.249)	0.224 (0.251)	0.218 (0.320)
Rmsd bonds (Å)	0.009	0.006	0.009	0.008
Rmsd angles (°)	1.13	0.94	1.01	0.91
Most favored (%)	96.77	96.56	95.96	97.15
Allowed (%)	3.23	3.44	4.04	2.85

Table S1: Data collection and refinement statistics of TfCa crystals.

Disallowed (%)	0.00	0.00	0.00	0.00
	Average B-fa	ctor/ Number of non	-hydrogen atoms	
Protein	15.4 / 3743	17.2 / 3735	28. 1 / 3743	30.3 / 3720
Ligands	26.5 / 33		36.6 / 18	41.7 / 15
solvent	26.3 / 689	30.2 / 730	29.2 / 210	36.9 / 444
PDB-ID	7W1I	7W1K	7W1L	7W1J

Values in parentheses are for the outermost resolution shells.

Table S2: Melting temperature of TfCa mutants with increased activity towards BHET. The melting temperature was determined using NanoDSF.

TfCa variant	melting temperature [°C]
wt	64.5
V376A	61.5
169W	62.9
R428A	64.3
I69W+V376A	60.3
V376A+R428A	60.8
I69W+R428A	62.2
I69W+V376A+R428A	59.4

Table S3: Individual contributions of amino acid residues to the ligand binding for TfCa and MHETase. Only amino acid residues of which the contribution to the binding energy is more than 1 kcal·mol⁻¹ in the catalytic pocket are included. The standard error reflects different interacting energy in individual snapshots from the MD simulations.

System	Residue	Pocket (<4.5 Å) [kcal·mol ⁻¹]
TfCa	I 69	-0.1 ± 0.1
	G 106	-1.4 ± 0.7
	G 107	-2.4 ± 0.9
	A 108	-3.6 ± 0.6
	E 184	-2.0 ± 1.7
	S 185	-2.5 ± 0.7
	A 186	-2.4 ± 0.8
	Q 263	-0.5 ± 0.7
	L 281	-0.7 ± 0.4
	L 282	-2.2 ± 0.4
	E 319	-0.1 ± 0.4
	Y 320	-1.2 ± 0.4
	F 323	-2.7 ± 0.6
	V 376	-0.7 ± 0.3
	F 377	-1.6 ± 0.4
	H 415	-1.5 ± 0.6
MHETase	S 131	-2.5 ± 0.6
	G 132	-2.8 ± 0.6
	S 225	-2.8 ± 1.1
	E 226	-2.0 ± 0.5
	L 254	-1.2 ± 0.4
	W 397	-3.2 ± 0.9
	Q 410	-0.2 ± 0.1
	R 411	-3.7 ± 0.8
	F 415	-1.8 ± 0.8

S 41	16	-1.5 ± 1.0
A 4	94	-0.9 ± 0.4
F 49	95	-1.9 ± 0.4
Н 52	28	-1.5 ± 1.0

Table S4: Ligand binding and unbinding events defined by the catalytic C-O distance for individual

 protein-ligand complexes with MHET as the ligand.

System	Leave	Return	In-between	Out
	(>4.5 Å)	(<4.5 Å)	(4.5–10.0 Å)	(>10.0 Å)
TfCa wt	2	0	6	3
MHETase	2	0	2	0

Table S5: Number of snapshots clustered based on the catalytic distance. The snapshots were clustered for the catalytic distance: (i) up to 4.5 Å, (ii) 4.5 - 10.0 Å, and (iii) above 10.0 Å. Listed are numbers of snapshots in each cluster and their percentages. MHET was used as the ligand.

System	Pocket	In-between	Out	Pocket	In-between	Out
	(<4.5 Å)	(4.5-10.0 Å)	(>10.0 Å)	[%]	[%]	[%]
TfCa wt	13485	15578	937	45	52	3
MHETase	22688	7312	0	76	24	0

Figures



Figure S1: Sequence alignment of TfCa with *p***-nitrobenzyl esterase (pNB-E) and a carboxylesterase.** The sequence as well as the structural alignment of TfCa were carried out with an pNB-E from *Bacillus subtilis* (PDB-ID: 1QE3) and a carboxylesterase from *Geobacillus stearothermophilus* (PDB-ID: 2OGS). The residues building the catalytic triad are labeled with a grey triangle.



Figure S2: Structural alignment of TfCa with *p***-nitrobenzyl (pNB-E) esterase and Est55.** The apoform of TfCa was structurally aligned to pNB-E from *B. subtilis* (PDB-ID: 1QE3) and the carboxylesterase Est55 from *G. stearothermophilus* (PDB-ID: 6OGS). **A-C** show the structures of the three enzymes with their domains whereas **D** shows the superimposition of A-C.



Figure S3: Ligand-soaked structure of TfCa with ligand BHET as well as apo-form of TfCa docked with DEP and MEP. A) Close-up view onto the active site of TfCa soaked with BHET (PDB-ID: 7W1L, 2.43 Å). **B)** Close-up view on the active site of TfCa E319L soaked with BHET and MHET (PDB-ID: 7W1I, 1.67 Å) in the solvent channel.



Figure S4: Alanine scan of the substrate binding pocket of TfCa. Using the substrate BHET, the residual activity of 15 mutants, obtained from the alanine scan of the substrate binding pocket, was determined. Mutants with a residual activity above 120 % were chosen for further characterization. Mutant I69A completely lost its enzymatic activity. Error bars indicate the standard deviation calculated from at least three replicates.



Figure S5: Semi-rational enzyme engineering of TfCa based on the elucidated structures. Residue M189 was mutated using site-saturation mutagenesis (SSM). The activity of mutants was determined using the model substrate pNPA. The amino acid substitutions to C, F, T and W were not obtained by the SSM method. None of the mutants exerted a significant increase in activity over 120 % compared to TfCa wt.



Figure S6: Hydrolysis of 3PET by TfCa over a time course of 6 h. The release of products from hydrolysis of 2 mM 3PET by TfCa is plotted. Time-course samples were taken at the indicated times and analyzed by uHPLC.



Figure S7: Exo-PETase function of the carboxylesterase TfCa. PET-NP were pre-treated using *Is*PETase PM for 2 or 4 h. After inactivation of *Is*PETase PM, TfCa wt or WA were added, and the reactions incubated for another 24 h. The aromatic degradation products BHET, MHET and TPA were analyzed by HPLC. Error bars indicate the standard deviation calculated from at least three replicates.



Figure S8: Relation of TfCa to enzymes with similar sequences. A phylogenetic tree was built from sequences with 55 % identity to TfCa. Four clades are shown in green, purple, blue and yellow.



В



2-(benzoyloxy)ethyl 2-hydroxyethyl terephthalate BA



Figure S9: Putative biocatalytic degradation pathways of 3PET. Based on which of the four ester bonds in 3PET is firstly hydrolyzed, different degradation pathways are possible. We proposed the most likely pathway in Figure 2 according to our experimental results. Here, other possible degradation pathways are shown. A) Pathways resulting when 3PET is firstly hydrolyzed into HEB and BECBA. **B)** Pathways resulting when 3PET is firstly cleaved into 2-(benzoyloxy)ethyl 2-hydroxyethyl terephthalate and BA. The ester bonds are numbered from one to four.



Figure S10: Comparison of residues contributing to binding of MHET in TfCa and MHETase. A) The residues contributing by more than 1 kcal/mol to the binding of MHET in TfCa are labeled and shown as sticks. **B)** The residues contributing by more than 1 kcal/mol to the binding of MHET in MHETase are labeled and shown as sticks. The MHET ligand is shown in yellow.



Figure S11: Confirming MEP as the product of DEP degradation by TfCa. The mass peaks resulting from LC-MS are shown for negative control measurement (blue), degradation sample (red) and the product ion scan for the degradation sample (green). The product ions were compared to Mass Bank (<u>https://massbank.eu/MassBank/RecordDisplay?id=UF420553&dsn=UFZ</u>) and were confirmed to be congruent with the product ions of MEP.

<u>Nucleotide Sequence</u> of TfCa wt including His-tag (yellow), TEV-protease cleavage site (gray) and linker region (green)

$\verb+atgcatcatcatcatcatgaaaatctgtattttcaggggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggtgcaggcgcaggtgcaggtgcaggcgcaggtgcaggcgcaggtgcaggtgcaggcgcaggtgcaggcgcaggtgcaggcgcaggtgcaggcgcaggtgcaggcgcaggtgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggtgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcgcaggcgcaggcgcaggcgcaggtgcaggtgcaggcaggcgcaggcqcaggcqcaggcqcaggcgcaggcqcaggcqcaggcqcaggcqcaggc$

gtggaaattgttattcgtaccggtagcggtgatgttcgtggtagcaaagaaaatggcattgccgtgtttcgtggtattccgtatgcagaacctccggttggtgcacatcgttttacagctcctcgccctcctcgtccgtgggatggtg ${\tt ttcgtgatgcaaccgaatttagcgcaaccgctccgcgtcctccgtatccggaagcaattggtgcactgctgattg}$ $a \verb+acgttttattccgggtgatgattatctgaccctgaatgtttggacaccggatccgaatgcagttggtctgccgg$ ${\tt ttatggtttggattcatggtggtgcatttaccaatggtagcggtagcgaaccggtttatgatggtgcagcatttg}$ $\verb|cacgtgatggtgttgttttttgtgagctttaattatcgcctgggcattattggttttgcagatctgccggatgcac||$ cgagcaatcgtggtctgctggatcagattgcagcactggaatgggttcgtgataatattgcacgtttcggtggcgatccgggtaatgttaccgttttttggtgaaagcgcaggtgcaatgagcgtttgtaccctgatggcaacaccgcgtgcacgtggtctgtttcgtcgtgcaattctgcagagcggtgcaggtaatatggcagttgcagcagaagatgcaaccaagctgctggatgttcagcagcaggttgcacaggaaattcagggagcacctgatccggcagtttggggtgaacgtattgcaggtggtagcgttctgctgcctttcgcaccggttattgatggtgaactgctgtctcagcgtccggcagaagcaattgccggaggcgcaggtcatgatgttgatctgctgtttggcaccaccaccgatgaatatcgtctgtttctgg ${\tt ctccgaccggcctgctgccgtttattaccagcgattatgttaccgcacatctggctaaaagcggtctggatgcag}$ atgcagcaaaagcatataccgcagaaggtcgcggcgaagaaccgggtgatattctggccagcattattaccgatcaggtgtttcgtattccggcactgcgtattgcagaaagccgtgttgatgcaccggcaccgcacctttggttatgaat $\verb|ccctggatcgtgcagcaagcctggttggcaccaatccgccggaagaactggccgaaaccgttcataatgcatggg||$ ${\tt ttcgttttgcaaccagcggtgatccgggttggccggcatggaatccggaaacccgtagcgttatgcgttttgatc}$ atccggttagcgaaatggttaccgatccgtatccggcaacacgtgcactgtgggatggcgttccgctgtga

2

<u>Protein Sequence</u> of TfCa wt including His-tag (yellow), TEV-protease cleavage site (gray) and linker region (green)

MHHHHHHENLYFQGAGAGAGAGAG VEIVIRTGSGDVRGSKENGIAVFRGIPYAEPPVGAHRFTAPRPPRPWDG VRDATEFSATAPRPPYPEAIGALLIERFIPGDDYLTLNVWTPDPNAVGLPVMVWIHGGAFTNGSGSEPVYDGAAF ARDGVVFVSFNYRLGIIGFADLPDAPSNRGLLDQIAALEWVRDNIARFGGDPGNVTVFGESAGAMSVCTLMATPR ARGLFRRAILQSGAGNMAVAAEDATTIAAVIAHRLGVEPTAAALAHVPVAQLLDVQQQVAQEIQGAPDPAVWGER IAGGSVLLPFAPVIDGELLSQRPAEAIAGGAGHDVDLLFGTTTDEYRLFLAPTGLLPFITSDYVTAHLAKSGLDA DAAKAYTAEGRGEEPGDILASIITDQVFRIPALRIAESRVDAPARTFGYEFAWRTPQLDGILGACHAVELPFVFR TLDRAASLVGTNPPEELAETVHNAWVRFATSGDPGWPAWNPETRSVMRFDHPVSEMVTDPYPATRALWDGVPL

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Article III

Synthesis of Modified Polyvinyl Alcohols and their Degradation Using an Enzymatic Cascade

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Supporting information for this article is given via a link at the end of the document.

Abstract: Polyvinyl alcohol (PVA) is a water-soluble synthetic vinyl polymer with remarkable physical properties including thermostability and viscosity. Its biodegradability, however, is low even though a large amount of PVA is released into the environment. Established physical-chemical degradation methods for PVA have several disadvantages such as high price, low efficiency, and secondary pollution. Biodegradation of PVA by microorganisms is slow and frequently involves pyrroloquinoline quinone (PQQ)-dependent enzymes, making it expensive due to the costly cofactor and hence unattractive for industrial applications. In this study, we present a modified PVA film with improved properties as well as a PQQ-independent novel enzymatic cascade for the degradation of modified and unmodified PVA. The cascade consists of four steps catalyzed by three enzymes with *in situ* cofactor recycling technology making this cascade suitable for industrial applications.

Polyvinyl alcohol (PVA) is a water-soluble synthetic vinyl polymer consisting of a carbon-carbon backbone and repeating 1,3-diols. Due to its versatile properties, PVA is used in many industrial applications such as fabric and paper sizing, fiber coating, film for packaging and more.^[1] Although PVA was considered a biodegradable polymer, it has become a major pollutant of industrial wastewater.^[2] The printing and dyeing industries, in particular, are major PVA emitters. Treatment of PVA wastewater via chemical or physical methods such as adsorption, filtration, ultrasonic degradation or the Fenton reaction are cost intensive, inefficient and can cause secondary pollution. Hence, alternative approaches (e.g., via microorganisms or enzymes) are required for the remediation of wastewater contaminated by PVA.[1] Additionally, in comparison to conventional desizing methods, enzymatic PVA degradation can be carried out under mild conditions.^[3] Microbial degradation of PVA was already reported for bacterial strains such as Pseudomonas putida VM15C and VM15A and Spingomonas sp. SA3 and SA2^[4] and has been proposed as a two-step process, (i) oxidation of one or two adjacent hydroxyl groups and (ii) subsequent cleavage of the resulting mono- or di-ketone structure. Step one was found to be carried out by a PVA oxidase or a pyrroloquinoline quinone (PQQ)-dependent PVA dehydrogenase (PVA-DH) while an aldolase or a diketone hydrolase catalyze the second step.^[5] Kawai and Hu^[5b] hypothesized that the polymer is cleaved extracellularly by PVA oxidases which results in fragments small enough to enter the periplasmic space. They base their suggestion on two observations: (i) PVA oxidases were found extracellularly whereas PVA-DHs were discovered membrane bound or periplasmatic^[6] and (ii) oxidized PVA can be hydrolyzed by enzymes^[7] but can also undergo spontaneous oxidation.^[8] In the periplasm, the smaller PVA fragments are further oxidized by the PQQ-dependent PVA-DH. Aldolases or diketone hydrolases subsequently degrade the PVA further until it can be taken up by the organism through the inner membrane.[5b] However, some organisms express only PVA-DH and no PVA oxidases, which suggests that extracellular PVA degradation plays a secondary role.^[5b]

Despite the fact that the microbial mechanism for PVA degradation has been known for a long time, research on degradation of PVA with isolated enzymes has been scarce. Further investigation of PVA-DH from *Sphingopyxis* sp. 113 has failed to corroborate initial findings because the recombinantly expressed enzyme formed largely insoluble inclusion bodies.^[9] Wei *et al.*, however, further investigated *Stenotrophomonas rhizophila* QL-P4 and were able to efficiently express a novel PVA oxidase.^[10] Nonetheless, current literature suggests that PQQ-dependent enzymes are needed for a complete degradation of Main Text Paragraph. PVA. Since PQQ is an expensive cofactor, this method is unattractive for industrial purposes.

In this work, we demonstrate a PQQ-independent enzyme cascade for the degradation of PVA which can act on modified

and unmodified PVA. To improve the properties of the PVA polymer, we firstly generated PVA bearing succinylated hydroxyl groups. Specifically, starting from a partially acetylated PVA material was desirable to study new hybrid materials that may find future applications in the packaging industries. Introducing succinate groups on the free hydroxyl groups via simple ester forming reactions was deemed attractive in altering the lipophilicity and mechanical properties in a substrate dependent manner. Succinic anhydride was identified as a desirable modifier that is biorenewable and biodegradable, readily available at low cost and non-toxic.^[11] A further advantage is that this protocol avoids the formation of harmful by-products and uses water as the sole solvent. Films modified with different amounts of succinic acid were synthesized after establishing a general protocol for the creation of succinate-modified PVA samples (Scheme 1).



Scheme 1. Synthetic process for the preparation of succinylated PVA. The initial succinylation is carried out in water at 80 °C. Different amounts of succinic anhydride were added to the PVA suspension to yield water-soluble polymers with varying properties. After cooling and evaporation of water, the modified PVA was subsequently partially cross-linked.

Prior reports on the succinylation of (bio)polymers include cellulose as well as secondary derivatization of the resulting succinate hybrids.^[12] This process was exploited using varying amounts of succinic anhydride (2, 4 and 6 g per 30 g PVA) and yielded reproducibly the desired PVA blends. In the following the modified PVA will be referred to as PVA-2 (2 g succinic anhydride),

PVA-4 (4 g succinic anhydride) and PVA-6 (6 g succinic anhydride).

Though the focus was on developing a straightforward batch process, initial studies indicated that a continuous flow process is viable which may have advantages when scaling this to the multi-kg scale with regards to reproducibility, automation, safety, and efficiency. Upon casting the aqueous hybrid materials into plastic boxes and slow evaporation of water in a fume hood, thin polymer films were obtained that could be easily peeled and used for further analysis. Infrared spectroscopy was used as a technique of choice indicating a distinct change in the carbonyl stretching region (i.e., 1600-1800 cm⁻¹) which is in agreement with the introduction of succinate moieties; i.e., 1714 cm⁻¹ for unmodified PVA vs. 1703 cm⁻¹ for the succinate hybrid (Supporting Information (SI), Figure S1).

Further and more comprehensive testing was performed externally and indicated that key parameters can be altered effectively and in dependence of the amount of succinic anhydride used (SI, Table S1). As such, all succinate hybrids were characterized by excellent mechanical properties and retained the water solubility/dispersibility of the original PVA. These parameters are critical for future use as packaging materials, and the ability to dissolve in aqueous environments is expected to expedite biodegradation which is also supported by a slow onset of disintegration in soil (SI, Table S1).

Next, we developed an enzymatic cascade for the degradation of the modified PVA using three biocatalysts. This cascade can be performed as a one pot reaction including an *in situ* cofactor recycling. All enzymes used are well characterized and either easily recombinantly expressible in *Escherichia coli* or commercially available.^[13] The enzyme cascade consists of four steps (Scheme 2) for modified PVA but can also be applied for unmodified PVA, starting at step 2. In step 1, ester bonds in the derivatized side chains are hydrolyzed by the commercially available lipase TL-IM resulting in unmodified PVA. The lipase is described to be 1,3-specific and originates from *Thermomyces lanuginosus*. Additionally, the immobilized enzyme accepts substrates with bulky side chains, making it an ideal candidate for the PVA degrading enzyme cascade.

After cleaving the ester bonds, the hydroxyl groups are oxidized to ketones by an alcohol dehydrogenase from *Lactobacillus kefir* (LK-ADH) utilizing the cofactor NADP⁺ with formation of NADPH (Scheme 2, step 2).^[13a] These ketones are then further oxidized to esters by the cyclohexanone monooxygenase (CHMO) variant M15 originally from the organism *Acinetobacter calcoaceticus*. CHMO M15 is utilizing the cofactor NADPH with formation of NADP⁺.^[13b] This, in principle, leads to an advantageous *in situ* cofactor recycling. Finally, the newly formed ester bond can be cleaved by lipase TL-IM through hydrolysis which results in smaller fragments of the polymer. Hence, a total of three enzymes in a one pot cascade can cleave PVA to release oligomers that are more accessible to further degradation by e.g., microorganisms or may serve as building blocks for upcycling of the resulting material.


Scheme 2. Enzyme cascade for the degradation of modified and unmodified PVA. In step 1, the commercial lipase TL-IM removes the esters (HAc and HSuc) from the PVA via hydrolysis which results in unmodified PVA with 1,3-diol functional groups. These diols are then oxidized into ketones by LK-ADH, using NADP⁺ as the cofactor and converting it into NADPH. NADPH is the cofactor for the subsequent enzymatic Baeyer-Villiger oxidation of ketones into ester-bonds which is performed by CHMO M15. In the last step, the ester bond is cleaved, which results in smaller PVA fragments. For PVA without modification, the same cascade can be applied, starting then from step 2. For simplicity, only one distinct example cascade pathway is shown, of course, steps 2-4 can also occur at further functional groups.

Degradation of PVA can be measured by staining the polymer using iodide. According to the Finley method, PVA forms a green complex with iodide in the presence of boric acid with an absorption maximum at 500 nm.^[14] Changes in the staining of PVA due to degradation of the polymer can thus be detected by absorbance measurements. PVA was incubated with crude cell lysates containing LK-ADH and CHMO M15 as well as the immobilized TL-IM in a one pot reaction. As negative control, cell lysate without overexpressed enzyme was used to exclude an influence of the lysate on the polymer.

The enzyme cascade caused a decrease in absorbance of the derivatized PVA film solution at 500 nm compared to the negative control when investigated with the Finley method. The degradation performance of PVA-4 film was evaluated at a wide range of pH, temperatures, reaction times, enzyme ratios and amounts of cofactor (Figure 1). To investigate the temperature range of the enzymes used for the cascade, each enzyme was incubated for one hour at varying temperatures (4-50 °C). Subsequently, the residual activity of each enzyme was measured and plotted (SI, Figure S2). It was found that LK-ADH and CHMO M15 are less stable in comparison to the immobilized TL-IM. These results are in agreement with the enzyme description for the TL-IM provided by the manufacturer Novozymes. According to the manufacturer, TL-IM has a temperature optimum of 50-75 °C. Thus, steps 2 and 3 of the PVA degradation (Scheme 2) are considered the crucial steps in the enzyme cascade.

Next, the pH of the reaction was varied in a range from 7 to 9 and, based on the results shown in Figure S2, different temperatures for the cascade reaction were studied in a range from 20 to 35 °C. It was found that the enzymatic degradation of PVA-4 ideally takes place at pH 8.5 and 20 °C under the tested conditions (Figure 1). The time dependent stability of LK-ADH and CHMO M15 was investigated at 20 °C and pH 8.5 over 24 h by following the increase or decrease of NADPH using the substrates (*R*)-1-phenyl ethanol (LK-ADH) or cyclohexanone (CHMO M15) (Figure 3). While CHMO M15 retained 80 % of its activity for the

duration of the experiment, the activity of LK-ADH decreased by 20 % in 24 h at 20 °C. Hence, the degradation of PVA by the enzyme cascade can be performed at 20 °C over 24 h without a major loss of enzymatic activity. Furthermore, the optimal amount of cofactor for the reaction was investigated. Since the reaction contains an *in situ* cofactor recycling system and in step 2 NADP⁺ is firstly required by LK-ADH for the formation of ketones, only NADP⁺ was added to the reaction. It was found that the efficiency of the reaction increases with increasing amounts of NADP⁺ up to 4 mM. However, the reaction efficiency did not improve when more than 4 mM NADP⁺ were added to the enzyme cascade.

Lastly, for a sufficient cofactor recycling system, the optimal ratio of LK-ADH to CHMO M15 was investigated for the degradation of PVA film PVA-4. From the Finley method we found that enzyme ratios of 1:1 or 2:1 were most favorable for the enzymatic reaction (Figure 1). It should be mentioned at this point that the enzyme ratio and the amount of cofactor are most likely interdependent. The investigation of the enzyme ratio was performed with 4 mM NADP+ whereas the investigation of the optimal amount of cofactor was carried out with a 1:1 LK-ADH to CHMO M15 ratio. In the stability testing of the enzymes, shown in Figure 1, LK-ADH performed with a higher activity (0.053 U per µL) compared to CHMO M15 (0.009 U per µL) which could lead to the conclusion that LK-ADH will convert NADP+ faster into NADPH than CHMO M15 converts NADPH into NADP⁺. However, the activity assay was carried out with the substrates (R)-1-phenylethanol and cyclohexanone and the activity for those substrates cannot be directly transferred to PVA. However, the enzyme ratios for PVA degradation were investigated with 2 mM NADP⁺ (data not shown) and 4 mM NADP⁺ which led to similar conclusions regarding the optimal enzyme ratio.

Thus, the improved degradation reaction of PVA-4 with the proposed enzyme cascade contained 4 mM NADP⁺, LK-ADH and CHMO M15 in a ratio of either 1:1 or 2:1 carried out at pH 8.5 and 20 °C over 24 h.



Figure 1. Investigation of the effect of various conditions on the enzymatic degradation of film PVA-4. The reaction conditions were optimized regarding pH, temperature, reaction time, the ratio of ADH to CHMO and the amount of cofactor. The best conditions were found to be pH 8.5, 20 °C, 24 h with 4 mM cofactor NADP⁺. The activity of LK-ADH was measured by following the increase of NADPH when converting (*R*)-1-phenyl ethanol. The activity of CHMO M15 was measured by following the decrease of NADPH when converting (U) was defined as the amount of substrate converted per minute by one μ L of enzyme lysate.

Table 1. Average Mn and Mw of PVA-films unmodified PVA, PVA-2, PVA-4 and PVA-6 degraded by the enzyme cascade. The average and the standard deviations were calculated from three replicates.

LK-ADH to CHMO ratio	Film	Treatment	M _n [g/mol]	M _w [g/mol]	PDI
1:1	Unmodified PVA	Enzyme cascade	$\textbf{37850} \pm \textbf{144}$	161767 ± 2970	4.27
		Negative control	40667 ± 230	168167 ± 2702	4.14
		Enzyme cascade	$\textbf{33407} \pm \textbf{190}$	98373 ± 410	2.94
	FVA-2	Negative control	35607 ± 163	101433 ± 814	2.85
	PVA-4	Enzyme cascade	$\textbf{35719} \pm \textbf{663}$	105867 ± 2581	2.96
		Negative control	39527 ± 215	111367 ± 1380	2.82
	PVA-6	Enzyme cascade	34823 ± 704	106600 ± 800	3.06
		Negative control	38533 ± 135	110467 ± 3044	2.87
2:1	Unmodified PVA	Enzyme cascade	36147 ± 1809	145267 ± 424	4.02
		Negative control	39823 ± 351	161200 ± 2425	4.05
	PVA-2	Enzyme cascade	34030 ± 177	97460 ± 438	2.86
		Negative control	35683 ± 121	101267 ± 473	2.84
	PVA-4	Enzyme cascade	35177 ± 232	103120 ± 3201	2.93
		Negative control	39060 ± 170	110500 ± 2252	2.83
	PVA-6	Enzyme cascade	34197 ± 770	104200 ± 2128	3.05
		Negative control	37541 ± 1293	109133 ± 2011	2.91

Using gel permeation chromatography (GPC) the molecular mass of PVA before and after enzymatic treatment was also explored. Here, in addition to PVA-4, unmodified PVA as well as PVA-2 and PVA-6 were investigated as well for degradation with the enzyme cascade under the above-mentioned conditions. The polydispersity index (PDI), the number average molecular weight

 (M_n) and the weight average molecular weight (M_w) were calculated from the measurements (Table 1). PDI increased in most conditions tested when the PVA film was treated with enzymes, indicating a broadening of the molecular weight distribution in comparison to the untreated films which in turn is an indicator for degradation of the polymer. Additionally, a decrease in Mn and Mw was observed in samples containing the enzyme cascade in comparison to the negative control. When PVA samples were treated with the enzyme cascade, both, Mn and M_w decreased in comparison to untreated PVA. As already observed with the Finley method, the GPC measurements confirmed that the enzyme ratio 1:1 or 2:1 result in a similar reduction of Mn and Mw and hence, that changing the ratio of enzyme from 1:1 to 2:1 does not influence the reaction significantly. The largest decrease in Mn was observed in degradation reactions with film PVA-4. Independently of the LK-ADH to CHMO ratio, Mn decreased by 10 % when PVA-4 was treated with enzyme. The largest decrease in Mw, however, was measured for unmodified PVA. When using a 2:1 LK-ADH to CHMO ratio, Mw decreased by 10 % for unmodified PVA whereas for PVA-4 it only decreased by 7 %. In general, the proportional decrease of M_w was lower in comparison to M_n in most cases. The exception to this is the PVA film without modification. Using an enzyme ratio of 2:1, Mw was reduced by 10 % and Mn by 9 % when the film was incubated with the enzyme cascade. In comparison to that, an enzyme ratio of 1:1 reduced Mw by only 4 % and Mn by 7 % indicating that the enzyme ratio of LK-ADH to CHMO M15 has a higher impact on PVA without modification in comparison to modified PVA. This could be due to the additional step in the reaction of modified PVA for hydrolyzing the ester bonds in the derivatized side chains of the polymer which delays the subsequent reactions of ADH and CHMO in comparison to unmodified PVA. Enhancement of enzyme stability of ADH and CHMO as well as prolonged reaction time could hence potentially lead to similar yields for modified PVA as were gained for unmodified PVA. Furthermore, from a larger decrease of Mw in comparison to Mn it can be concluded that larger molecules were more readily degraded when an enzyme ratio of 2:1 was used for unmodified PVA. M_w is taking the weight of each polymer chain into account and hence the value is less influenced than Mn when smaller molecules are preferentially degraded. This in turn leads to the conclusion that larger amounts of LK-ADH are needed for the degradation of unmodified, larger weight PVA molecules. Even though LK-ADH was proven to tolerate a wide variety of substrates and to also accept bulky side chains^[15], the polymer is most likely challenging for the enzyme and an increase of the enzyme amount could hence help with degrading larger molecules. Enzyme engineering of LK-ADH towards acceptance of larger side changes could further improve the degradation rate of PVA.

In summary, a modification of PVA was achieved with succinic anhydride. This was realized via a simple chemical process using water as solvent at elevated temperature rendering succinylated PVA films through wet casting techniques. Most importantly, the here described novel enzyme cascade consisting of four steps carried out by three enzymes that can break down the modified PVA with improved properties as well as PVA without modification. The in situ recycling of the cofactor NADP(H) makes this enzyme cascade self-sufficient, more versatile, and applicable in comparison to published (microbial) systems for PVA degradation.

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Keywords: degradation • enzyme catalysis • enzyme cascade • plastic • polyvinyl alcohol • synthesis

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Entry for the Table of Contents



Enzymatic degradation of polyvinyl alcohol (PVA). Biodegradation of the water-soluble PVA by microorganisms is slow and frequently involves pyrroloquinoline quinone (PQQ)-dependent enzymes. In this study, we present a modified PVA film with improved properties as well as a PQQ-independent novel enzymatic cascade consisting of a lipase (TL-IM), an alcohol dehydrogenase (LK-ADH) and a Baeyer-Villiger monooxygenase (CHMO M15) for the degradation of modified and unmodified PVA.

Supporting Information ©Wiley-VCH 2021 69451 Weinheim, Germany

Synthesis of Modified Polyvinyl Alcohols and their Degradation Using an Enzymatic Cascade

Gerlis von Haugwitz, Kian Donnelly, Mara Di Filippo, Daniel Breite, Max Phippard, Agnes Schulze, Ren Wei, Marcus Baumann and Uwe T. Bornscheuer*

Abstract: Polyvinyl alcohol (PVA) is a water-soluble synthetic vinyl polymer with remarkable physical properties including thermostability and viscosity. Its biodegradability, however, is low even though a large amount of PVA is released into the environment. Established physicalchemical degradation methods for PVA have several disadvantages such as high price, low efficiency, and secondary pollution. Biodegradation of PVA by microorganisms is slow and frequently involves pyrroloquinoline quinone (PQQ)-dependent enzymes, making it expensive due to the costly cofactor and hence unattractive for industrial applications. In this study, we present a modified PVA film with improved properties as well as a PQQ-independent novel enzymatic cascade for the degradation of modified and unmodified PVA. The cascade consists of four steps catalyzed by three enzymes with in situ cofactor recycling technology making this cascade suitable for industrial applications.

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Table of Contents

Table of Contents
Experimental Procedures
Materials
Synthesis of succinate-PVOH-418 hybrids and generation of thin films
Production of enzymes
Degradation of PVA by the enzymatic cascade
Determining PVA concentration by a modified Finley method
Gel permeation chromatography
Characterization of enzymes regarding temperature stability
Results and Discussion
References
Author Contributions

Experimental Procedures

Materials

Polyvinyl alcohol (PVA) standards were purchased from PSS Polymer Standards Service GmbH (Mainz, Germany). Chemicals and consumables were purchased from Merck KGaA (Darmstadt, Germany), Sigma-Aldrich (Steinheim, Germany) and Thermo Fisher Scientific (Waltham, MA, USA) unless stated otherwise. Lipase *Thermomyces lanuginosus* immobilized on silica gel (Lipozyme TL-IM) was purchased from Novozymes (Bagsværd, Denmark). PVOH-418 was purchased from Sekisui Specialty Chemicals (Dallas, Texas, United States).

Synthesis of succinate-PVOH-418 hybrids and generation of thin films

A general synthetic protocol was established whereby solid succinic anhydride (2 g, 4 g or 6 g) was added to a solution/suspension of PVOH-418 (30 g in ca. 300 mL deionised water) and vigorously stirred at 80 °C for 5 h. The set-up thereby comprised of a Schott glass bottle (500 mL volume containing a 2 cm magnetic stir bar) and an IKA hotplate with magnetic stirring. Within 1 h a clear solution was obtained. This material was then poured without prior cooling into plastic storage boxes (ca. 40 x 20 cm) aiming for 25% of solution per box (usually 3 on this scale). After two days of evaporation in a ventilated space (i.e., a fume hood), films were peeled off and stored between paper to avoid curling.

Production of enzymes

The alcohol dehydrogenase from *Lactobacillus kefir* (LK-ADH) as well as the cyclohexanone monooxygenase (CHMO) variant M15, originally from *Acinetobacter calcoaceticus*, were recombinantly expressed in *Escherichia coli* (*E. coli*) BL21. For that purpose, cells were grown in lysogeny broth medium including 50 μ g/L ampicillin (Amp) overnight at 37 °C and 220 rpm. The main culture was grown in terrific broth medium including 50 μ g/L Amp and in the case of LK-ADH addition of 1 mM MgCl₂. Inoculation was done with 1 % of the main culture. Cells containing the plasmids for CHMO M15 were induced by autoinduction by adding 0.2 % lactose and 0.05 % glucose to the culture medium. The main culture was incubated for 3 h at 37 °C and afterwards for 21 h at 21 °C. Cells containing the plasmid for LK-ADH were grown at 37 °C until an OD600 of 0.5 and afterwards the enzyme expression was induced by adding 1 mM IPTG to the culture. The subsequent incubation took place at 21 °C for 21 h.

Cells were harvested by centrifugation at 10,000 ×g for 5 min, pellets were washed with 10 mM sodium phosphate buffer (pH 8.5). The pellet from a 50 mL main culture was resuspended in 10 mL 10 mM sodium phosphate buffer (pH 8.5) and lysed by sonication (3x1.5 min, 50 % pulse) with SONOPULS HD 2070 (BANDELIN electronic GmbH & Co. KG, Berlin, DE). The soluble fraction from the crude cell lysate was separated by centrifugation at 10,000 ×g for 30 min followed by filtration through a 0.2 µm membrane before usage.

Degradation of PVA by the enzymatic cascade

PVA was dissolved at 50 °C in 10 mM sodium phosphate buffer with a concentration of 40 mg/mL and the pH was adjusted to 8.5. 100 µL LK-ADH-lysate, 100 µL CHMO M15-lysate, 2 mg of immobilized lipase TL-IM and 4 mM NADP⁺ were added to 250 µL of the PVA stock solution and filled up to 500 µL with 10 mM sodium phosphate buffer (pH 8.5). As negative control *E. coli* BL21 lysate with an empty vector was used. Reactions were incubated for 24 h at 20 °C and 1000 rpm. Reactions were performed in triplicates unless stated otherwise. The analysis of samples regarding concentration of PVA was done by a modified Finley method. Analysis regarding the molecular weight of the remaining PVA after degradation was done by gel permeation chromatography (GPC). For GPC measurements the reactions were scaled up to a total volume of 2 mL.

Determining PVA concentration by a modified Finley method

For the determination of the PVA concentration, a modified Finley method according to Mohamed *et. al.*^[1] was used, which can colorimetrically quantify the green complex formed by PVA with iodide in the presence of boric acid.^[1b] A potassium iodide solution was prepared from 2.5 g/L KI and 12.7 g/L l₂. 40 μ L of potassium iodide solution were mixed with 60 μ L of boric acid (4 g/L) and 40 μ L of sample. Using a microplate reader (Infinite® M200 pro, Tecan Group Ltd. (Männedorf, Switzerland)) the absorbance of every sample was measured at 500 nm.

Gel permeation chromatography

Determination of the molecular weight was carried out using gel permeation chromatography (Tosoh EcoSEC, HLC-8320GPC, equipped with a pre-column (PSS Suprema Pre-column 10 μ , 8x50 mm) and three columns (PSS Suprema 10 μ , 1000 Å/100 Å/30 Å, 8x300 mm). The eluent flux and temperature were set to 1 mL/min and 45 °C, respectively. Mn, and Mw were then determined using the instrument's software.

Characterization of enzymes regarding temperature stability

Enzymes were incubated at different temperatures in the range of 4–50 °C for one hour. Afterwards, the residual activity was determined at 25 °C and pH 7. The activity of all enzymes was determined spectrophotometrically using different substrates. In the case of the lipase TL-IM, the formation of *p*-nitrophenol (pNP) from *p*-nitrophenyl acetate (pNPA) was monitored. For this purpose, 2 mg of TL-IM were added to 900 μ L of 50 mM sodium phosphate buffer (pH 7), followed by adding 100 μ L pNPA (10 mM in dimethyl sulfoxide (DMSO)) to start the reaction with a final substrate concentration of 1 mM. After one minute of reaction, the amount of pNP (extinction coefficient: ϵ = 17,500 M⁻¹cm⁻¹) was determined at 410 nm in a microplate reader.

For LK-ADH and CHMO M15 the increase or decrease of the co-factor NADPH was followed at 340 nm. Reactions were performed in a similar way as described for LK-ADH by Becker *et al.*² Prior to the reaction, LK-ADH lysate was diluted 1:40 and CHMO M15 was diluted 1:5. (*R*)-1-phenylethanol (LK-ADH) and cyclohexanone (CHMO M15) were used as substrates for the enzymes. 20 μ L of (diluted) lysate were added to 0.5 mM NADP(H) and 1 mM of the respective substrate in a total volume of 200 μ L.

Results and Discussion



Figure S1. Representative infrared spectra of PVOH-418 (left) and succinylated PVA (right). The spectra indicate a distinct change in the carbonyl stretching region (i.e., 1600-1800 cm⁻¹) which is in agreement with the introduction of succinate moieties; i.e., 1714 cm⁻¹ for PVOH-418 vs 1703 cm⁻¹ for succinylated PVA.



Figure S2. Investigating the optimal temperature of the enzymatic cascade. All three enzymes used in the cascade were investigated for their residual activity after incubation for one hour in a temperature range from 4-50 °C. While TL-IM remained 100 % residual activity over the whole temperature range, LK-ADH was only 20 % active after 1 h at 50 °C and the activity of CHMO M15 significantly decreased at temperatures over 30 °C.



Figure S3. Representative GPC chromatogram for enzyme degraded sample (green) and negative control (blue).

Criteria	Target	Suc2	Suc1	Suc3
Method of manufacturing	Pellet to film	Film via wet casting	Film via wet casting	Film via wet casting
Oxygen Transmission (cc/m²/day) *23°C, 0% humidity*	<10	21.7	22.2	29.9
Water Vapour (cc/m²/day) *38°C, 90% humidity*	<13.8 (1wk) <6.57 (2wk)	525.4	433.1	696.9
Avg. Gauge (µm)	25-120	42	141	95
Tensile Strength (N)	>50	196	77	60
Puncture (N)	>20	91	108	84
Dispersibility / Solubility @25°C		√ /x	√ /x	√ /x
Dispersibility / Solubility @40°C (sec) (avg)		39/110	72/1151	27/102
Dispersibility / Solubility @60°C		✓ /x	✓ /x	√ /x
Disintegration	6 months	n.a.	Small holes	8 weeks intact

Table S1. Summary of key parameters for different succinylated PVOH-418 materials. The chemical composition of the films differed in the amount of succinic anhydride: 2 g (Suc2), 4 g (Suc1) or 6 g (Suc3) were used per 30 g PVOH-418.

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Author Contributions

Conceptualization, U.T.B., M.B.; Substrate generation and characterization, K.D., M.D.F., and M.B.; Enzyme expression, characterization and enzymatic reactions, G.H.; Gel permeation chromatography measurements, D.B.; Writing – Original Draft, G.H., and M.B.; Writing, review and editing, all authors; Supervision and funding acquisition, R.W., M.B. and U.T.B.

Eigenständigkeitserklärung

Hiermit erkläre ich, dass diese Arbeit bisher von mir weder an der Mathematisch-Naturwissenschaftlichen Fakultät der Universität Greifswald noch einer anderen wissenschaftlichen Einrichtung zum Zwecke der Promotion eingereicht wurde.

Ferner erkläre ich, dass ich diese Arbeit selbstständig verfasst und keine anderen als die darin angegebenen Hilfsmittel und Hilfen benutzt und keine Textabschnitte eines Dritten ohne Kennzeichnung übernommen habe.

Gerlis Maria von Haugwitz

List of Publications

R. Wei, <u>G. von Haugwitz</u>, L. Pfaff, J. Mican, C. P. S. Badenhorst, W. Liu, G. Weber, H. P. Austin, D. Bednar, J. Damborsky, U. T. Bornscheuer, Mechanism-Based Design of Efficient PET Hydrolases, *ACS Catal.*, **2022**, 12, 3382–3396.

<u>G. von Haugwitz</u>, X. Han, L. Pfaff, Q. Li, H. Wei, J. Gao, K. Methling, Y. Ao, Y. Brack, J. Mican, C. G. Feiler, M. S. Weiss, D. Bednar, G. J. Palm, M. Lalk, M. Lammers, J. Damborsky, G. Weber, W. Liu, U. T. Bornscheuer, R. Wei, Structural Insights into (Tere)phthalate-ester Hydrolysis by a Carboxylesterase and its Role in Promoting PET Depolymerization, *ACS Catal.*, **2022**, accepted.

<u>G. von Haugwitz</u>, K. Donnelly, M. Di Filippo, D. Breite, M. Phippard, A. Schulze, R. Wei, M. Baumann, U. T. Bornscheuer, Synthesis of Modified Polyvinyl Alcohols and their Degradation Using an Enzymatic Cascade, *Angew. Chem. Int. Ed.*, under review.

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